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STATISTICAL REPORT OF THE MANUFACTURING
DATA OF M30A1 PROPELLANT



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Note

This report is the first in a planned series of the study of high pressure-temperature coefficient propellant for the M203 charge. Contained in this report is propellant data for FY77 and FY79 production. As data for FY80 and subsequent years becomes available, this report will be updated and continued until the high pressure-temperature coefficient problem is resolved.

Acknowledgments

The authors wish to express appreciation to Radford AAP for furnishing all manufacturing data, and to MISD for providing computer programs for speeding up the analysis.

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Abstract

The M203 propelling charge had exhibited a high lot to lot variability of gun pressure (at hot firings) in the recent production lots. A statistical analysis was conducted to search for possible cause of the variability.

> A computer data file was generated for storing the data. Two computer programs provided by MISD were used for speeding up the analysis. In addition several computer programs were written to retrieve data for the plotting routine and for the stepwise regression analysis.

Two types of trends were observed from the plots and were summarized in Appendix 1. Results of the stepwise regression indicated that the pH value (Nitroguanidine) and % Total Volatile (composition) show a relatively high correlation to the gun pressure (at hot firings), also, the % Graphite (composition) and the combination of % Total Volatile (composition) and % Moisture (Potassium Sulfate) exhibit a functional relationship with the DP/DT (70 to 145)^oF (difference in pressure/at different temperature range). A summary of the final regression results is presented in Appendix 2.

Some major changes in the source of ingredients and process conditions were observed from Radford Manufacturing data. In FY79, the supplier of the Ethyl Centralite was switched from Chemische Werke, West Germany to Van de Mark, New York. The source of Potassium Sulfate was also changed from Naval Ammo Depot Crane, Ind. to Mellinekrodt Inc. In the same year, the amount of graphite added to the process of blending/glazing was reduced from 5 lb 6.4 oz to 3 lb per 5400 pounds of propellant.

- V -

Introduction

M30Al propellant produced in FY77 for the 155MM M203 propelling charge exhibited a pressure - temperature coefficient of approximately 60 psi/ $^{\circ}$ F at the temperature range from 70 $^{\circ}$ F (ambient) to 145 $^{\circ}$ F (hot). All the hot firings of these particular M203 prop charges resulted in relatively low pressures. The same type of propellant manufactured in FY79 has exhibited a pressure temperature coefficient of about double the coefficient observed in FY77 production. The hot firings in this case have resulted in higher pressures. These high pressures have significantly reduced the safety margin between the service pressure and maximum pressure requirements, which were enjoyed from FY77 production.

To investigate the cause of variability of the pressure - temperature coefficient, Radford AAP was requested to furnish all manufacturing data including those acceptance test results of all ingredients.

This report is a statistical analysis of all the data provided by Radford AAP.

Discussion

A statistical analysis of all manufacturing data including the acceptance test results of all ingredients was conducted. The purpose of this analysis is to search for any functional relationships between the manufacturing data and pressure - temperature coefficient. Besides the pressure - temperature coefficient, other output results, such as the closed bomb and peak chamber pressure, were also considered during the analysis. Since the output results depend highly on the manufacturing data (purity of the ingredient, process, etc) therefore, the output results in this case are defined as dependent (or response) variables and the manufacturing data defined as independent variable. The dependent and independent variables which were considered in this analysis are summarized in Table 1 and Table 2, respectively.

Two types of approach have been utilized in this analysis. The first approach is to plot the manufacturing data against the pressure - temperature coefficient or other output results. By plotting, a decreasing or increasing trend could be easily identified. The second approach is to conduct a stepwise regression analysis on those variables.

This stepwise regression is a statistical procedure of selecting the best correlated independent variables for a particular dependent variable, and fit them into a regression equation. A preselected F value, $F(1,n-2,\alpha)$, is required in this stepwise procedure and is highly dependent on the degrees of freedom ($n-2$; where n is the number of observation) and the specified percent of confident level (α) of the entering independent variable. The preselected F value in this particular analysis is 5.12 and was obtained from the F distribution table at $F(1,7,0.95)$. The process of selecting is based on the partial F value calculated at each stage. If the calculated F value of a entering independent variable is greater than the preselected F value, the variable will be retained into the regression equation; otherwise, the variable will be rejected and another variable will be entered. This process is continued until no more variables will be entered and no more are rejected.

After selecting the best variables through comparison of the F values, a correlation coefficient (R^2) will be calculated. This correlation coefficient is an indicator of measuring the degree of correlation of the variables. As the correlation coefficient approaches to unity, the regression equation obtained from the stepwise procedure will become a precise model representing the relationship between the independent and dependent variables. This equation will be further used to predict the outcome of the dependent variable with a given value of the independent variable.

Because of a large amount of data involved, a computer data file was then generated to store them. Two computer programs provided by MISD were utilized to speed up the analysis. One program is used to plot graphs and the other one is used to conduct the stepwise regression analysis. Several computer programs were also prepared to retrieve data for plotting and as well as for the stepwise regression analysis.

After plotting all the manufacturing data against the pressure data or other output tested results, two types of trends were actually observed with the following classification (a) strong trend (b) slight trend. Both of these trends are summarized in appendix 1.

Four independent variables which belong to the strong trend category have been retrieved for the stepwise regression analysis. The dependent variables which are used in the regression are the pressure data (fired at 145°F) and DP/DT (70 to 145°F, difference of pressure data at the temperature range from 70 to 145°F). The result of the regression has indicated that the pH value (nitroguanidine), contained F value equal to 15.837, and % graphite, contained F value equal to 30.90, show a relatively high correlation to the pressure at 145°F and DP/DT (70 to 145)°F, respectively. A summary of the final result of regression analysis is presented in Appendix 2.

One major problem noted during the analysis was that some data represented the ingredients at time of purchase rather than when it was utilized. For example, all the average particle diameters of the nitroguanidine were measured at the source. This material was then stored for several years before use. Because of inadequate storage conditions, the crystal structure is believed to have grown. Although this report showed no correlation of nitroguanidine size with pressure obtained, analysis of particle size at the time of use might correlate. But this additional data was not available at the time of this analysis. Also some parameters upon review showed little to no variation in recorded values and were not utilized in this analysis. In addition, some major changes which were noted from the Radford manufacturing data are important enough to be mentioned in this report. These changes are as follows:

1. Changes in source of ingredients:

a. In 1977, the original supplier of Ethyl Centralite was Chemische Werke, West Germany. In FY79, Van De Mark, New York has become the new supplier of this ingredient.

b. Potassium Sulfate was originally obtained from Naval Ammo Depot Crane (manufacturer unknown) and is currently obtained from Mallinckrodt.

2. Changes in process conditions: In FY79 the amount of graphite added to the process of blending/glazing was reduced from 5 lb 6.4 oz to 3 lb per 5400 pounds of propellant.

Conclusions

1. The analysis of data showed the following:

a. Data plottings of independent variables (e.g. % Total Volatile, % Ethyl Centralite, etc.) vs dependent variables (e.g. pressure at 145°F, DP/DT (70 to 145)°F, RQ, etc) indicates the existence of strong and slight trends (see Appendix 1). For example, several independent variables (e.g. % Graphite, % Total Volatile, pH of Nitroguanidine, etc.) appear strongly to increase the pressure (145°F) of the propellant.

b. Results of stepwise regression analysis indicated that the pH of Nitroguanidine and % Graphite in the propellant show a relatively high correlation to the pressure at 145°F and DP/DT (70 to 145)°F (difference of pressure at temperature range from 70 to 145°F), respectively. A summary of the final results is presented in Appendix 2.

2. There was insufficient data available to determine the following:

a. If changes in physical data of a constituent material from time of manufacture to the time of incorporation into the propellant affect the pressures obtained.

b. If changes in sources of supply of constituent materials affect pressures obtained.

c. If changes in process conditions affect pressures obtained.

Recommendations

Based on the preliminary results obtained, it is recommended that the study be continued to:

a. Evaluate those parameters which appear to cause pressure increase.

b. Determine if the following factors affect the pressure observed:

1. Aging /storage conditions of constituent materials.
2. Changes in source of supply of constituent materials.
3. Changes in propellant processing conditions.

References

N.R. Draper, H. Smith, "Applied Regression Analysis". Wiley

Table 1:
Summary of the dependent variables used in the plotting:
Explanation

		<u>Fired at -65°F</u>	<u>Fired at 70°F</u>	<u>Fired at 145°F</u>	
1.	Pressure -65				(Pressure 145°F minus Pressure -65°F)/(210 x 100)
2.	Pressure 70				(Pressure 145°F minus Pressure 70°F)/(75 x 100)
3.	Pressure 145				(Pressure 70°F minus Pressure -65°F)/(135 x 100)
4.	DP/DT ₁ . (-65 -145) °F				Relative Quickness 90°F minus Relative Quickness -40°F
5.	DP/DT ₂ (70 -145) °F				Relative Force 90°F minus Relative Force -40°F
6.	DP/DT ₃ (-65 -70) °F				Test RD (Pressure 145°F minus Pressure -65°F) CALI RD (Pressure 145°F minus Pressure -65°F)
7.	RQ90 -(RQ-40)				
8.	RF90 -(RF-40)				
9.	$\frac{DP(\text{TEST})}{DP(\text{CALI})}/DT_1$ (-65 -145) °F				
10.	$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_2$ (70 - 145) °F				
	DP (CALI)				

Table 2
Summary of Independent Variables Used In The Plotting

	<u>Short Title Used in The Plots</u>
1. % Nitrogen	(Nitrocellulose)
2. Fineness	()
3. % Ash	()
4. Viscosity	()
5. Freeness	()
6. % Water	(Nitroglycerine)
7. % Nitrogen	()
8. Average Particle size	(Nitroguanidine)
9. % Ash	()
10. pH Value	(pH (NGU))
11. Total Volatiles	()
12. % Sulfates	()
13. Solidification point °C	(Ethyl Centralyte)

14. Volatile Content	(-)	V.C. (ETH)
15. % Ash Content	(-)	
16. Sum of Amines	(-)	
17. % Moisture	(Potassium Sulfate)			Mois (PS)
18. % Moisture	(Graphite, Grade 4)			
19. % Ash	(-)	% Ash (G4)
20. Granulation	(-)	
21. Nitrocellulose	(% Composition)			
22. Nitroglycerine	(-)	
23. Nitroguanidine	(-)	
24. Ethyl Centralite	(-)	E.C. (AC)
25. Potassium Sulfate	(% Composition)			
26. Total Volatiles	(% Composition)			T.V. (AC)

27. Graphite, Grade 4 G4 (TC)
28. Length (Grain Dimensions)
29. Diameter ()
30. Perforation ()
31. Inner Web ()
32. Outer Web ()
33. Avg Web ()
34. Web Difference ()
35. L/D ()
36. L/d ()
37. L Uniformity ()
38. D Uniformity ()
39. Year Storage of Nitroguandine Yr (STORAGE) NGU

Table 3:
Result of plots with strong trends
and slight trends

Independent Variable	pH Value (Nitroguanidine)	% Moisture (Potassium Sulfite)	% Ash (Graphite)	Volatile Content (Ethyl Centralite)	% Nitrogen (Nitrocellulose)	Viscosity (Nitrocellulose)	Freeness (Nitrocellulose)	Total Volatile (% Comp)	Ethyl Centralite (% Comp)	Graphite (% Comp)	Nitroglycerine (Comp)	Length of Grain	Perforation Diameter D/d	Length Uniformity of Grain	Diameter Uniformity of Grain	Year Storage of Nitroguanidine
Pressure 70																
Pressure -65																
Pressure 145																
DP/DT ₃ - (-65-70) ^o P																
DP/DT ₂ - (70-145) ^o P																
DP/DT ₁ - (-65-145) ^o P																
RF 90 - (RF-40)																
RP 90 - (RP-40)																
DP (TEST) - (-65-145) ^o P																
DP (CALC) - (70-145) ^o P																

S = Strong trend
W = Slight trend

Appendix 1: Evaluation of Computer Graph Output

As previously mentioned all plots were generated by a computer program. A title and a table of data appear on every plots. The values listed at the left side of the table are the values of the independent variable and were plotted on the X coordinate; likewise, the values at the right side are belonged to the dependent variable and were designated on Y coordinate. These pairs of X,Y values are arranged in a chronological order. A symbol \times on the plot is an indication of the first pair of X, Y value being plotted. The rest of data was then plotted and connected by the lines in a chronological order.

Types of trends observed from the plots are summarized below.

A. Summary of The Strong Trend Plots

<u>Fig #</u>	<u>Independent Variable</u>	<u>Vs.</u>	<u>Dependent Variable</u>
1	pH Value (Nitroguanidine)		Pressure at 145°F
2	Total Volatile (% Composition)		Pressure at 145°F
3	% Ethyl Centralite (% Composition)		Pressure at 145°F
4-7	% Moisture (Potassium Sulfate)		$\frac{DP}{DT_2} (70 - 145)^\circ F$
8-11	Total Volatile (% Composition)		$\frac{DP \text{ TEST}}{DP \text{ CALI}} / DT_2 (70 - 145)^\circ F$
			$\frac{DP \text{ TEST}}{DP \text{ CALI}} / DT_1 (-65 - 145)^\circ F$
			RQ90 - (RQ -40)
12-16	% Graphite (% Composition)		$\frac{DP}{DT_1} (-65 - 145)^\circ F$
17-21	% ASH (in Graphite)		$\frac{DP}{DT_2} (70 - 145)^\circ F$
			$\frac{DP \text{ (TEST)}}{DP \text{ (CALI)}} / DT_1 (70 - 145)^\circ F$
			$\frac{DP \text{ (TEST)}}{DP \text{ (CALI)}} / DT_2 (-65 - 145)^\circ F$
			RQ90 - (RQ -40)
22-24	Yr (Storage) Nitroguanidine		$\frac{DP}{DT_2} (70 - 145)^\circ F$
			$\frac{DP \text{ TEST}}{DP \text{ CALI}} / DT_2 (70 - 145)^\circ F$
			$\frac{DP \text{ TEST}}{DP \text{ CALI}} / DT_1 (-65 - 145)^\circ F$

PRESSURE VS. PH VALUE
C034

TEMP. = 145.

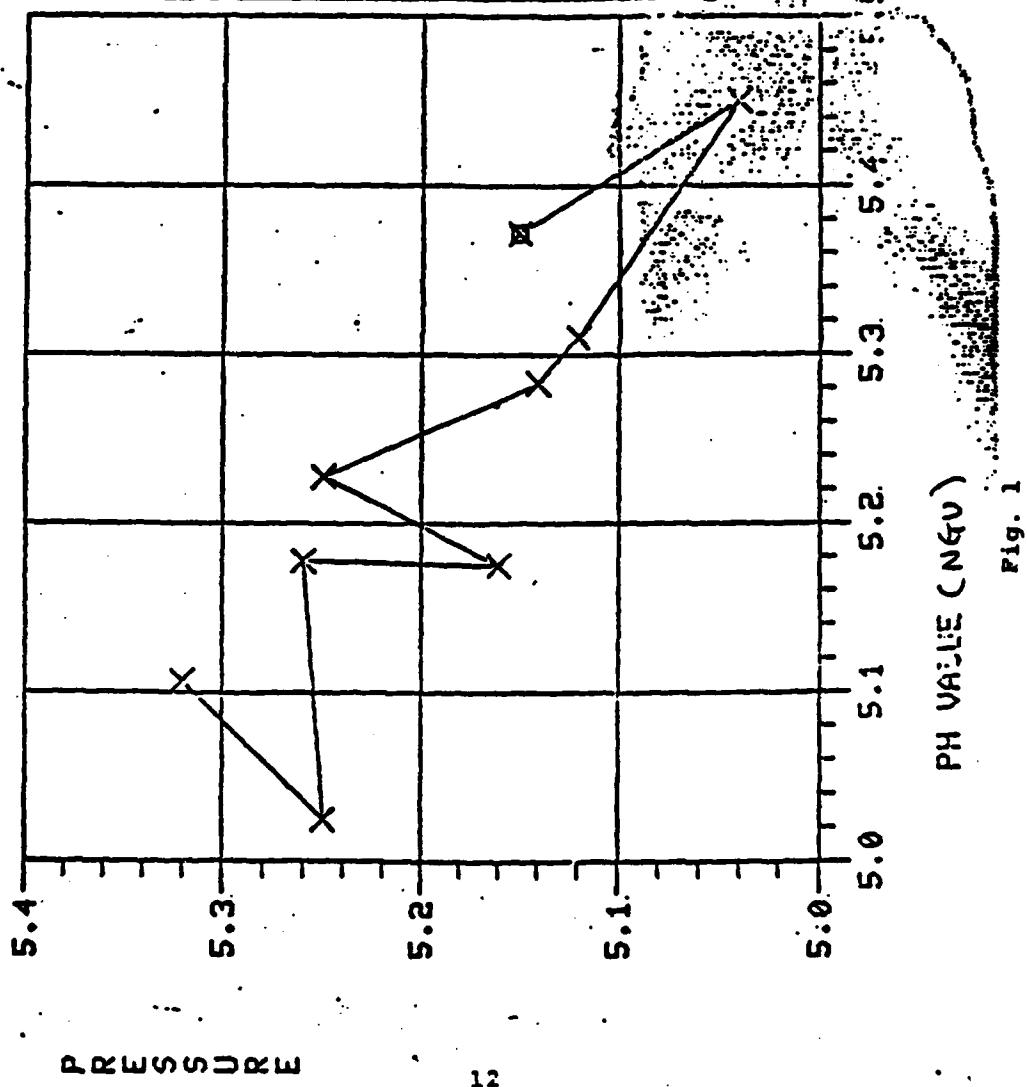


Fig. 1

TEMP = 145.

PRESSURE VS. TOTAL VOLATILES ,C106

DATA
3300,
3400,
2500,
1800,
6700,
1800,
0300,
1200,
1500,
0515
0504
0512
0514
0525
0526
0516
0525

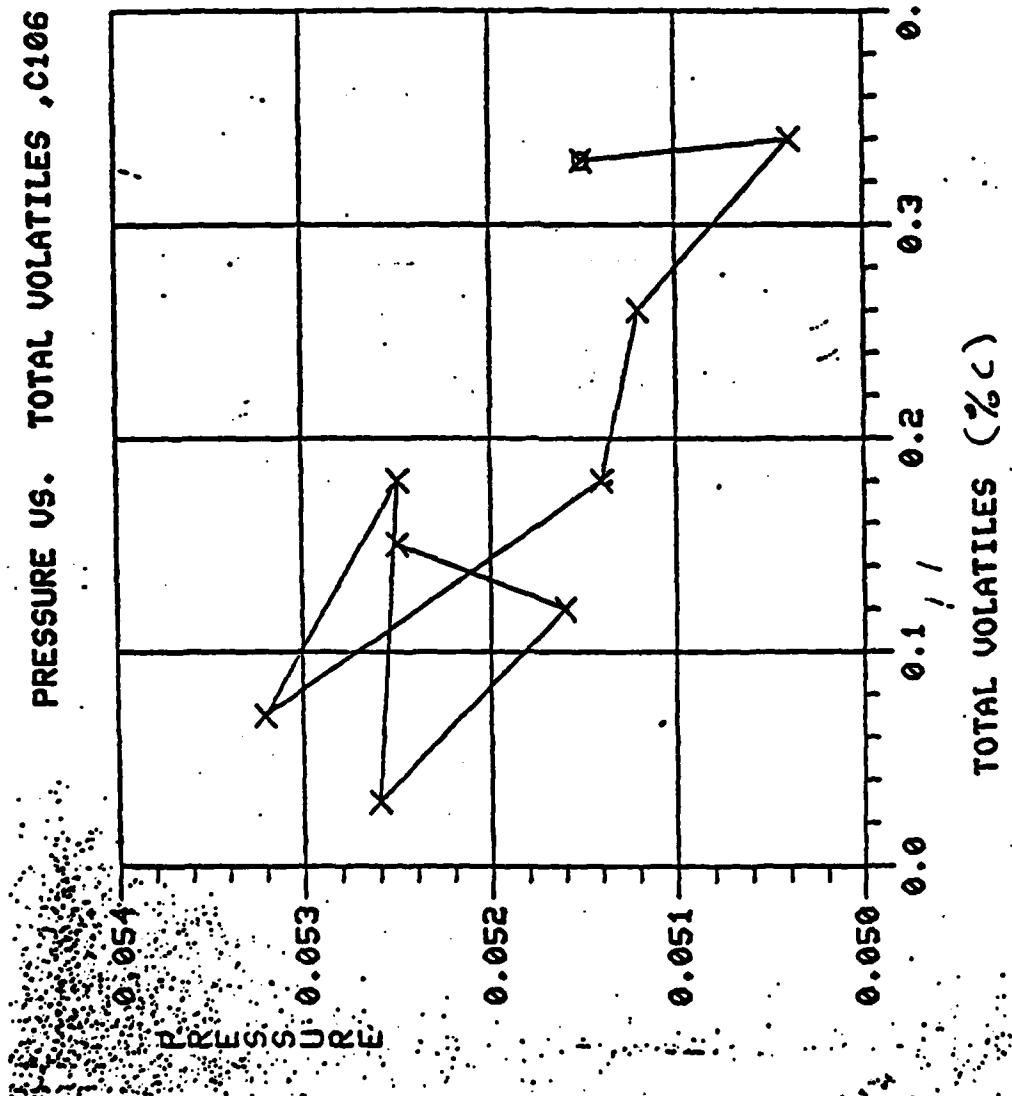


FIG. 2

PRESSURE VS. ETHYL CENTRAL ,C104 TEMP = 145.

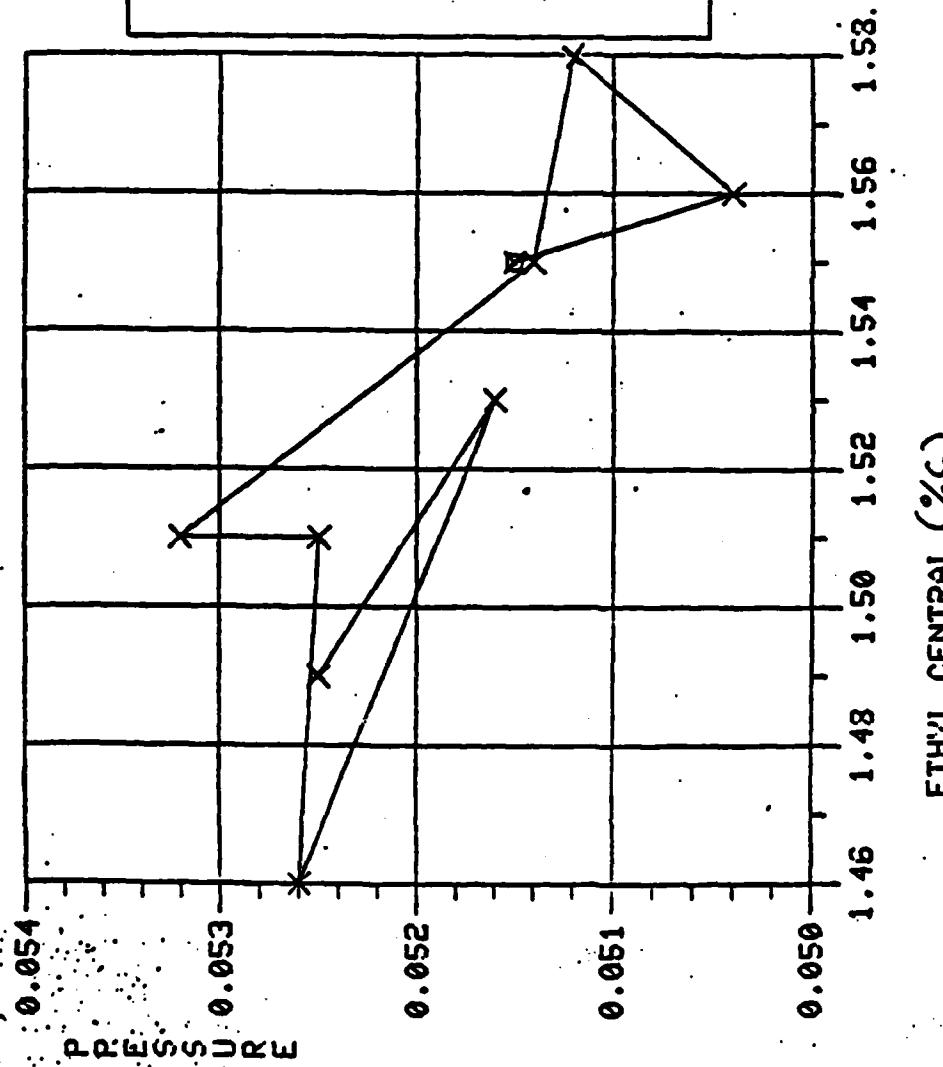


Fig. 3.

C051

PRESSURE COEFFICIENT, DP/DT VS. % MOISTURE :

TEMP. RANGE IS (70.-145)°F

PRESSURE COEFFICIENT DP/DT

DATA

.0100,	.8533
.0050,	.6533
.0075,	.6800
.0200,	.2267
.0200,	1.1600
.0150,	.9733
.0100,	.0400
.0100,	.0800
.0200,	1.2133

% MOISTURE (PS)

Fig. 4

0.020
0.015
0.010
0.005
0.6
0.8
1.0

$DP(RAD-T)/DP(RAD-C)_{145-70}$ vs MOIS(PS)

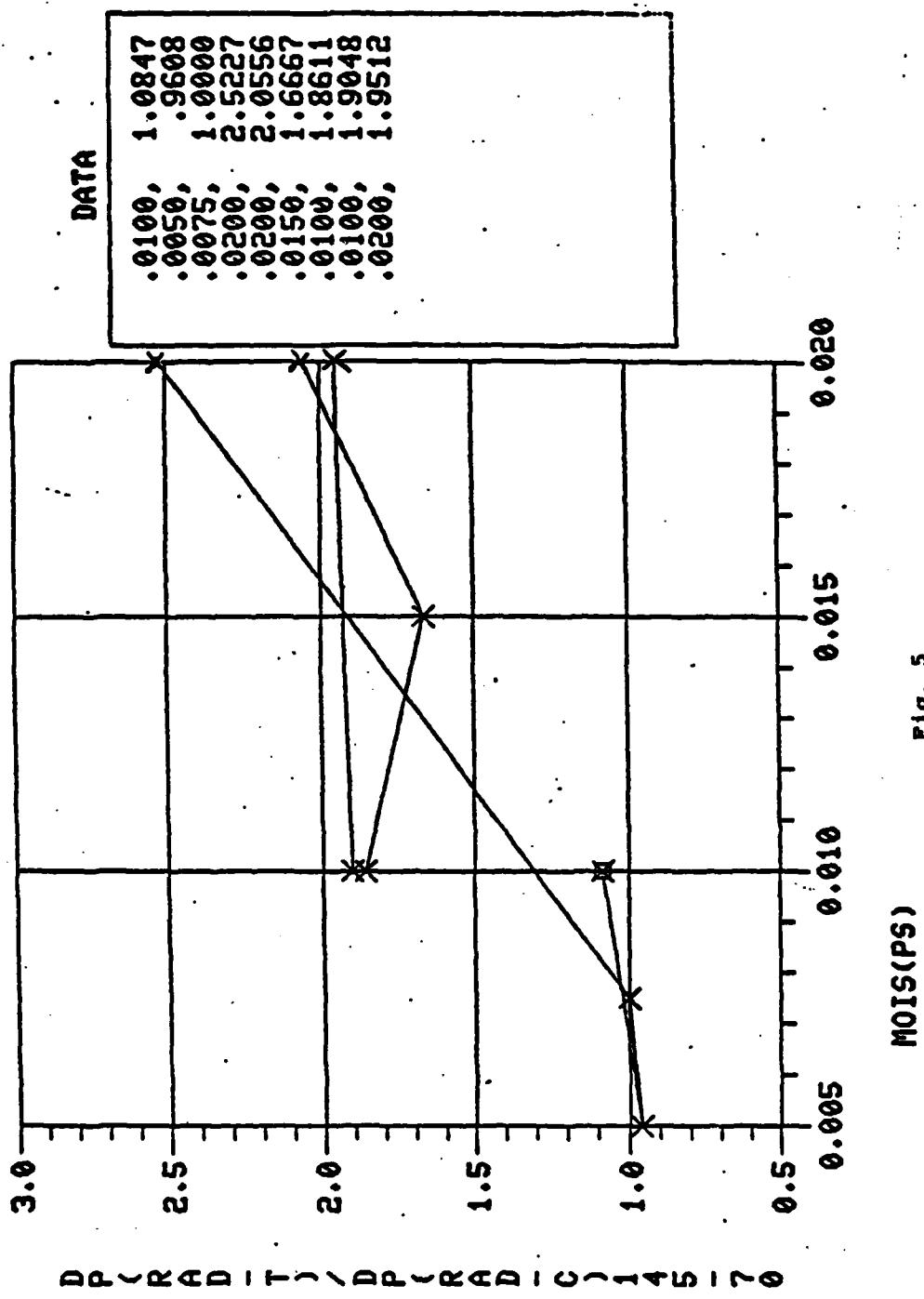


Fig. 5

DP(RAD-T)/DP(RAD-C)145--65 USMOIS(PS)

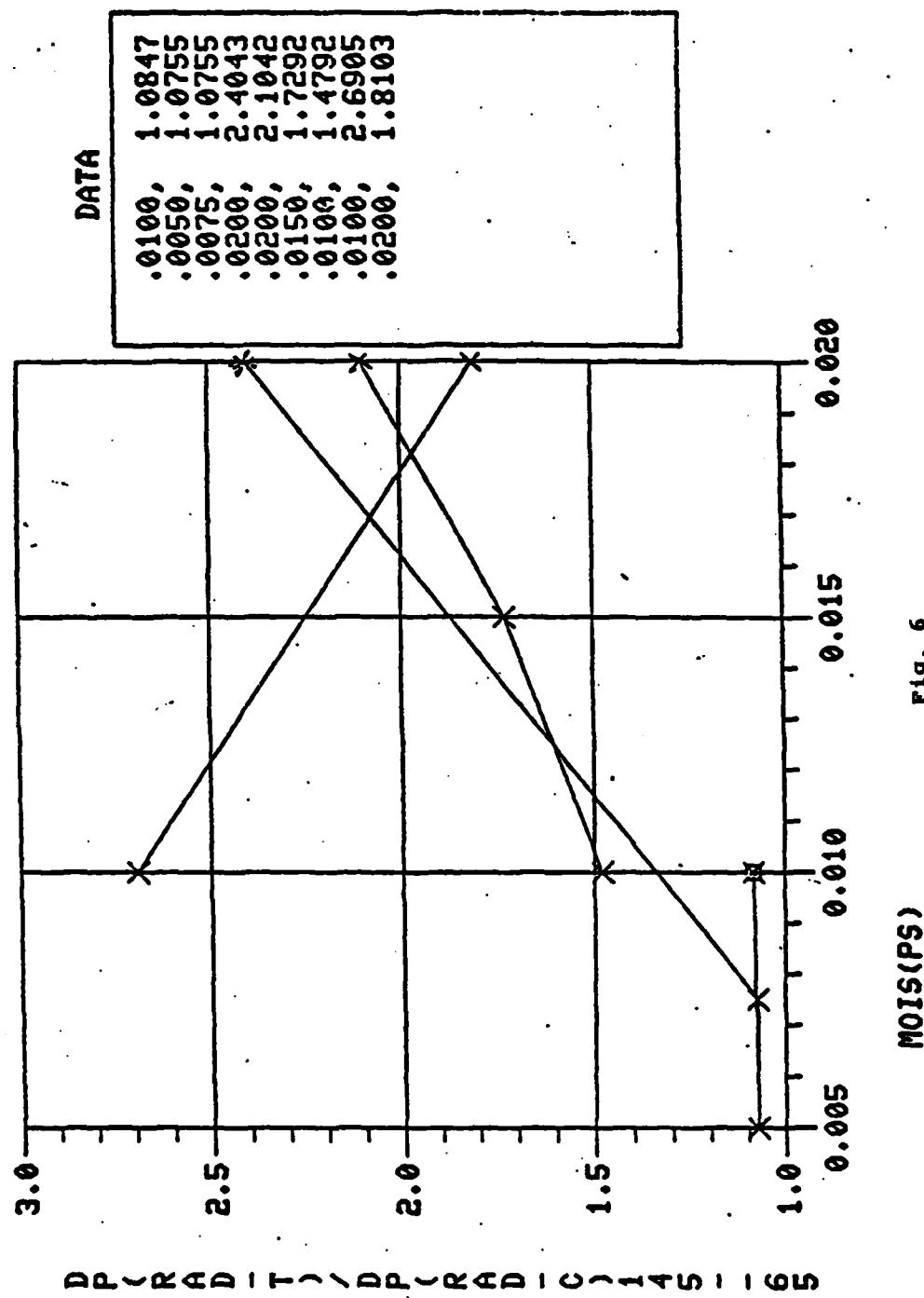
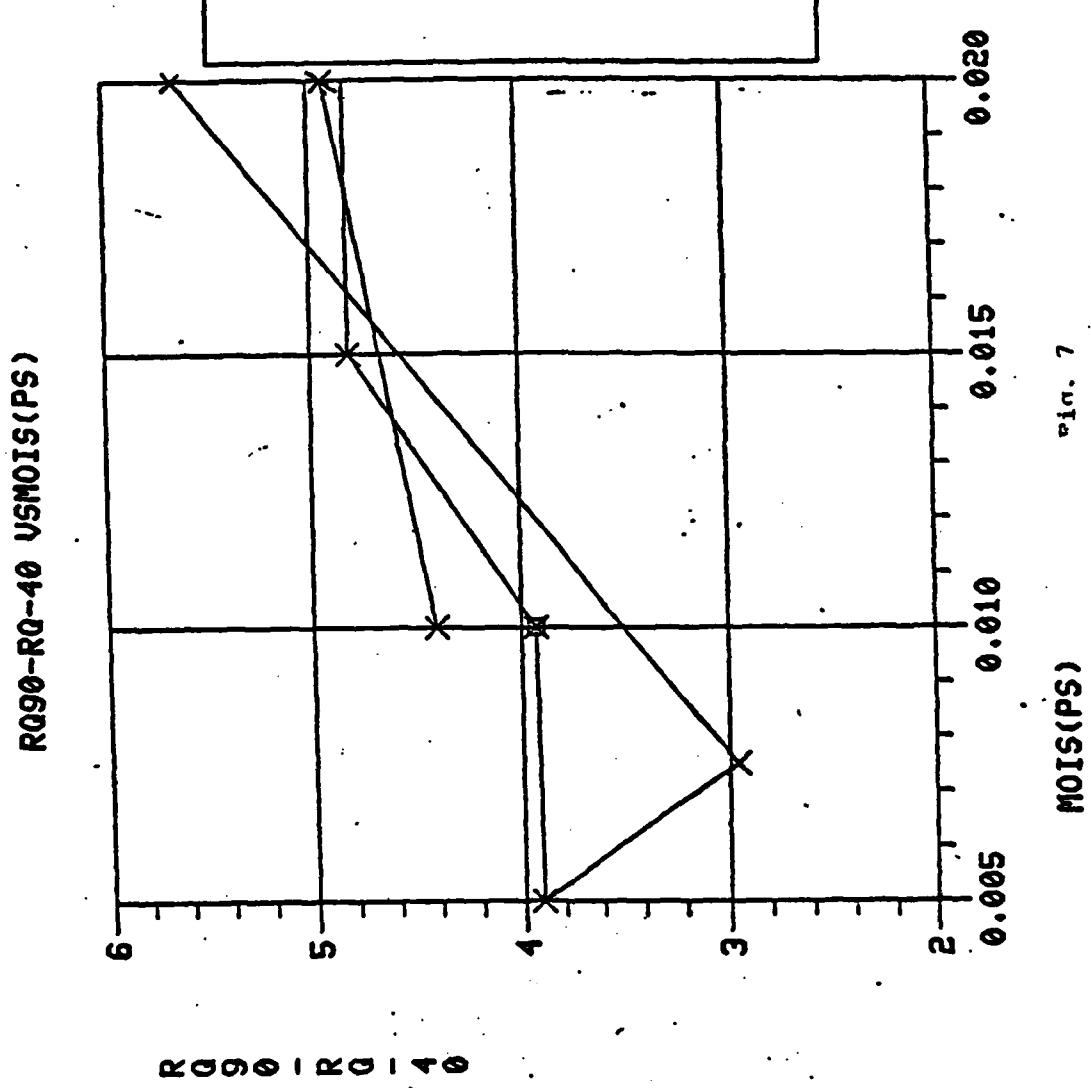


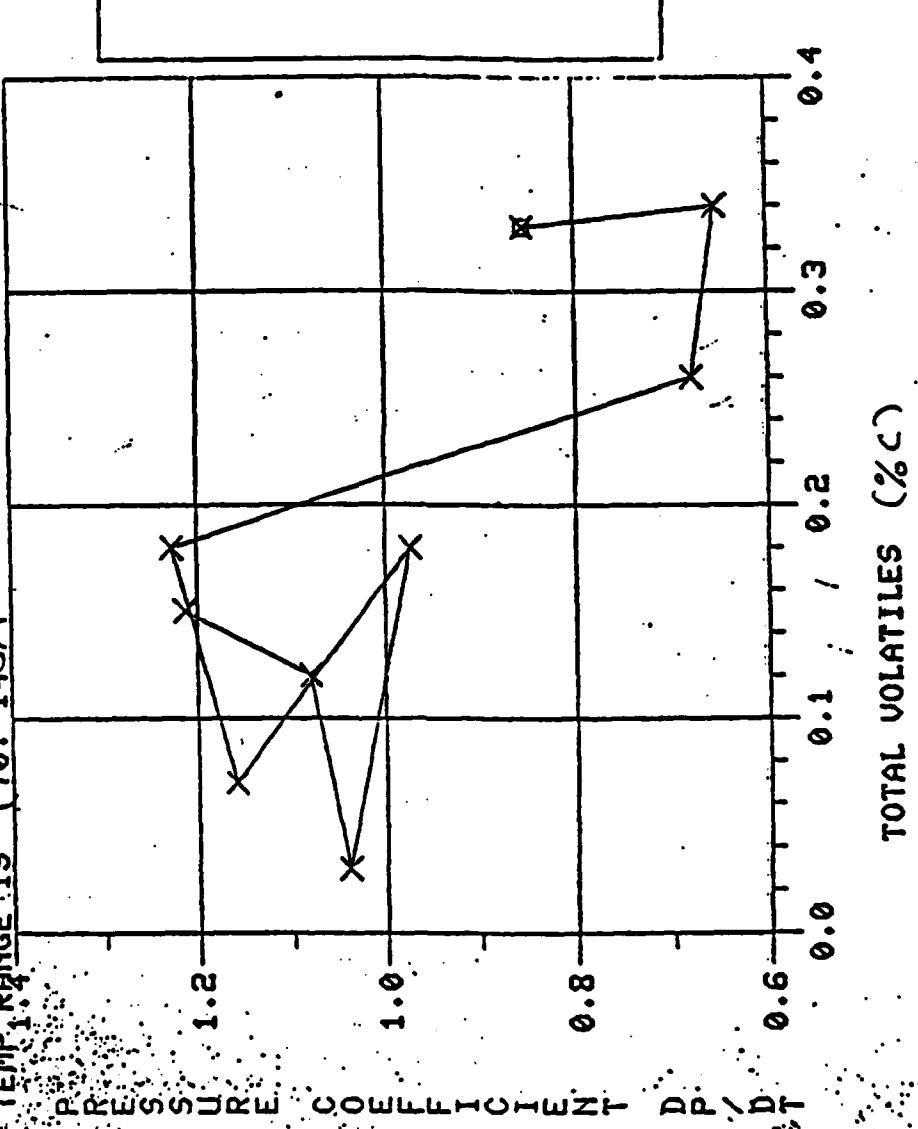
Fig. 6



RC001 RC140

PRESSURE COEFFICIENT, DP/DT VS. TOTAL VOLATILES ,C106

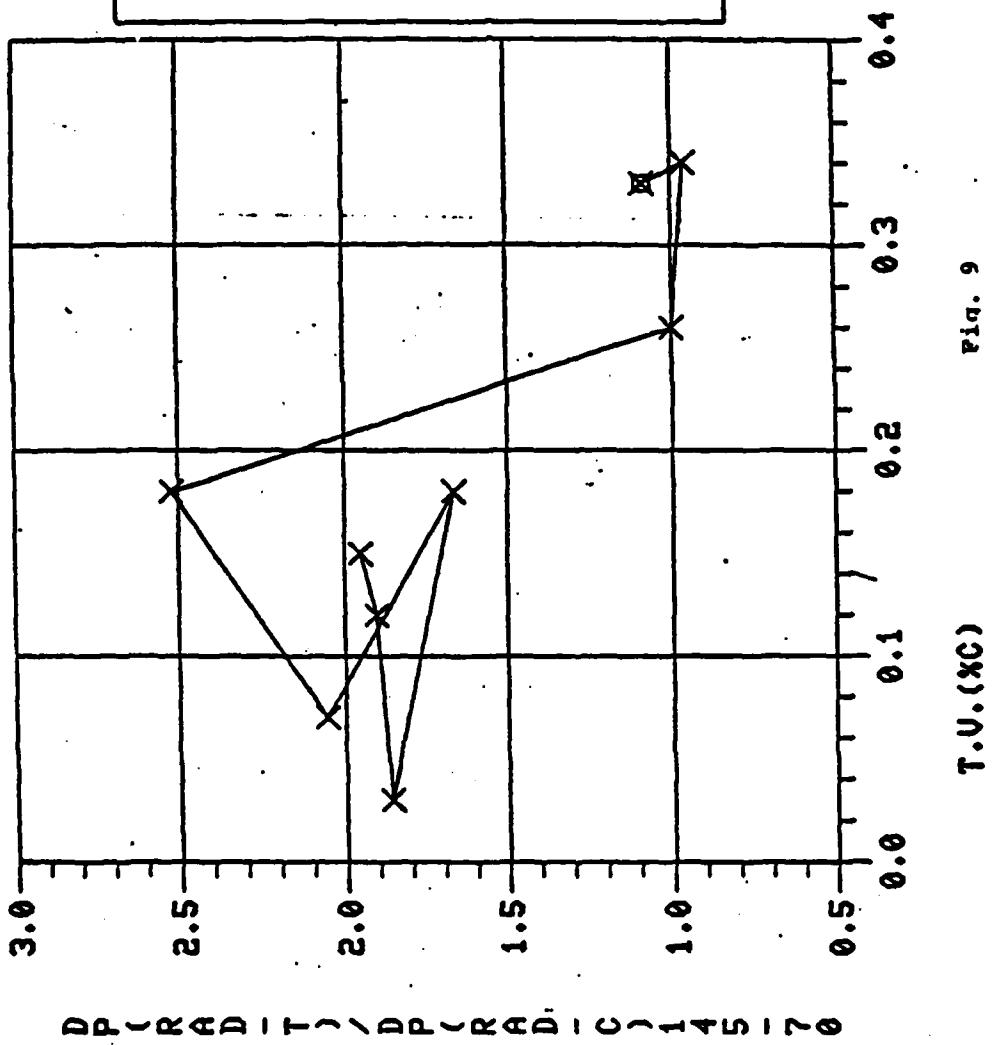
TEMP. RANGE IS $(70.-145)^\circ\text{F}$



DATA	
3300,	8533
3400,	6533
2600,	6800
1800,	1.2267
0700,	1.1693
0700,	1.1693
1800,	1.9733
0500,	1.0700
1200,	1.0800
1500,	1.2133

Fig. 9

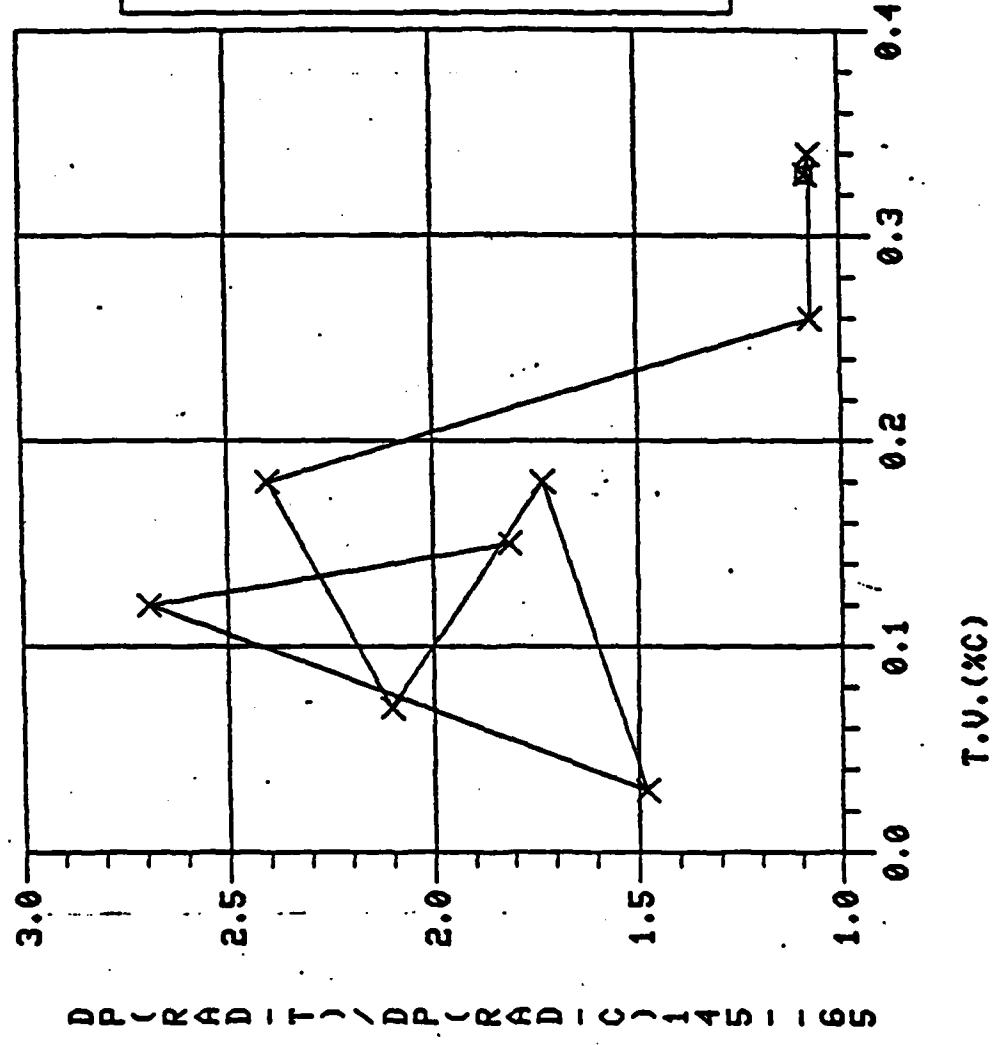
DP(RAD-T)/DP(RAD-C)145-70 VS T.U.(XC)



DP(RAD-T)/DP(RAD-C)145-70

Fig. 9

DP(RAD-T)/DP(RAD-C)145--65 UST.V.(%)

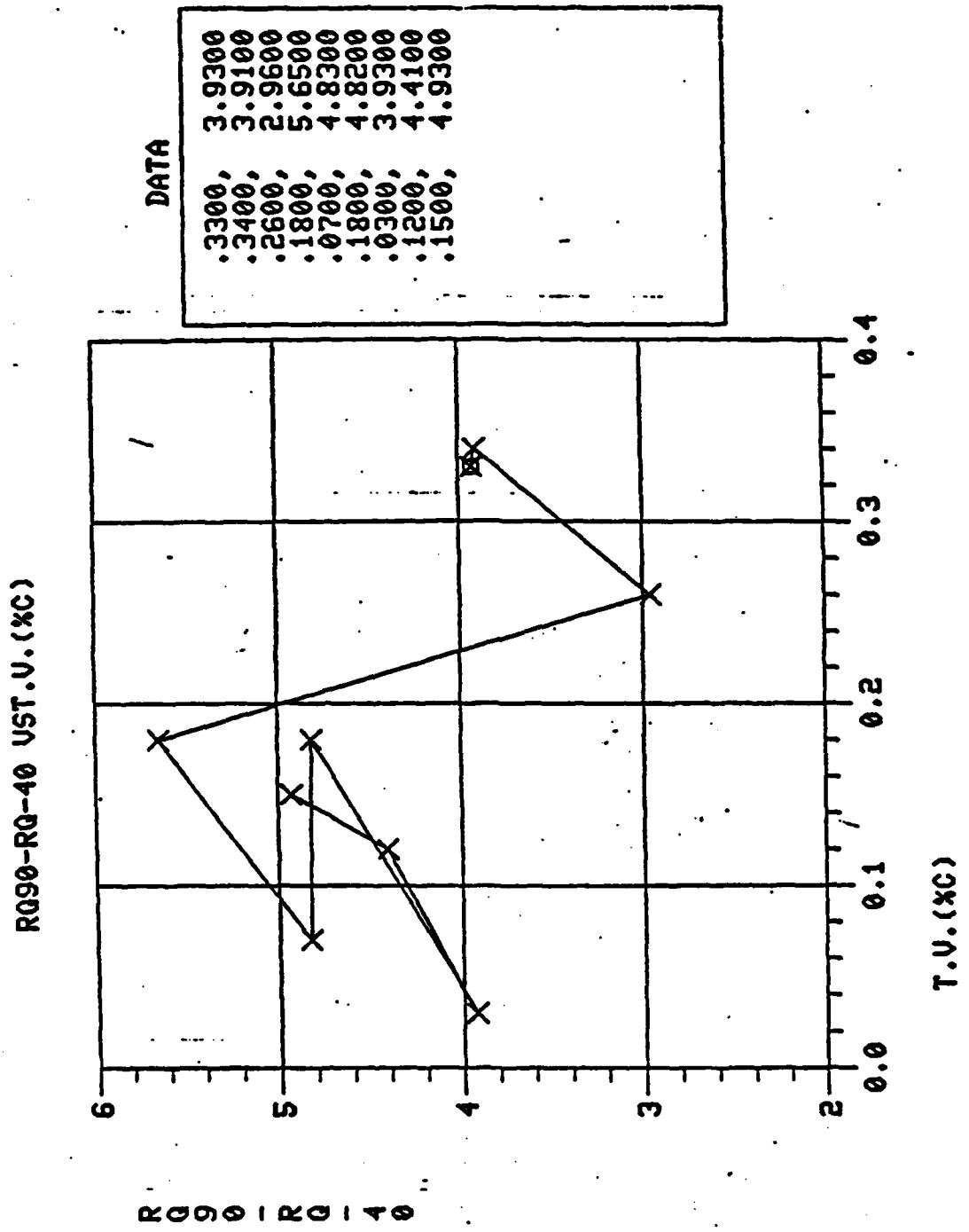


DP(RAD-T)/DP(RAD-C)145--65

DATA

.3300,	1.0847
.3400,	1.0755
.2600,	1.0755
.1800,	2.4043
.0700,	2.1042
.1800,	1.7292
.0300,	1.4792
.1200,	2.6905
.1500,	1.8103

Fig. 16



RQ90-RQ-40 UST.U. (xc)

C107

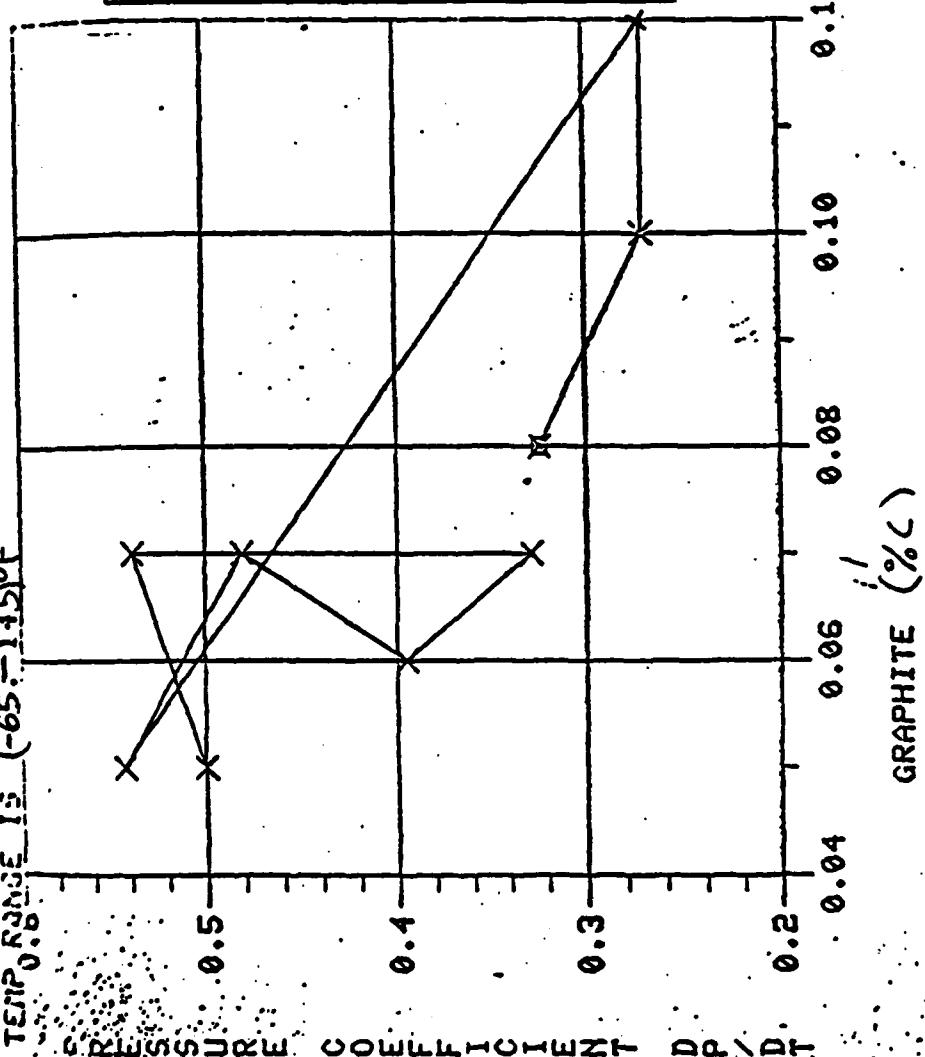
PRESSURE COEFFICIENT, DP/DT VS. GRAPHITE

TEMP RANGE IS (-65 - 145)°F

COMPOSITION COEFFICIENT DP/DT

DATA

.0800,	.3238
.1000,	.2714
.1200,	.5429
.1500,	.4810
.1700,	.3952
.2000,	.3286
.2500,	.5381
.3000,	.5000



PRESSURE COEFFICIENT, DP/DT VS. GRAPHITE
C107

TEMP RANGE IS (70.-145)°F
PRESSURE COEFFICIENT DP/DT

DATA

• 0800,	• 8533
• 1000,	• 6533
• 1200,	• 6267
• 1500,	• 1.2267
• 1750,	• 1.1667
• 2000,	• 1.1667
• 2500,	• 0.9733
• 3000,	• 1.0467
• 3500,	• 1.0867
• 4000,	• 1.2133

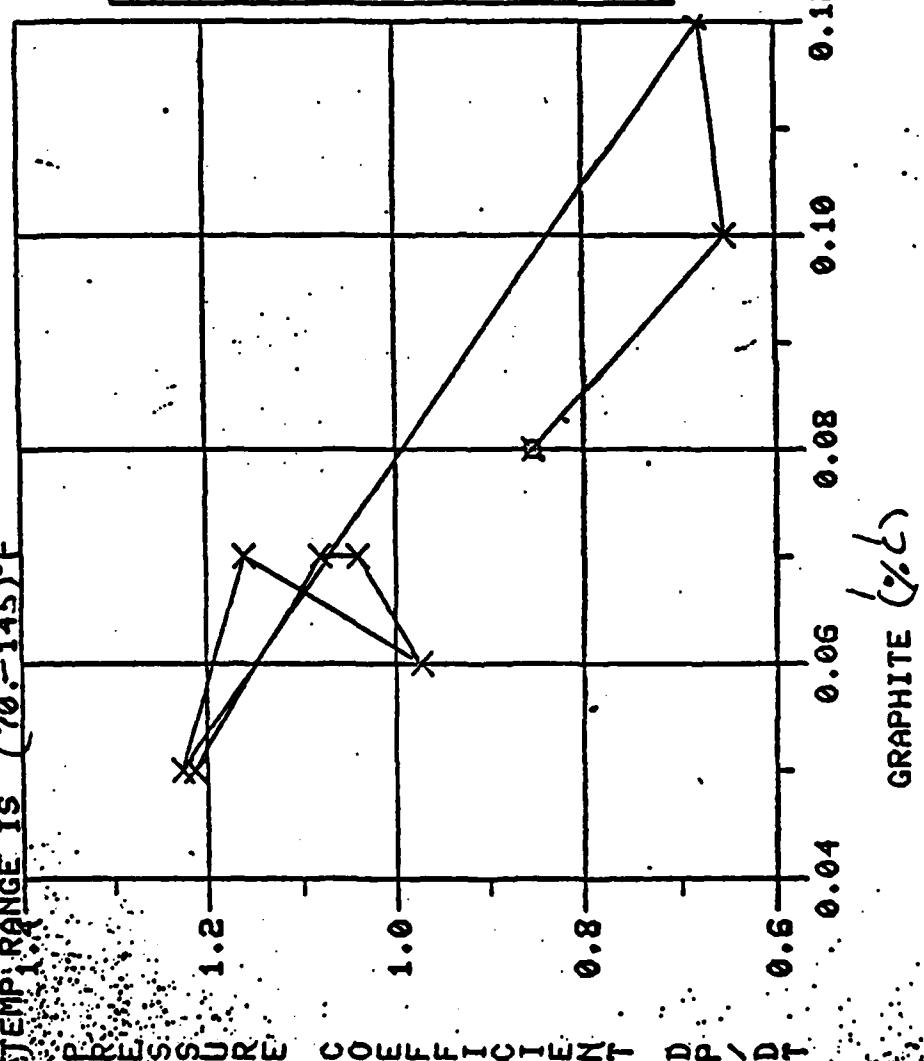


Fig. 13

$\frac{DP(\text{RAD-T})}{DP(\text{RAD-C})} \sim 145 - 70$ VS $G4(\text{KC})$

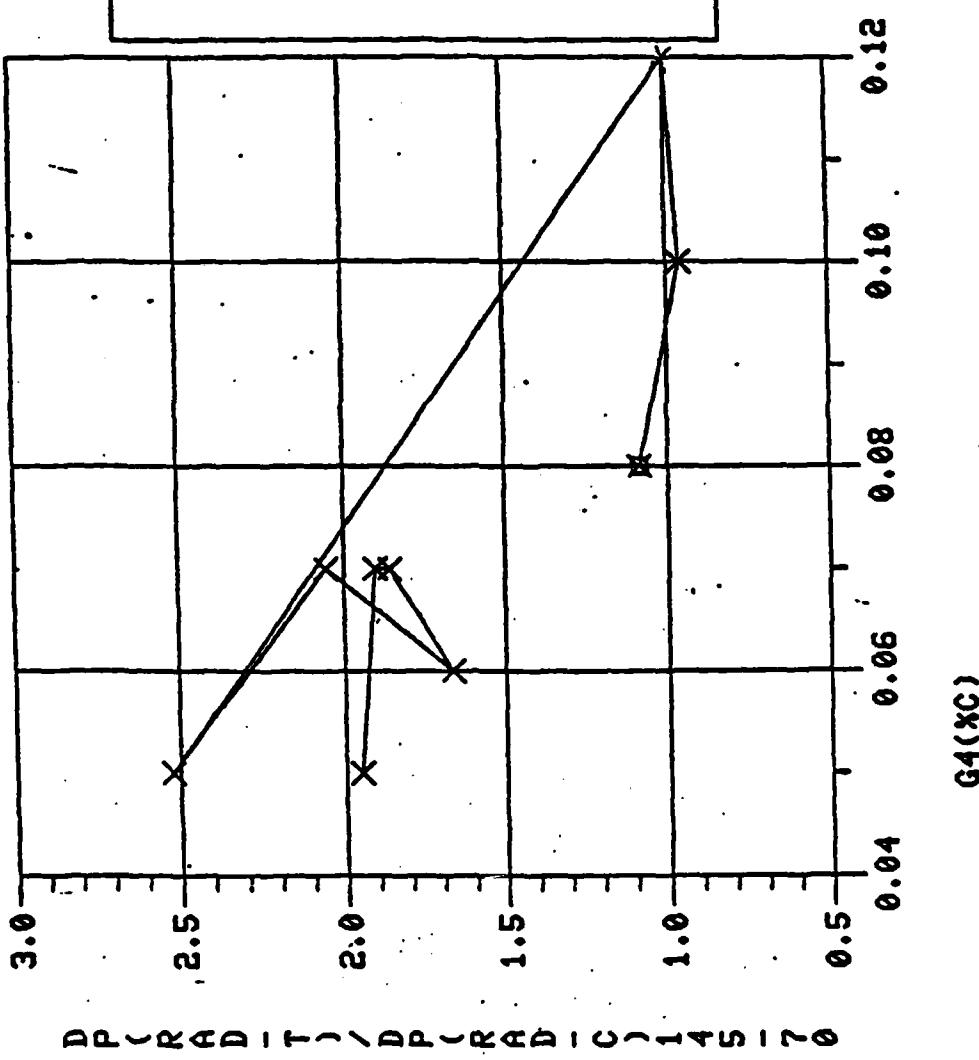


Fig. 14

$D_P(RAD-T)/D_P(RAD-C) \sim 145 \sim -65$ USG4(χ_C)

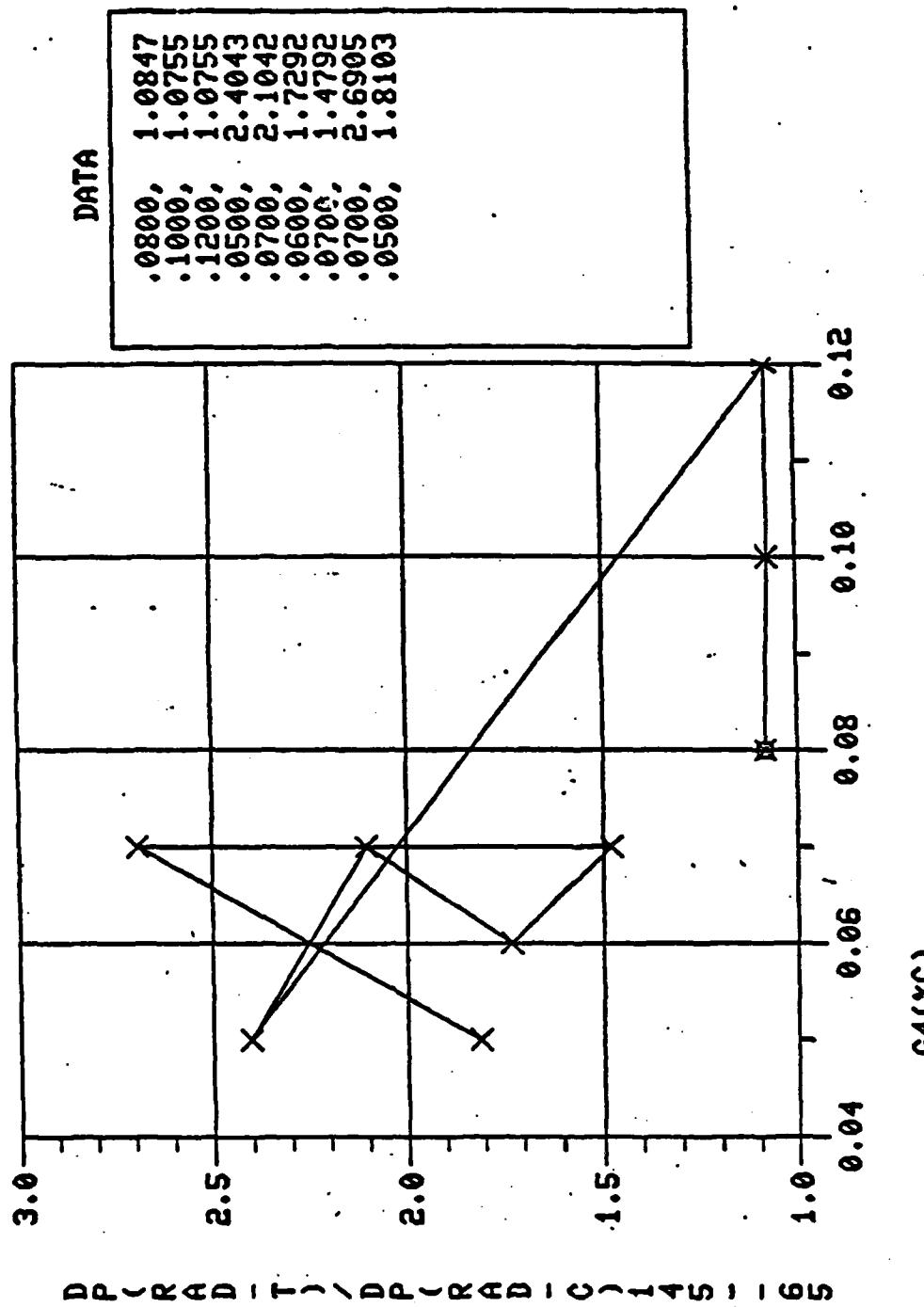
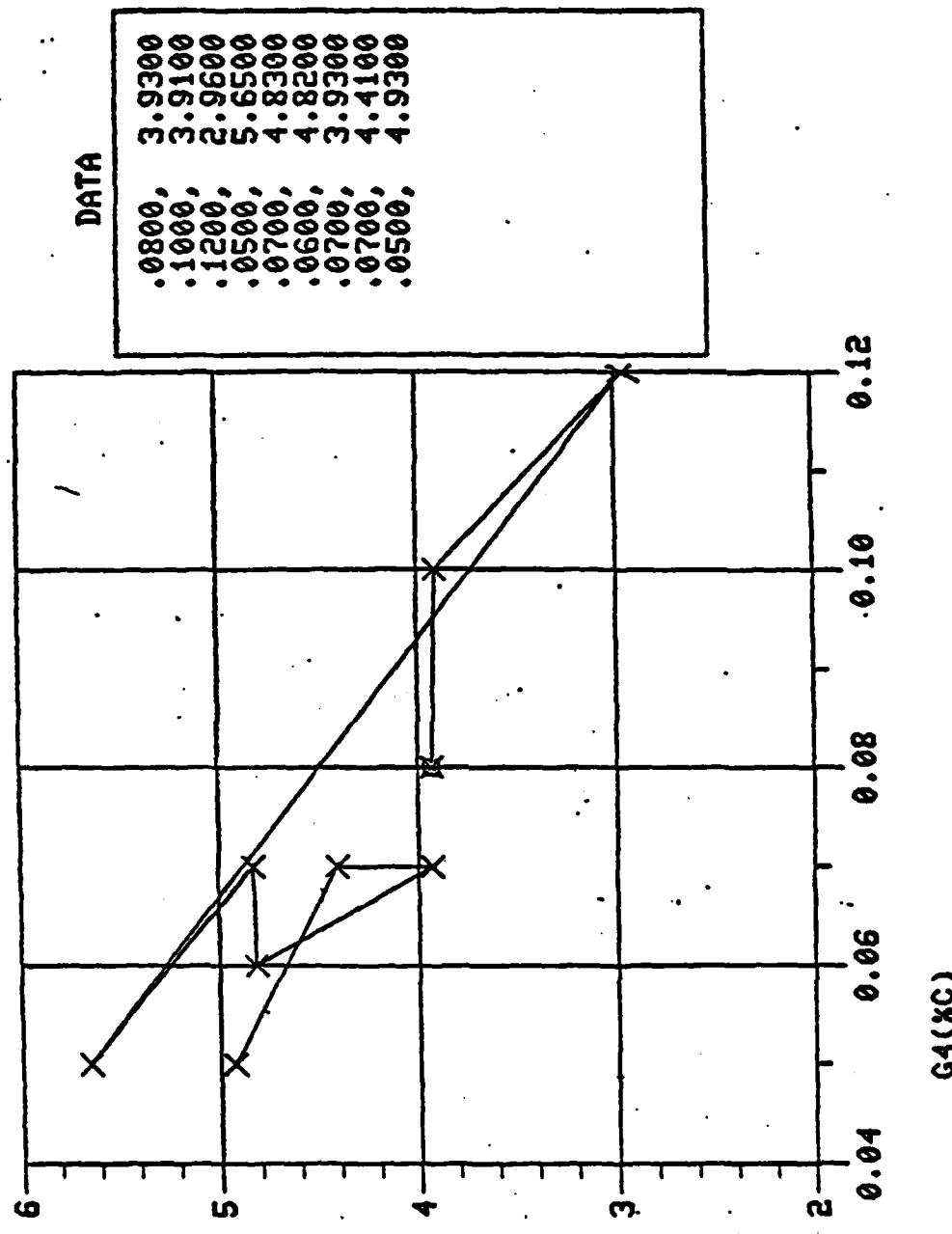


Fig. 15

R090-R0-40 USG4(XC)



R090-R0-40

,C062

PRESSURE COEFFICIENT, D_P/D_T VS. % ASH
TEMP. RANGE IS (-65 TO 145)°F

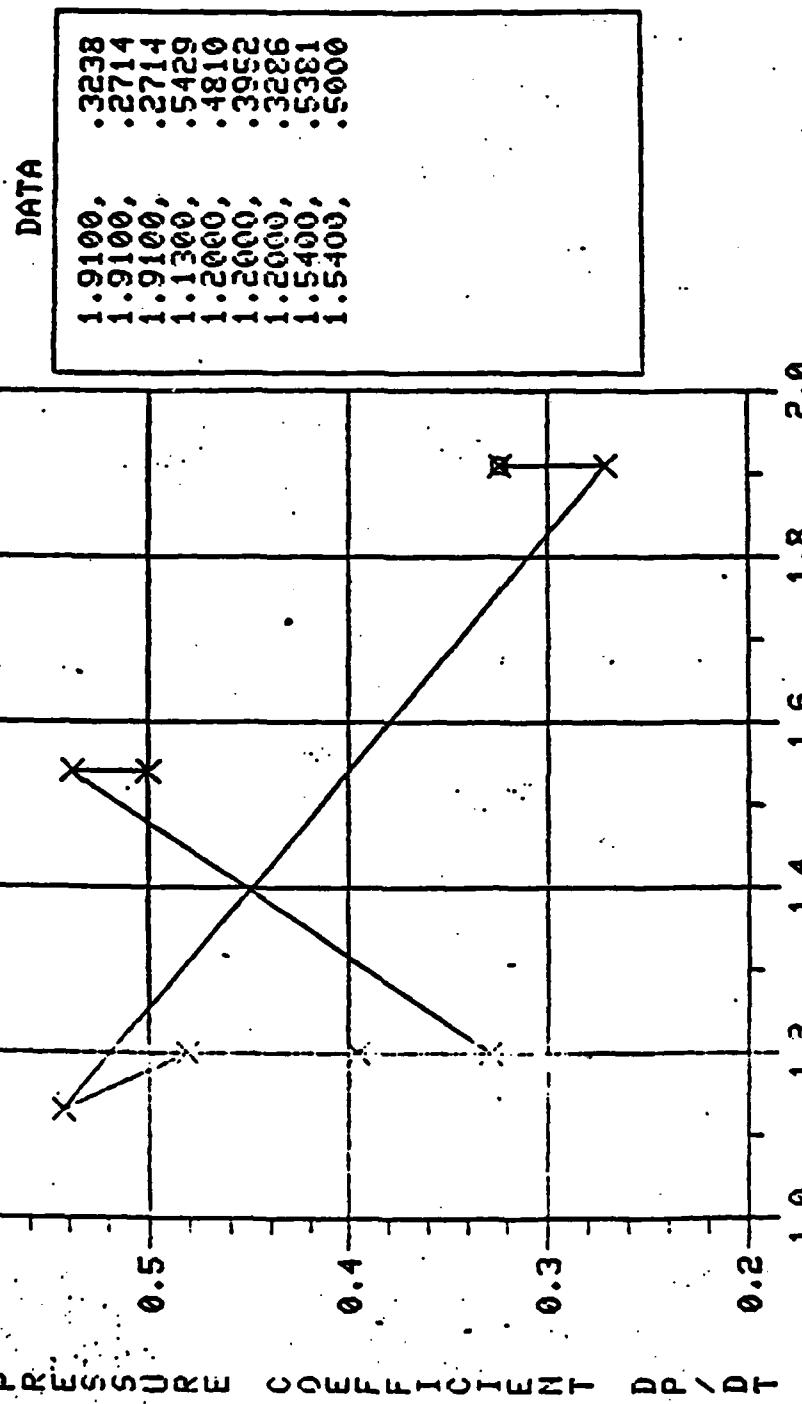


Fig. 17.

C0662

PRESSURE COEFFICIENT, DP/DT VS. % ASH

TEMP RANGE IS $(70 - 145)^\circ\text{F}$

PRESSURE COEFFICIENT DP / DT

DATA

1.9100	.8533
1.9100	.6533
1.9100	.6800
1.1300	1.2267
1.2000	1.1603
1.2000	.99733
1.2000	.0499
1.5400	.0399
1.5400	1.2133

% ASH (G4)

Fig. 18

$D_P(RAD-T)/D_P(RAD-C) 145-65$ VS $XASH(G4)$

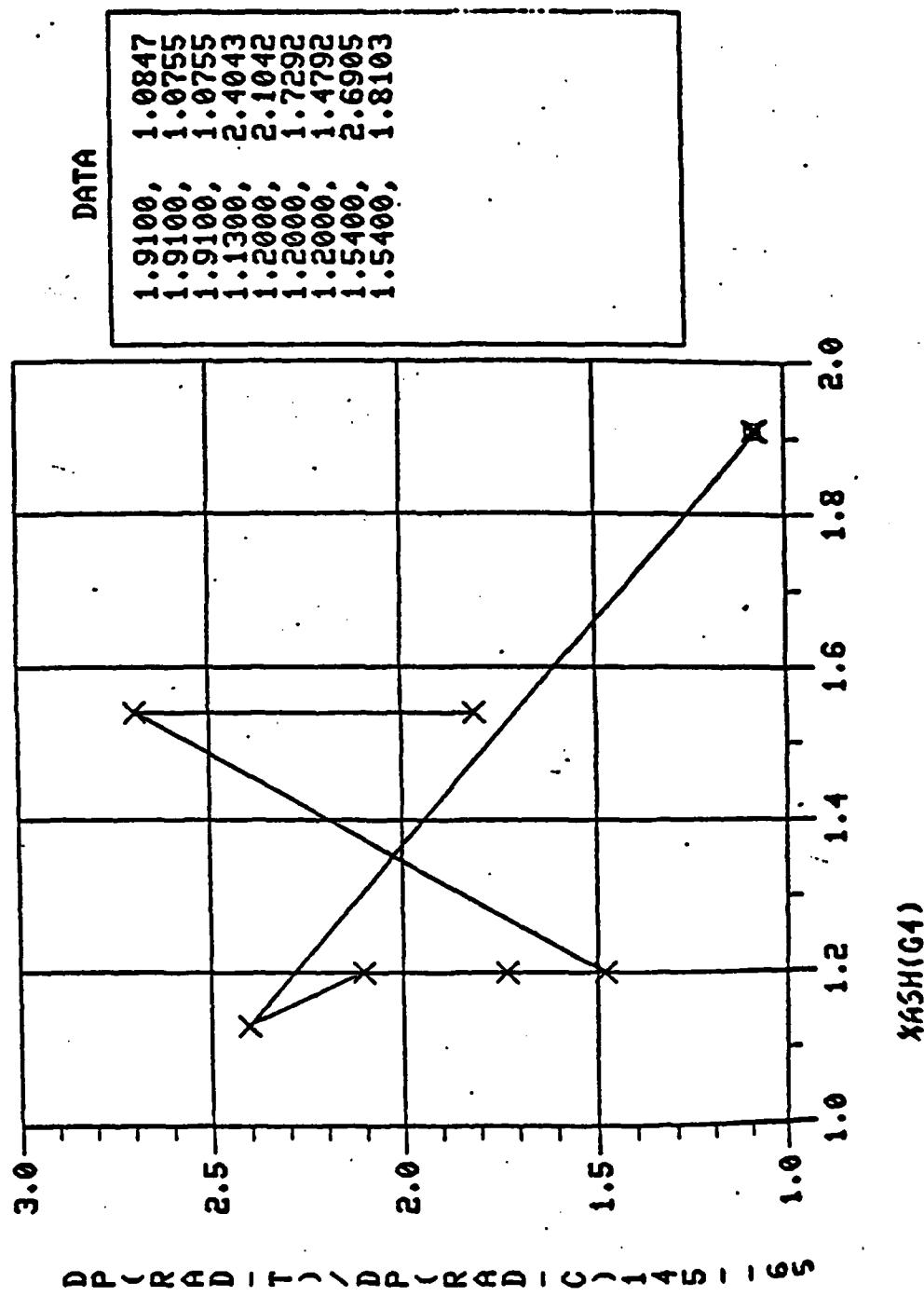


Fig. 19

$DP(RAD-T)/DP(RAD-C)_{145-70}$ VS $XASH(G4)$

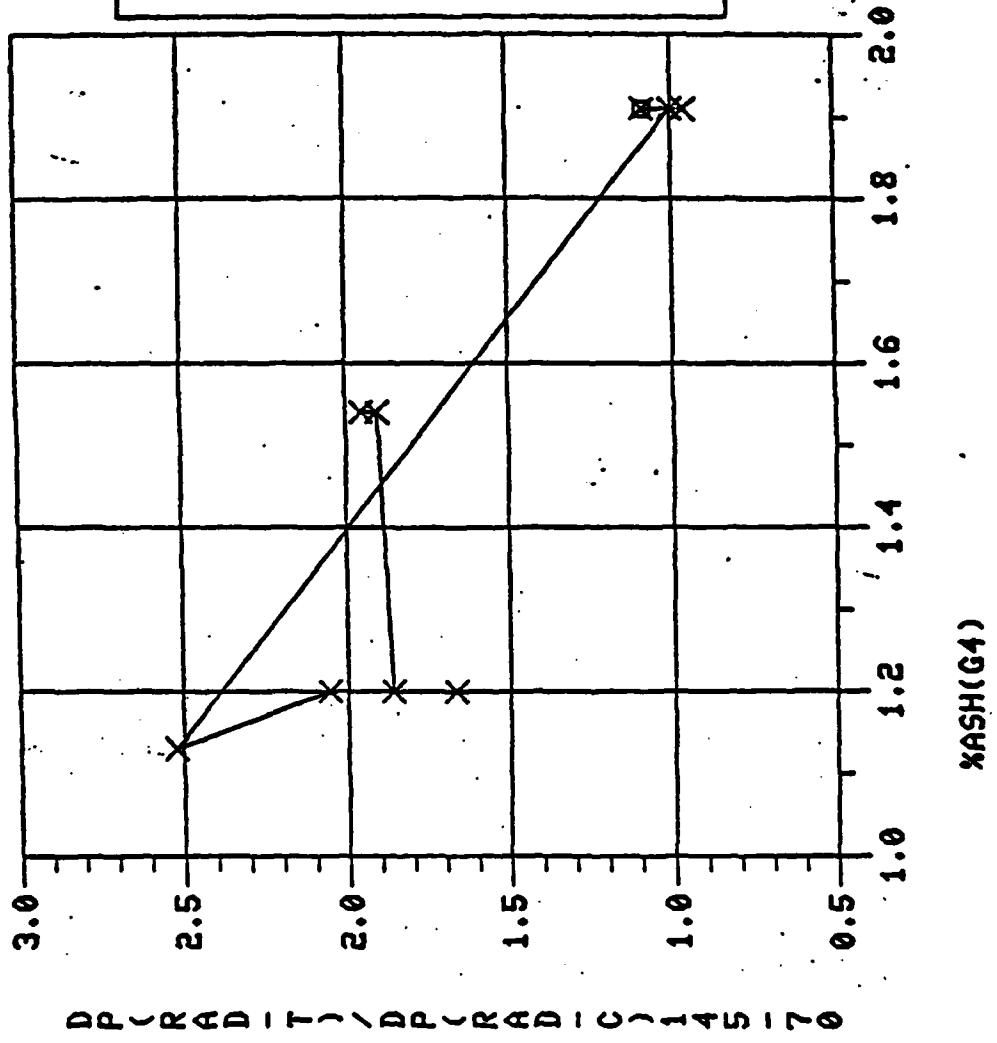


Fig. 23

RQ90-RQ-40 USKASH(G4)

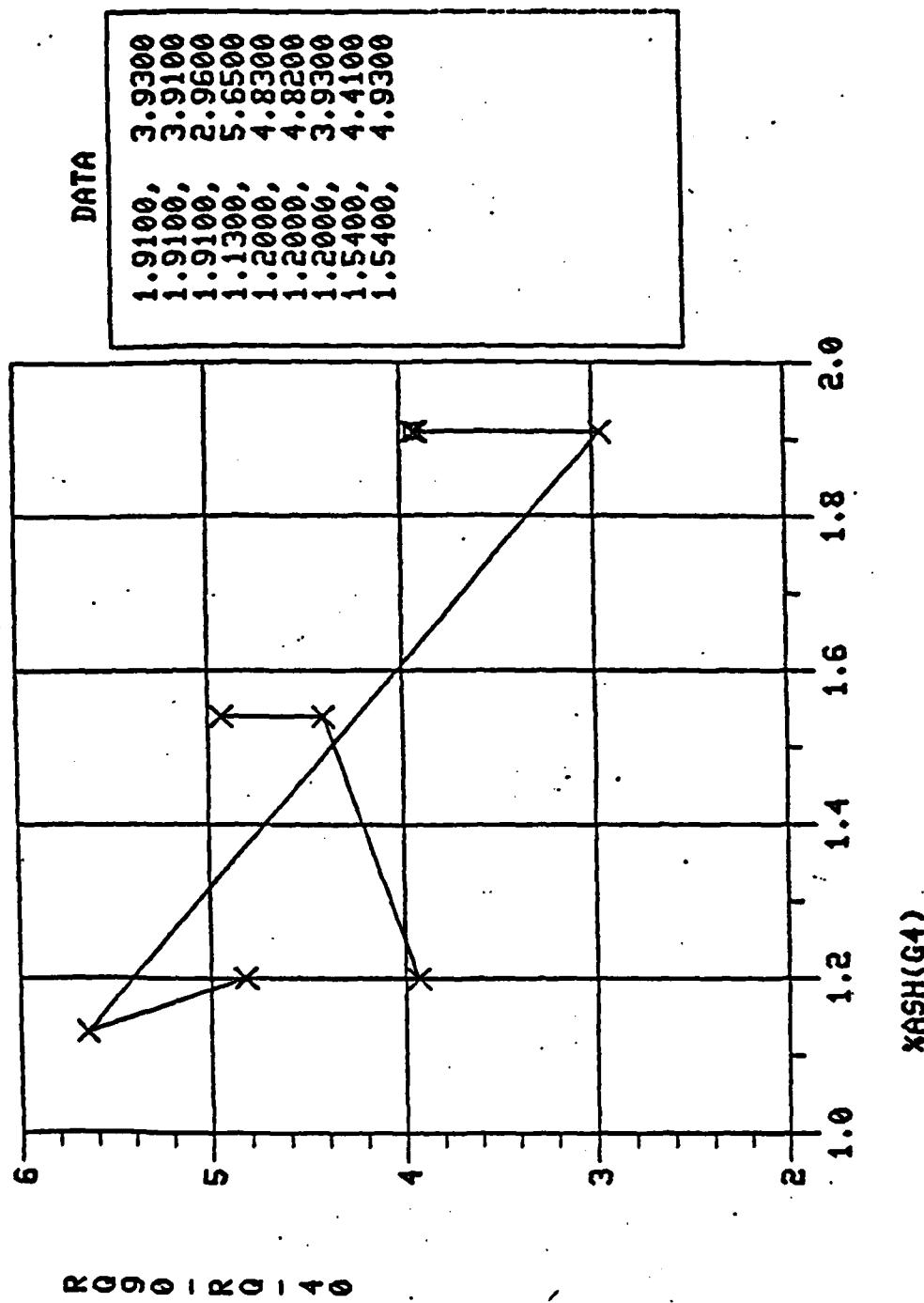


Fig. 21

PRESSURE COEFFICIENT, DP/DT VS. YR(STORAGE NGU) , C191

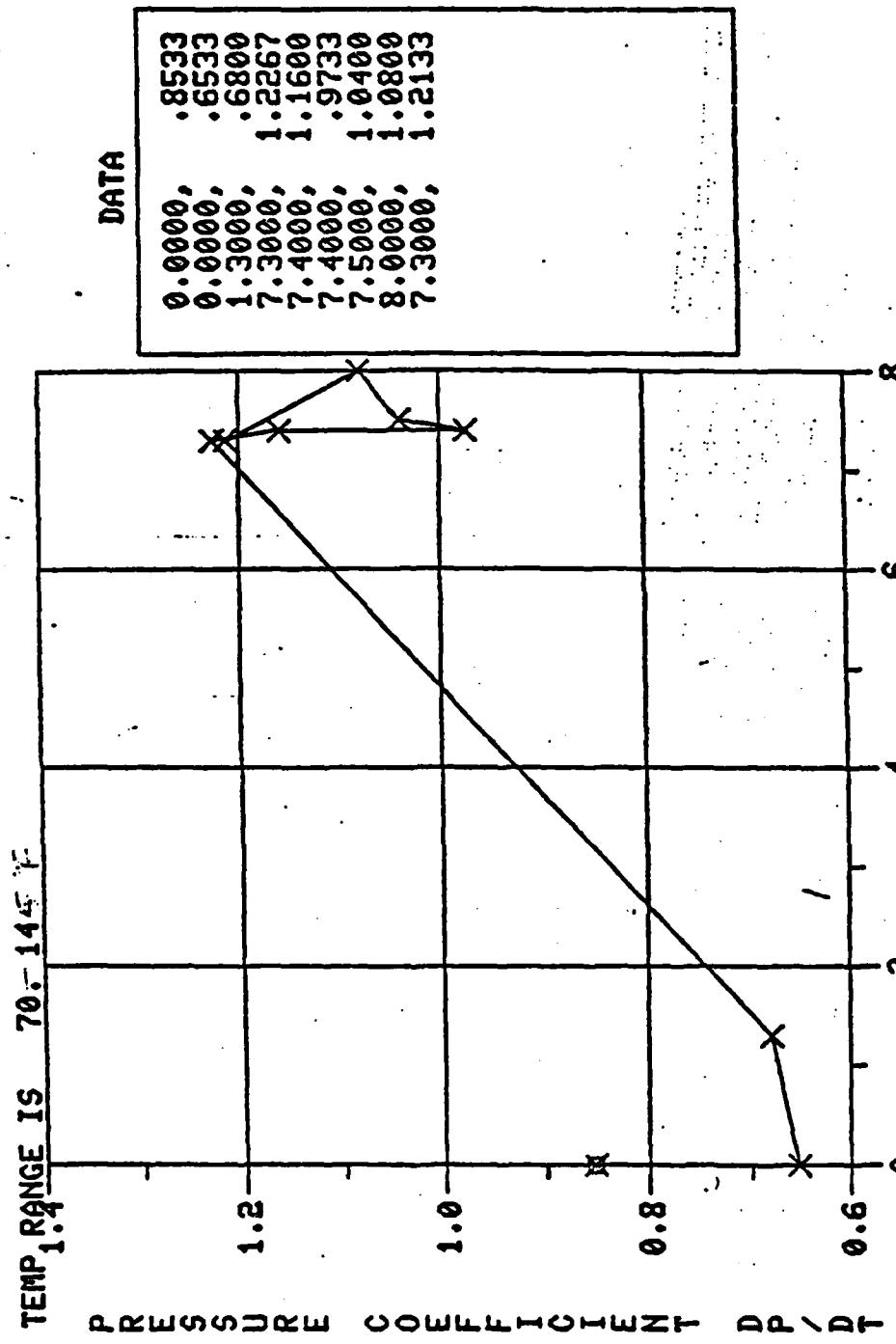


Fig. 22

$DP(RAD-T)/DP(RAD-C)145-70$ VS $YR(STORATE)$

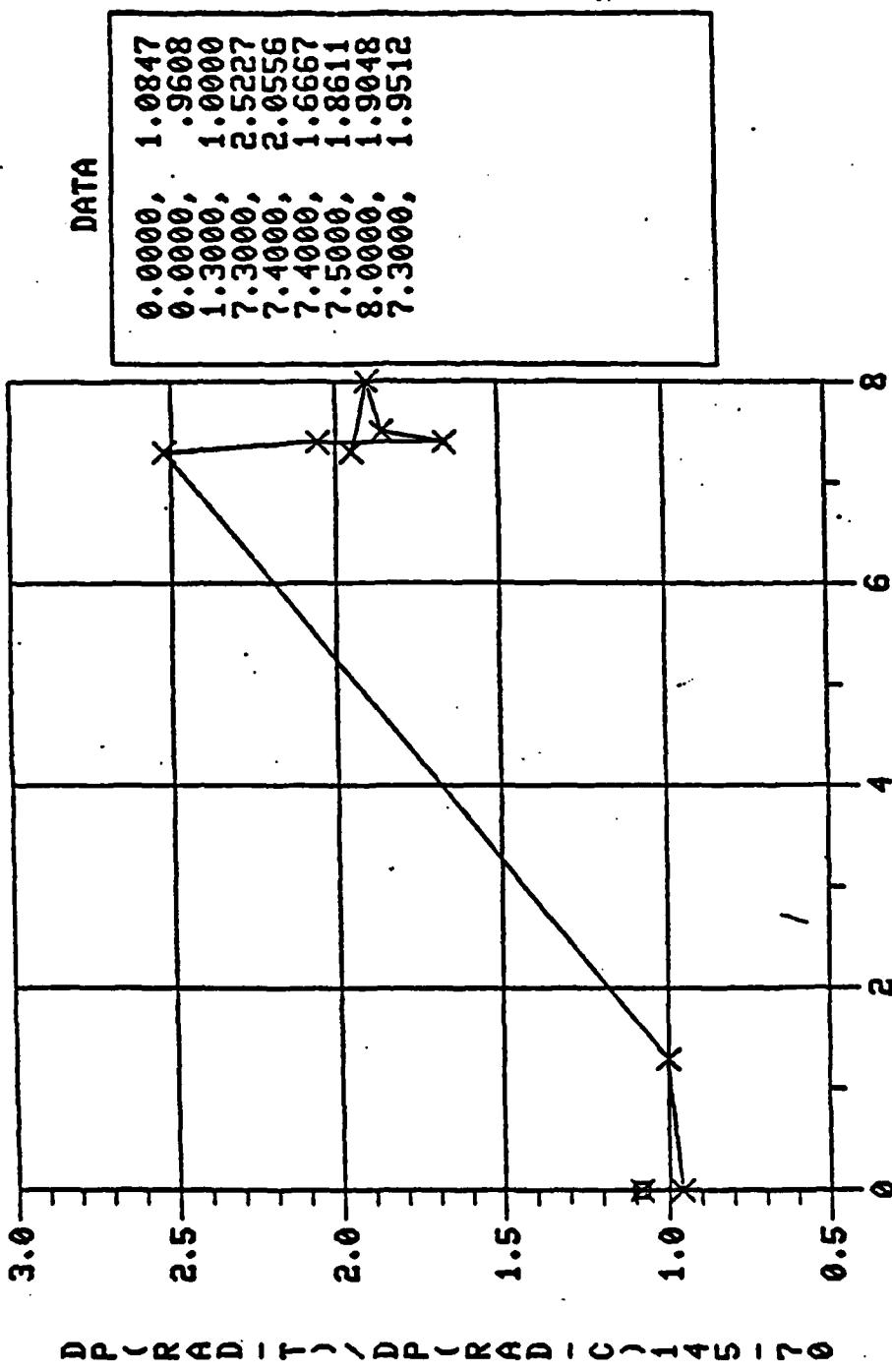
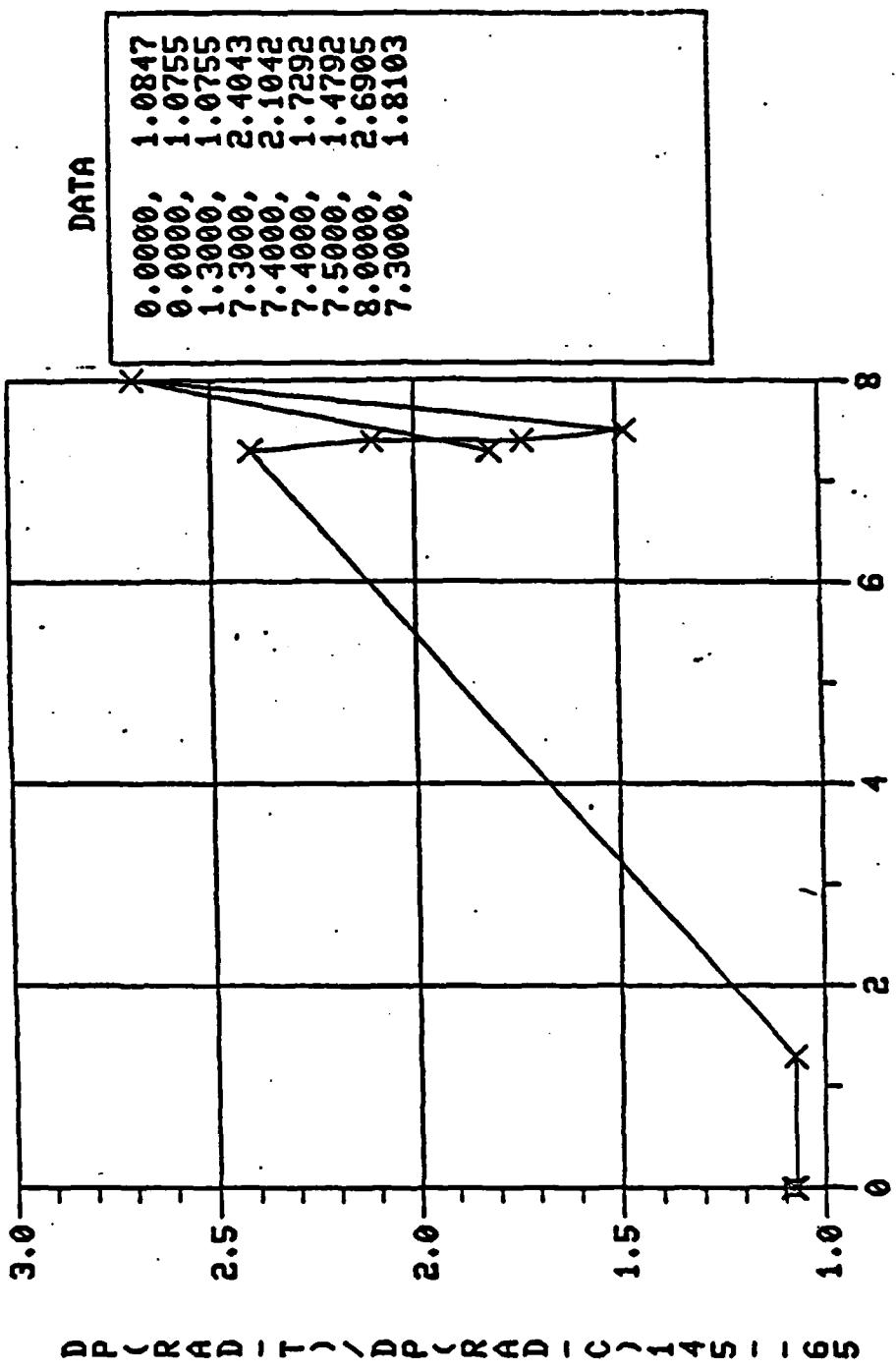


Fig. 23

$YR(STORATE)$ Nitroxazine

DP(RAD-T)/DP(RAD-C)145--65 VS YR(STORAGE)



Pig. 24

B. Summary of weak or slight trend
Plots

Fig # Independent Variable

25 % N₂ in Nitrocellulose

26 Viscosity

27-30 Freeness (Nitrocellulose)

31-34 PH Value (Nitroguanidine)

35-38 % Ethyl Centralite (% Composition)

39-44 Volatile Content (in Ethyl Centralite)

45-48 % Moisture (in Potassium Sulfate)

49-50 % Nitroglycerine (% Composition)

Dependent Variable

Pressure at 145 °F
 $\frac{DP}{DT_2} (70 - 145) °F$

Pressure at 70 °F
 $\frac{DP}{DT_2} (70 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_2 (70 - 145) °F$

$RQ90 - (RQ - 40)$
 $\frac{DP}{DT_2} (70 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_2 (70 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_1 (65 - 145) °F$

$RQ90 - (RQ - 40)$

$\frac{DP}{DT_2} (70 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_2 (70 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_1 (-65 - 145) °F$

$RQ90 - (RQ - 40)$

$RQ90 - RQ - 40$
Pressure at 70 °F

Pressure at 145 °F
 $\frac{DP}{DT_2} (70 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_1 (-65 - 145) °F$

$\frac{DP(\text{TEST})}{DP(\text{CALI})} DT_2 (70 - 145) °F$

Pressure at -65 °F

Pressure at 70 °F

Pressure at 145 °F

$\frac{DP}{DT_1} (-65 - 145) °F$

Pressure at -65

$\frac{DP}{DT_3} (-65 - 70) °F$

51 Length of Grain
52 Perforation Diameter
53 D/d

Pressure at 145°F
Pressure at -65°F
 $\frac{DP}{DT_2} (70 - 145)^\circ F$

54-57 Length uniformity of grain

RQ90-RQ -40
Pressure at 70°F
 $\frac{DP}{DT_2} (70 - 145)^\circ F$

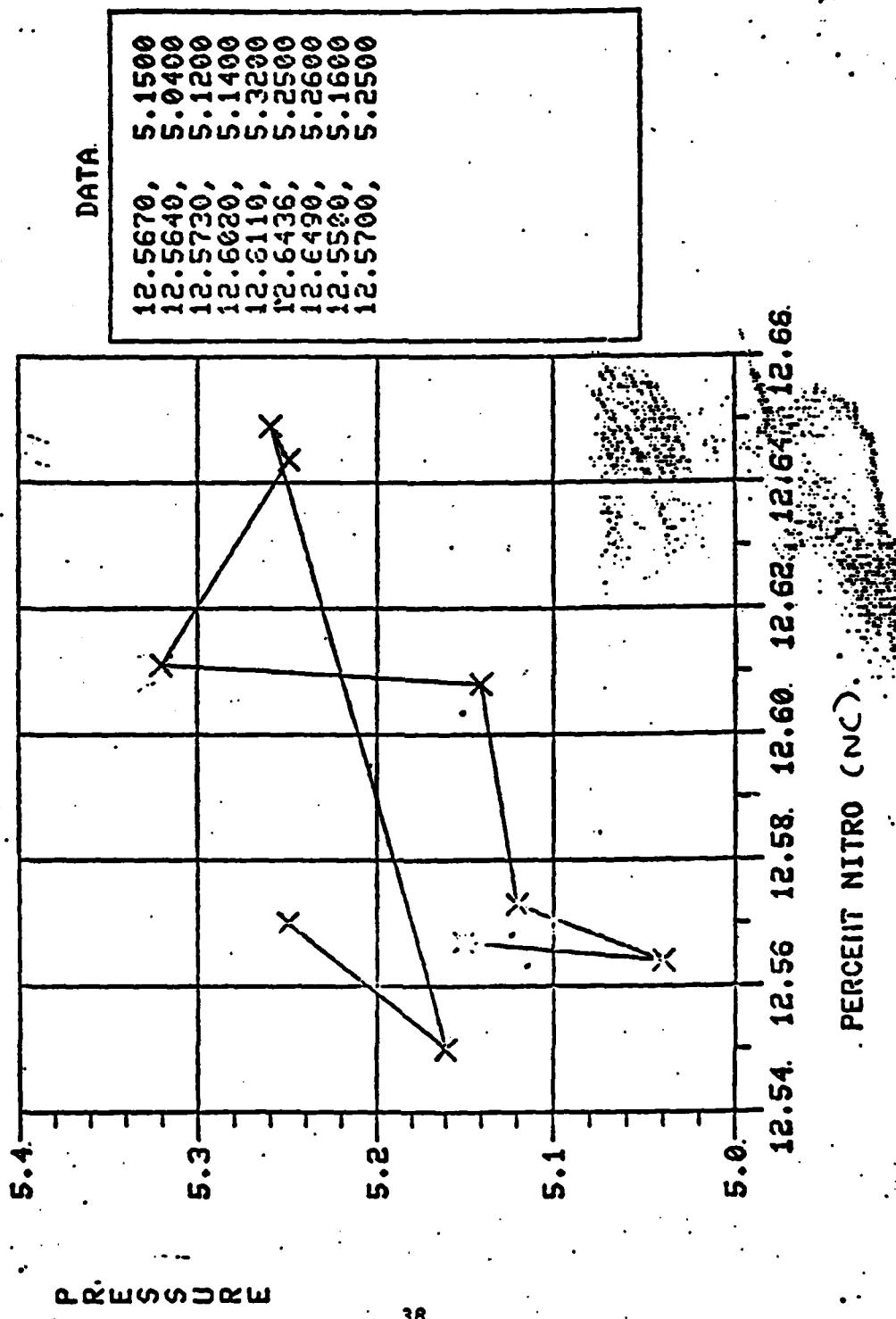
$\frac{DP(\text{TEST})}{DP(\text{CAL})}/DT_2 (70 - 145)^\circ F$
Pressure at 145°F
 $\frac{DP}{DT_2} (70 - 145)^\circ F$

58-61 Diameter uniformity of grain

RQ90-RQ -40
 $\frac{DP(\text{TEST})}{DP(\text{CAL})}/DT_2 (70 - 145)^\circ F$
Pressure at 145°F
RQ90-(RQ -40)

62-63 Yr (Storage) Nitroguanidine

PRESSURE VS. PERCENT NITRO, C011 TEMP = 145.



C014

PRESSURE COEFFICIENT, D_P/D_T VS VISCOSITY

TEMP RANGE IS 79 - 140

PRESSURE COEFFICIENT D_P/D_T

DATA

12.2222,	85.3333
13.1818,	65.3333
13.1666,	63.0000
13.2222,	122.6667
14.9999,	116.0000
14.0000,	97.3333
12.1030,	104.0000
16.7143,	108.0000
9.3333,	121.3333

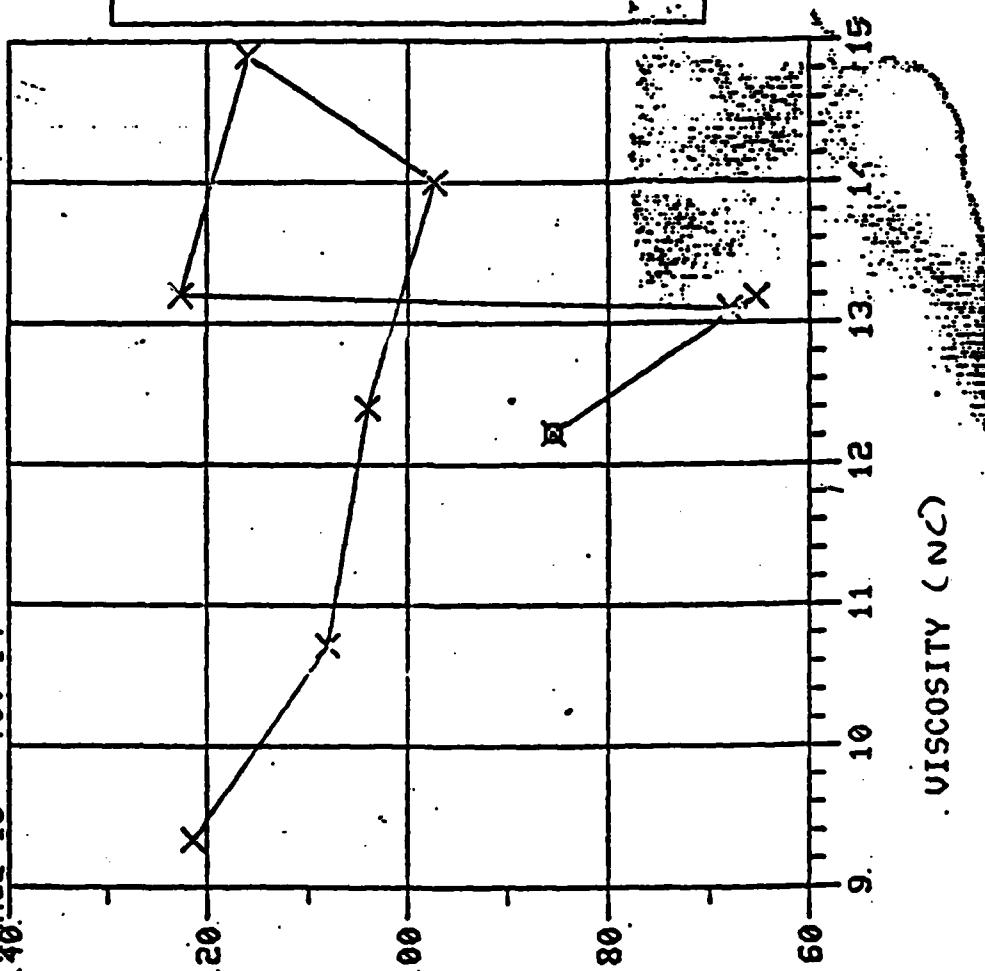


Fig. 26

PRESSURE US. FREENESS
C015 TEMP = 70.

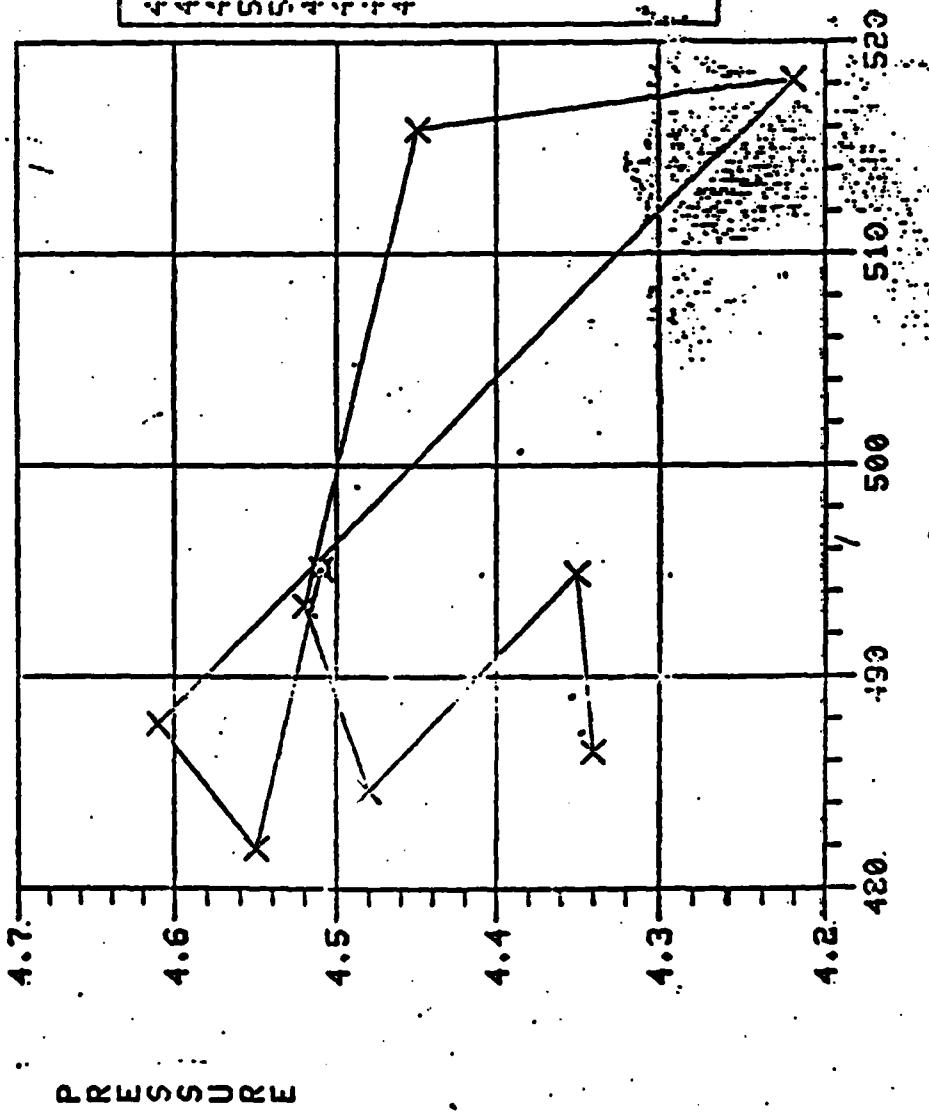


Fig. 27

.C015

PRESSURE COEFFICIENT, DP/DT VS. FREENESS

TEMP RANGE IS (70-145)°F

PRESSURE COEFFICIENT DP/DT

DATA

495.1000, 85.3333
481.9900, 65.3333
487.2600, 62.0000
516.2600, 122.6667
515.3000, 116.0000
479.3636, 97.3333
434.6000, 104.0000
434.2571, 103.0000
426.4444, 121.3333

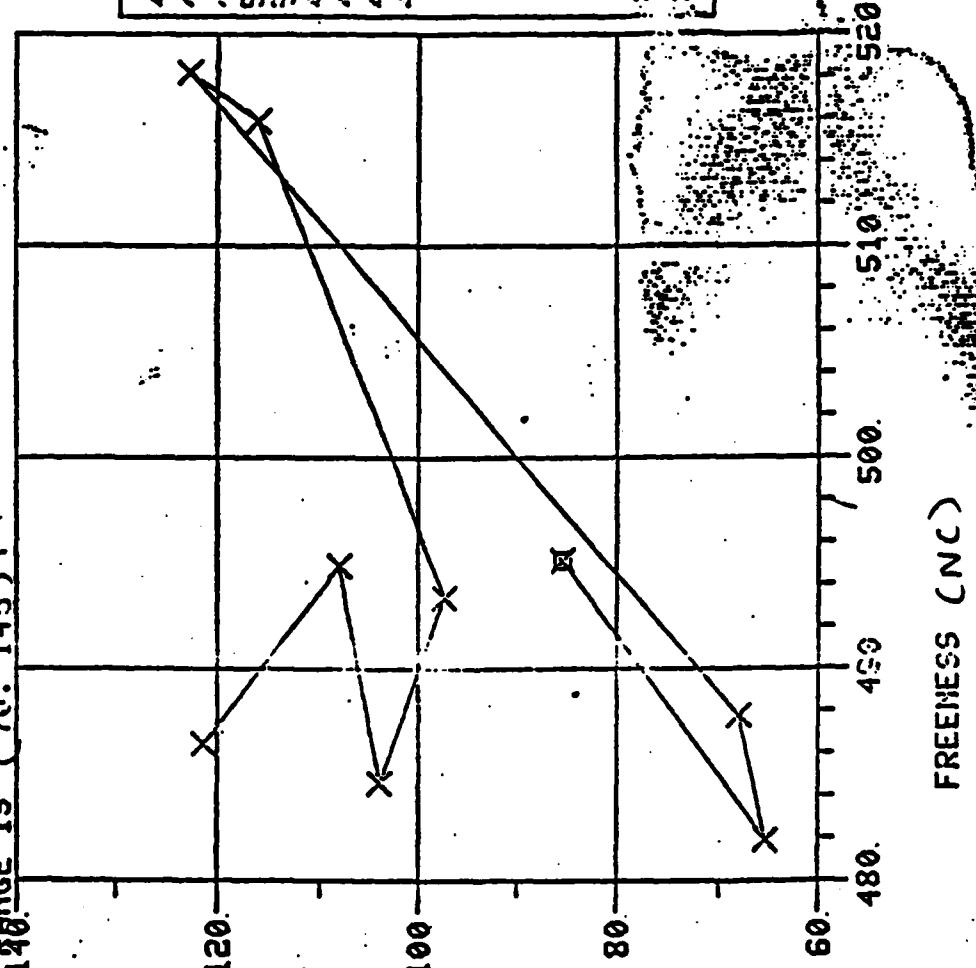


Fig. 29

DP(RAD-T)/DP(RAD-C)145-70 VS FREE(NC)

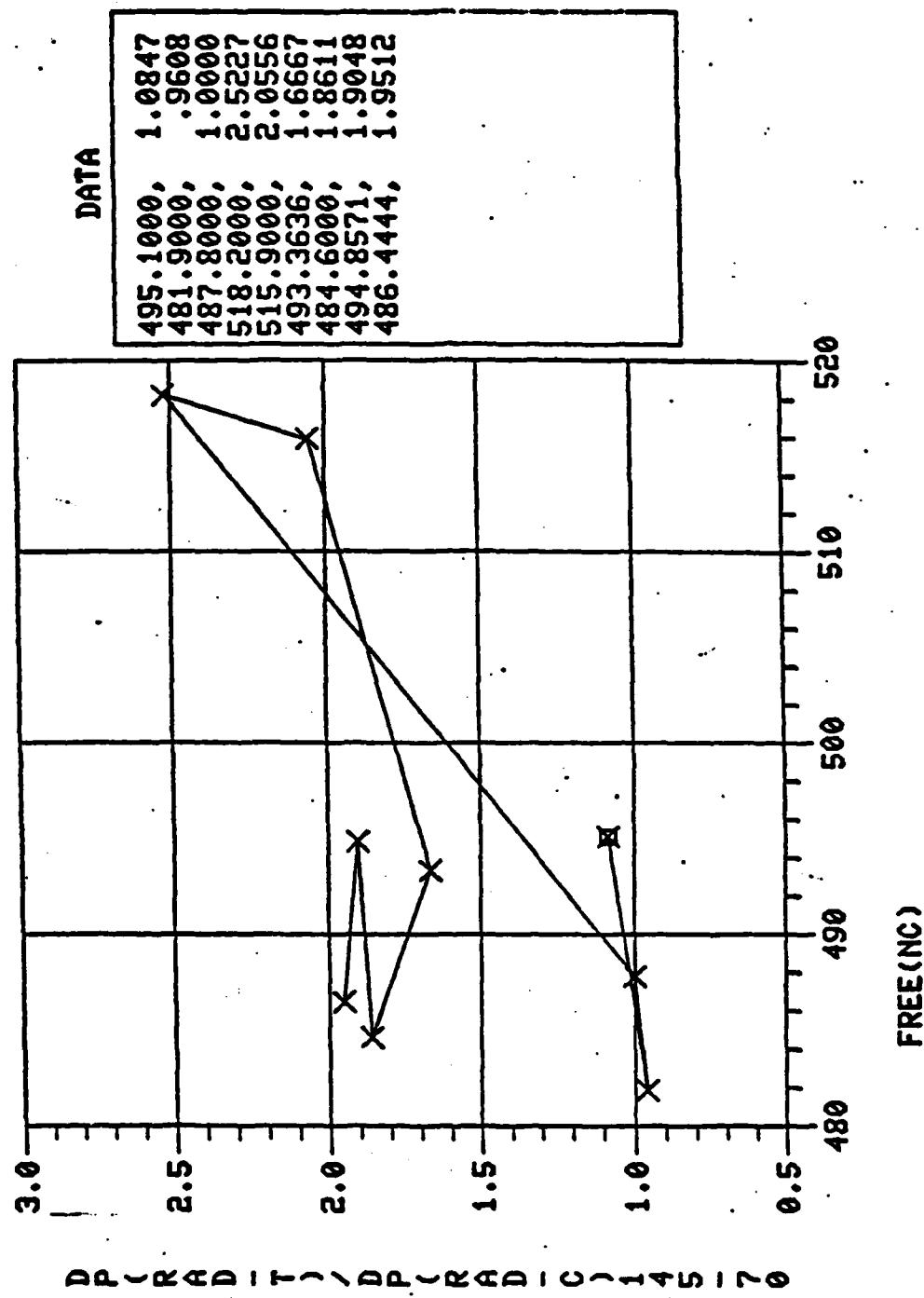


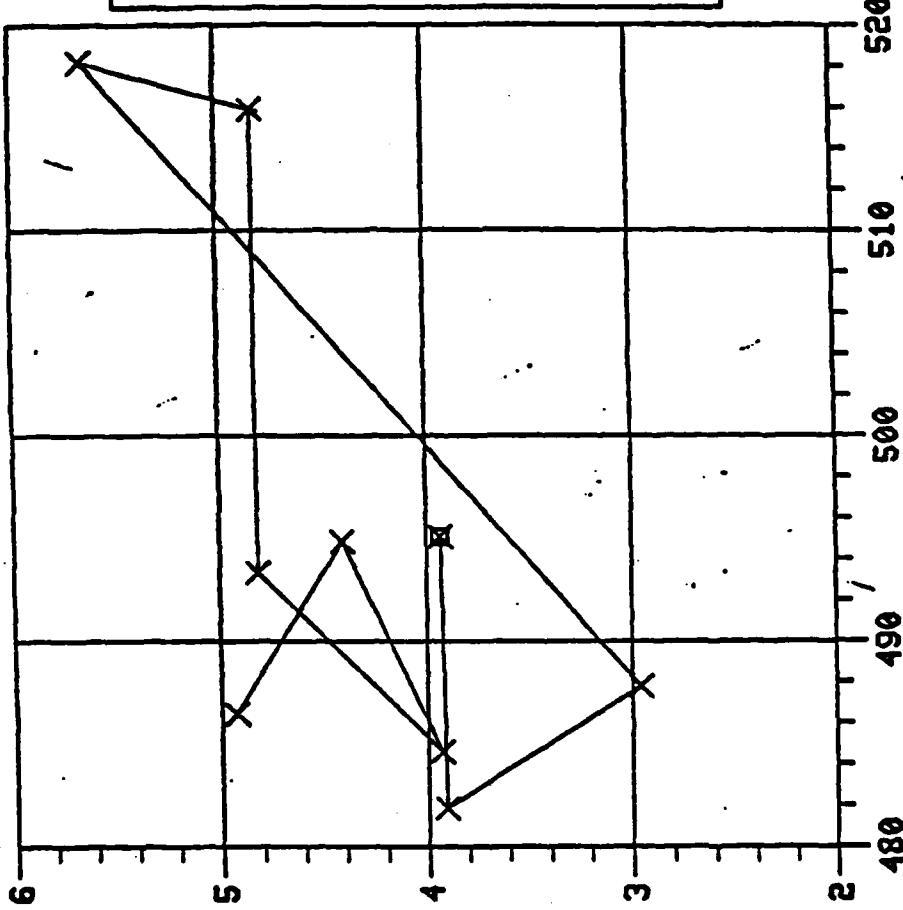
Fig. 29

RQ90-RQ-40 USFREE(NC)

RQ90+RQ-40

DATA

495.1000,	3.9300
481.9000,	3.9100
487.8000,	2.9600
518.2000,	5.6500
515.9000,	4.8300
493.3636,	4.8200
484.6000,	3.9300
494.8571,	4.4100
486.4444,	4.9300



FREE (NC)

Fig. 30

C034

PRESSURE COEFFICIENT, DP/DT VS PH VALUE

TEMP RANGE IS (70-145)°F

PRESSURE COEFFICIENT DP/DT

DATA

5.3720	85.3333
5.4500	65.3333
5.3103	68.0000
5.2833	122.6667
5.1067	116.0000
5.0250	97.3333
5.1773	104.0000
5.1750	108.0000
5.2278	121.3333

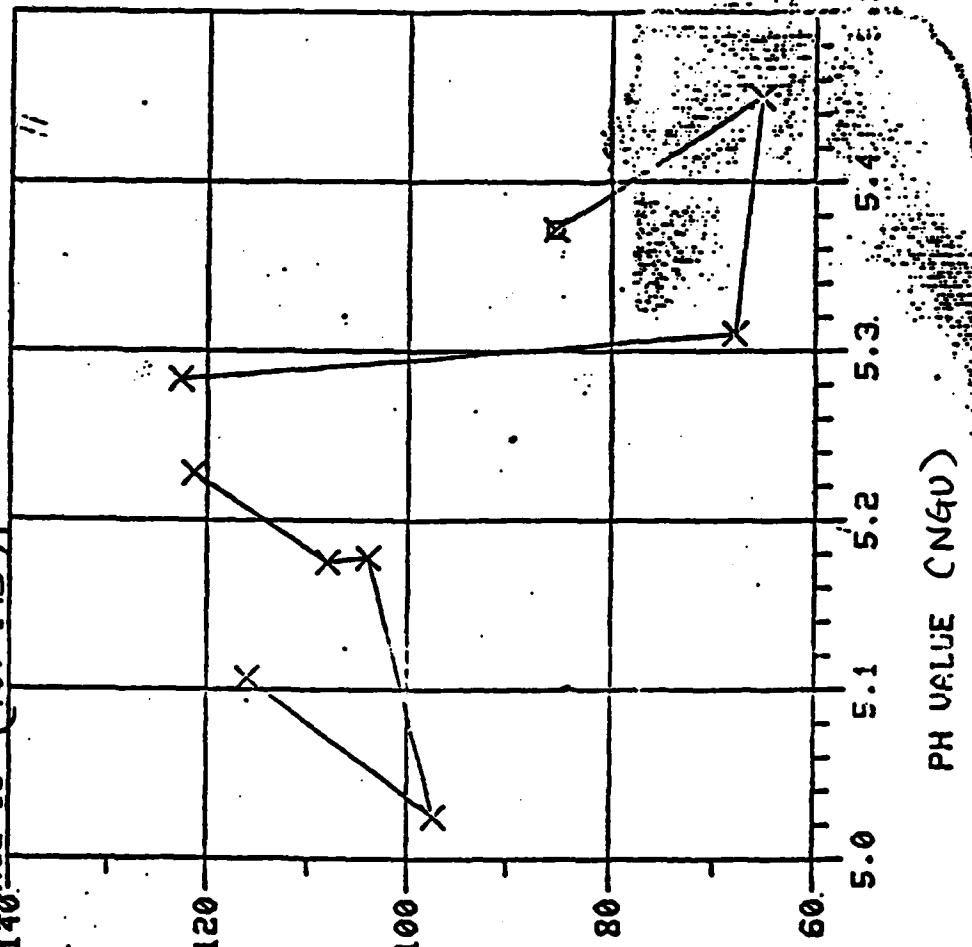


Fig. 31

$D_P(RAD-T) / D_P(RAD-C)_{145-70}$ VS PH(NGU)

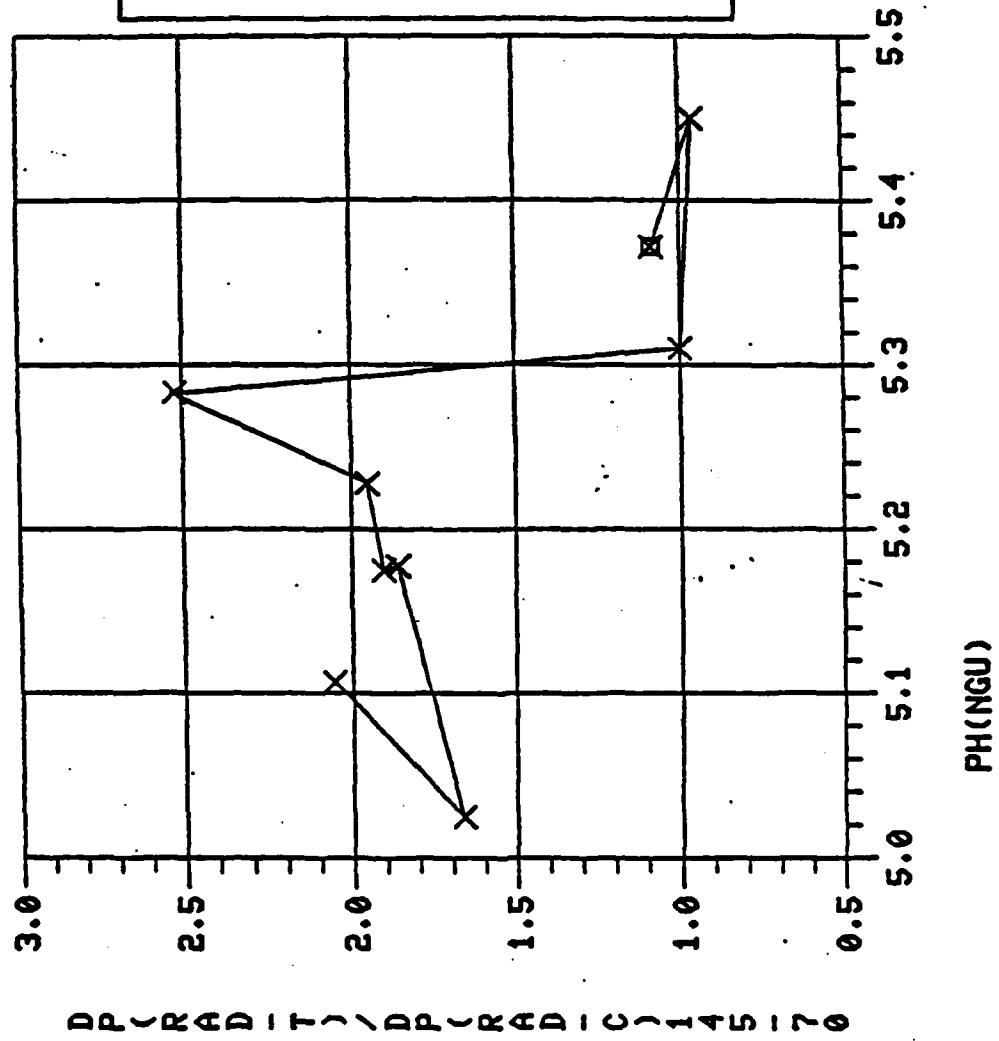


Fig. 32

DP(RAD-T)/DP(RAD-C)145--65 USPH(NGU)

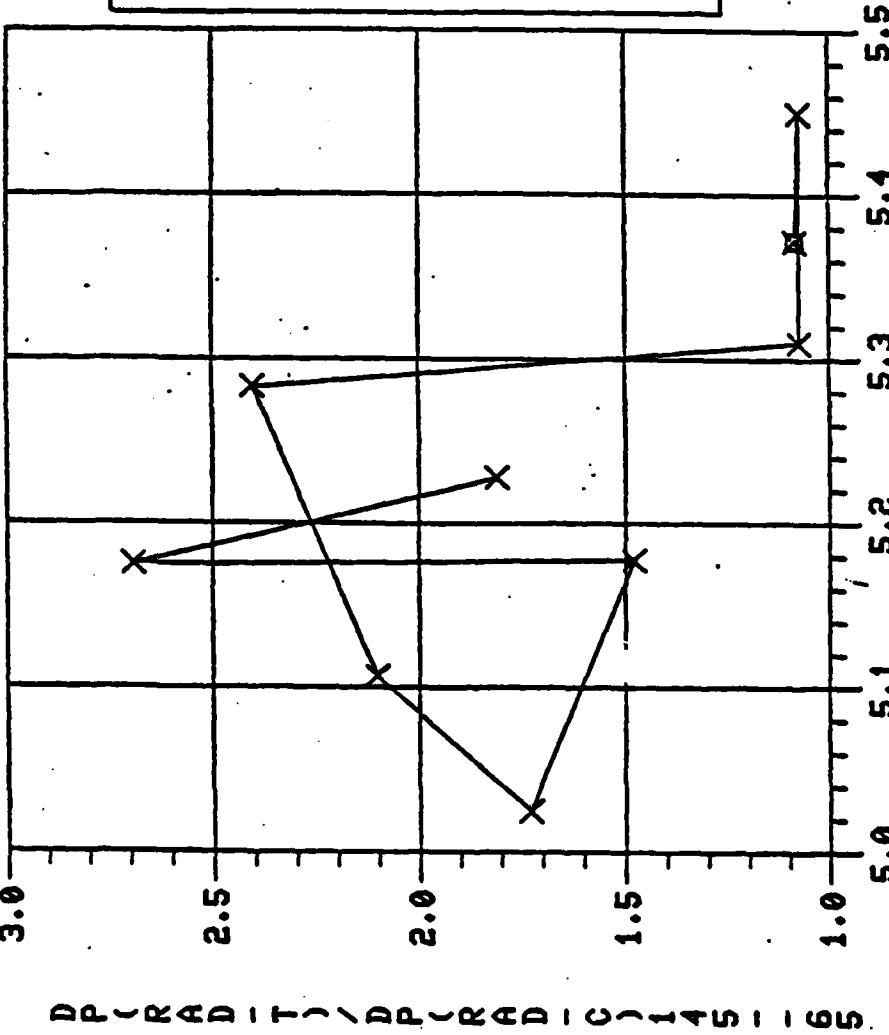
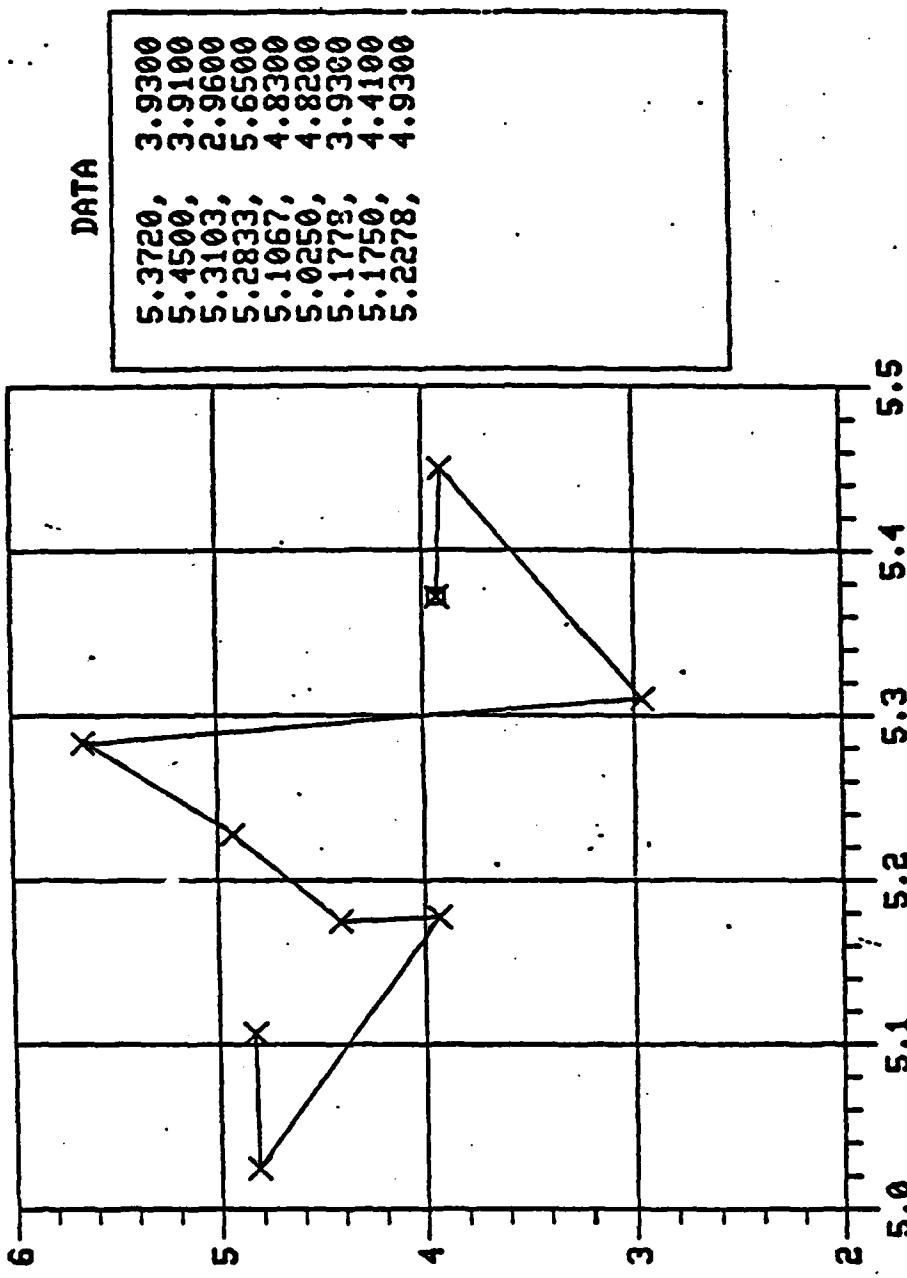


Fig. 33

RQ90-RQ-40 USPH(NGU)



RQ90-RQ-40

Fig. 34

PRESSURE COEFFICIENT, DP/DT VS. ETHYL CENTRAL, .C104

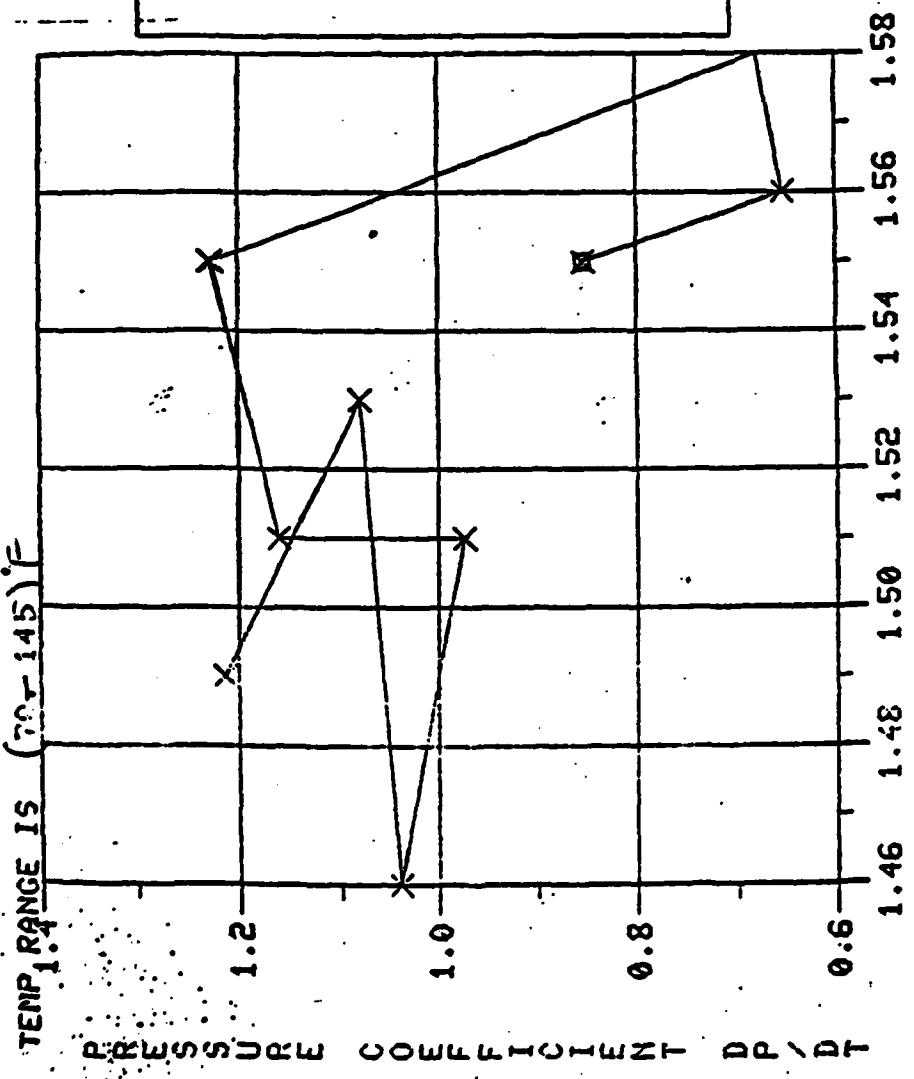


Fig. 35

$DP(RAD-T)/DP(RAD-C)_{145-70}$ VS E.C. (KC)

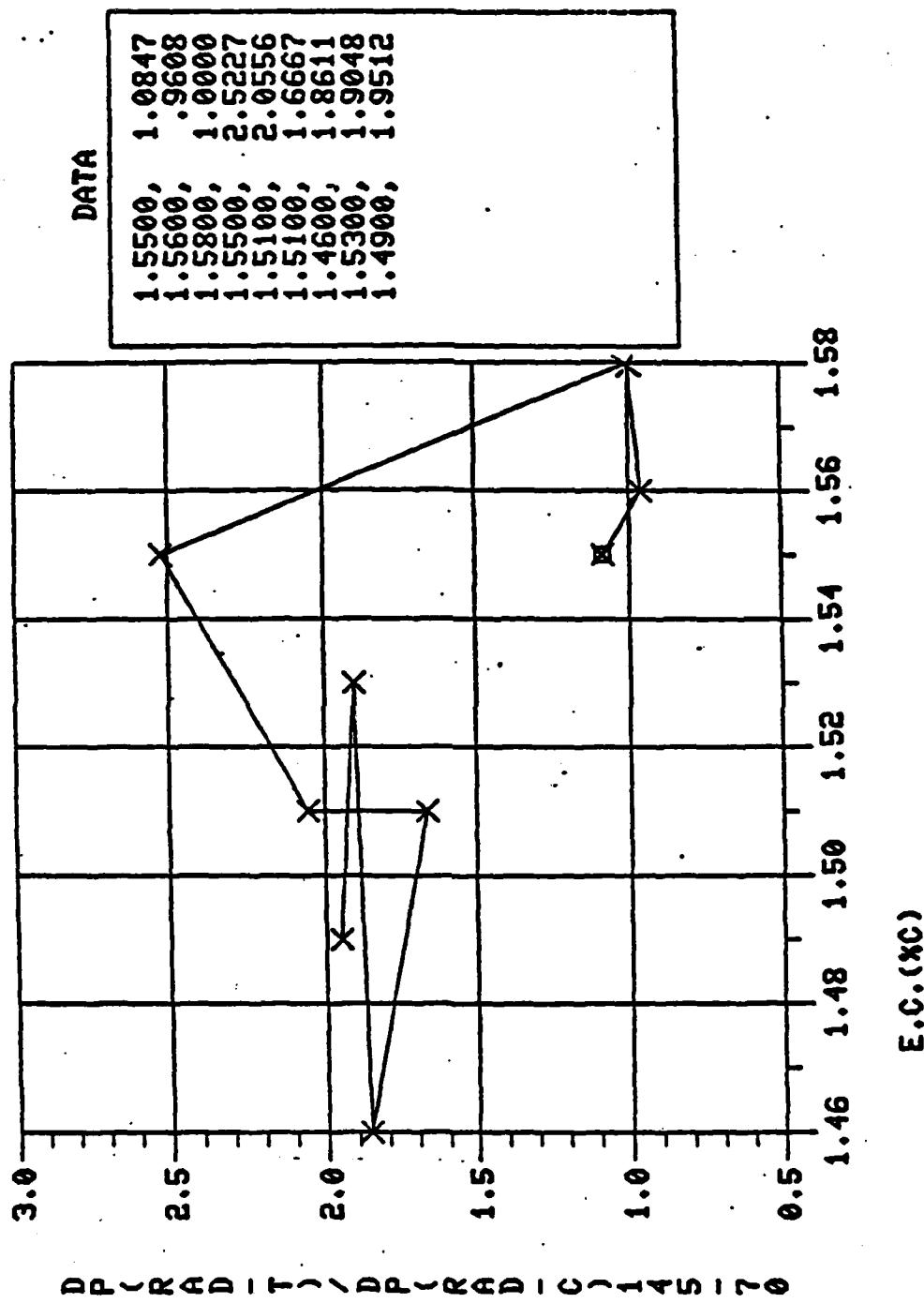


Fig. 36

DP(RAD-T)/DP(RAD-C)145--65 USE.C.(XC)

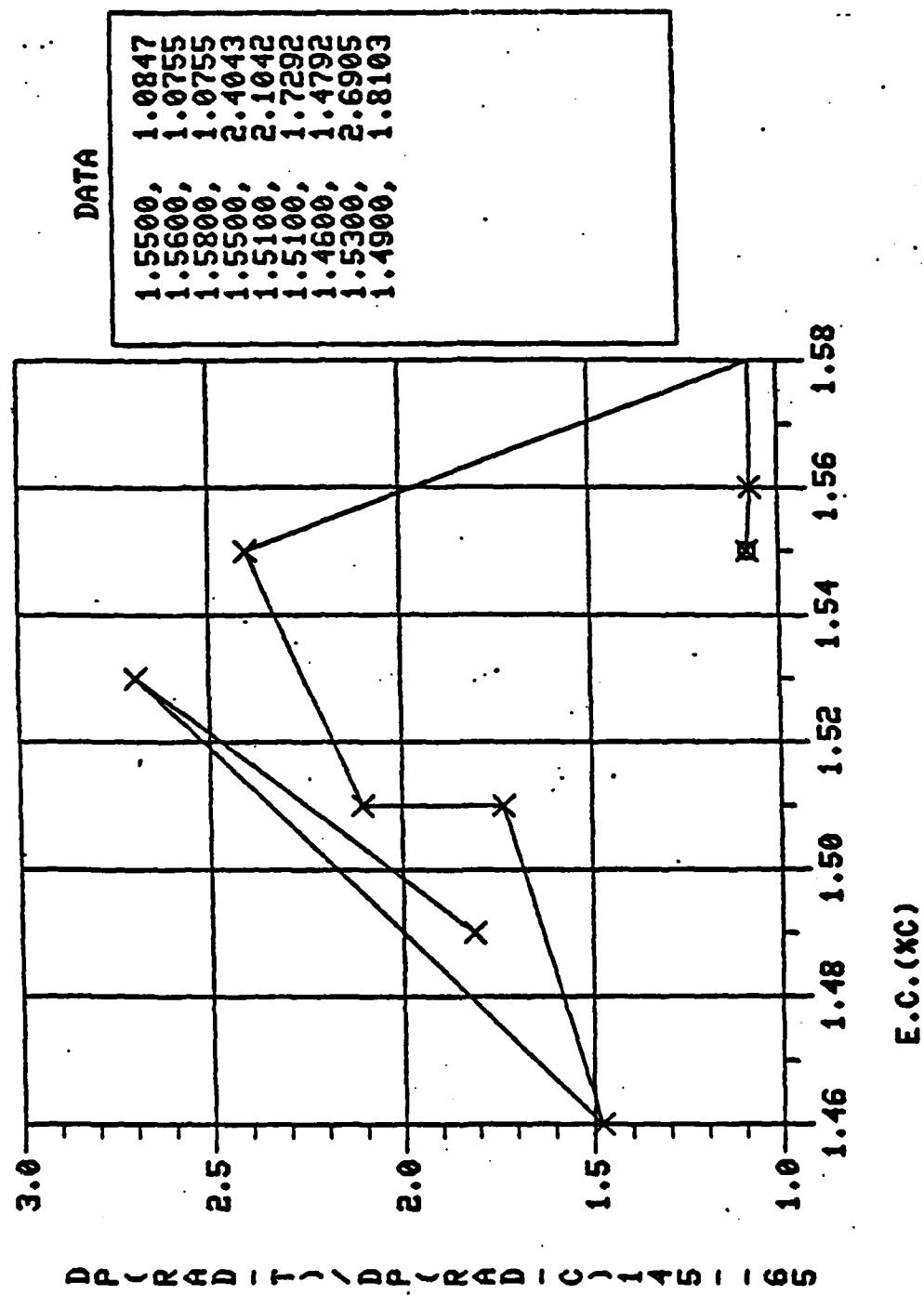
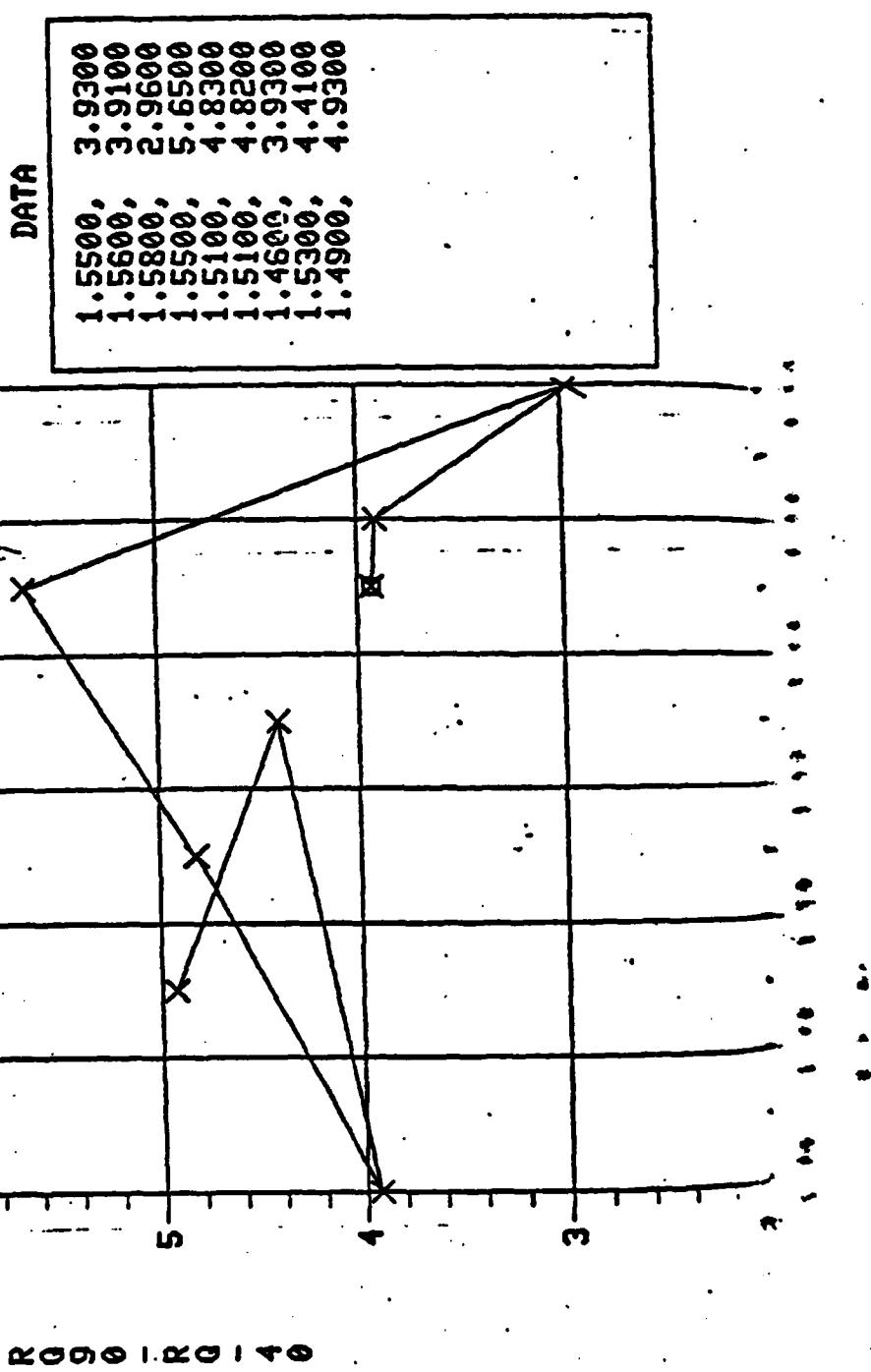


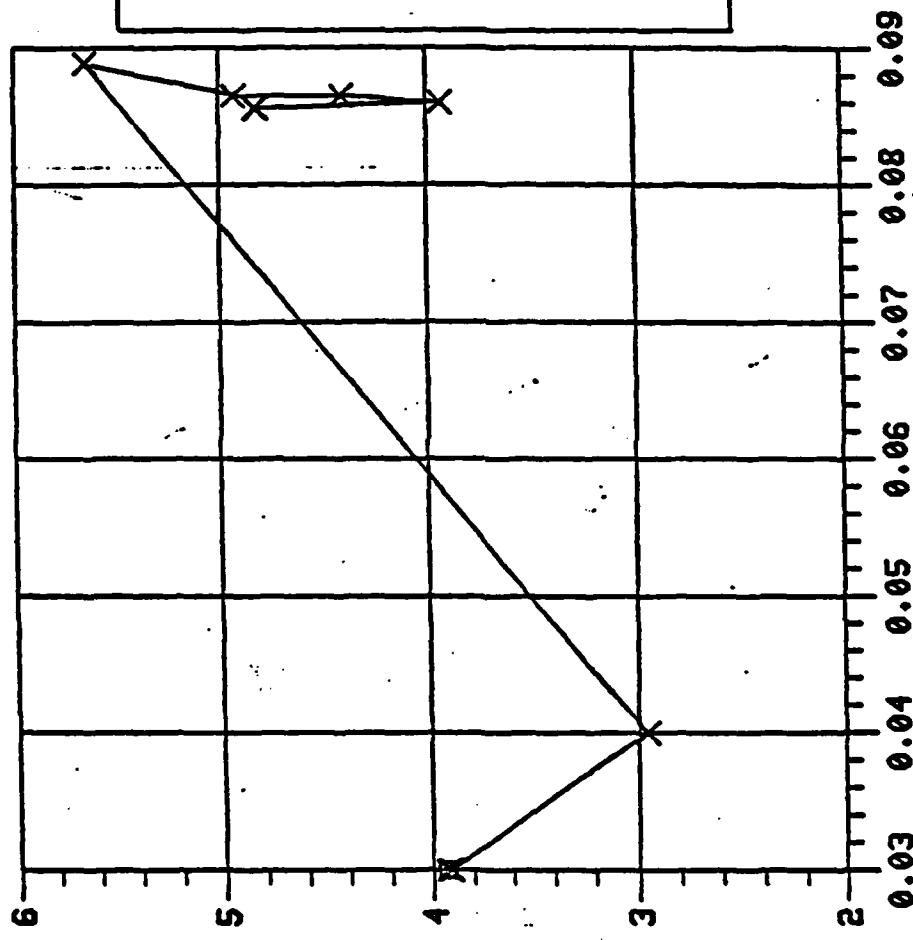
Fig. 37

RQ90-RQ-40 USE.C. (XC)



Via. 38

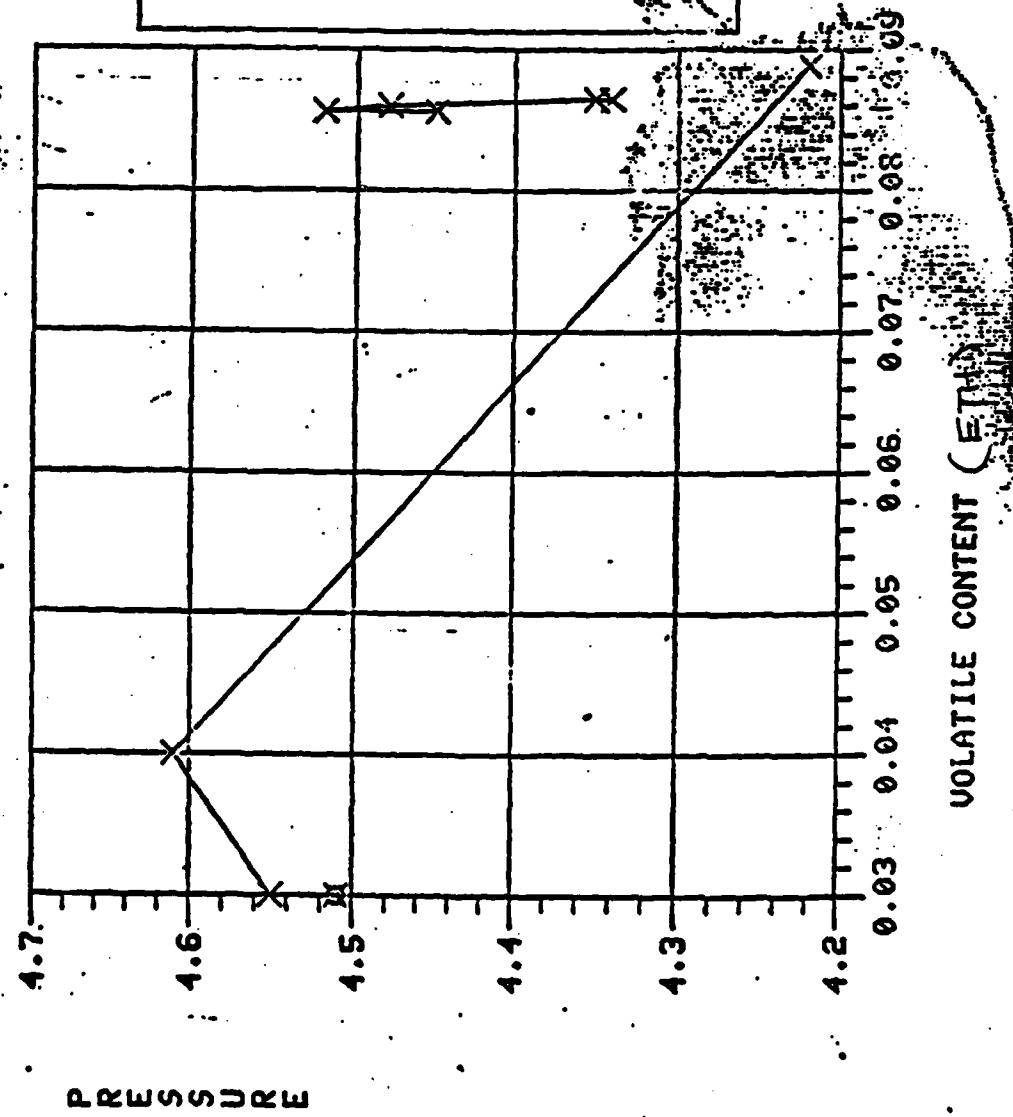
RQ90-RQ-40 USV.C. (ETH)



RQ90 | RQ-40

PRESSURE VS. VOLATILE CONTENT (CET)

TEMP = 70.



DATA	
0.300,	4.5100
0.300,	4.5500
0.400,	4.6100
0.289,	4.2200
0.256,	4.4500
0.256,	4.5200
0.369,	4.4800
0.365,	4.3500
0.265,	4.3400

PRESSURE VS. VOLATILE CONTENT, CO₂ AT TEMP. = 145.

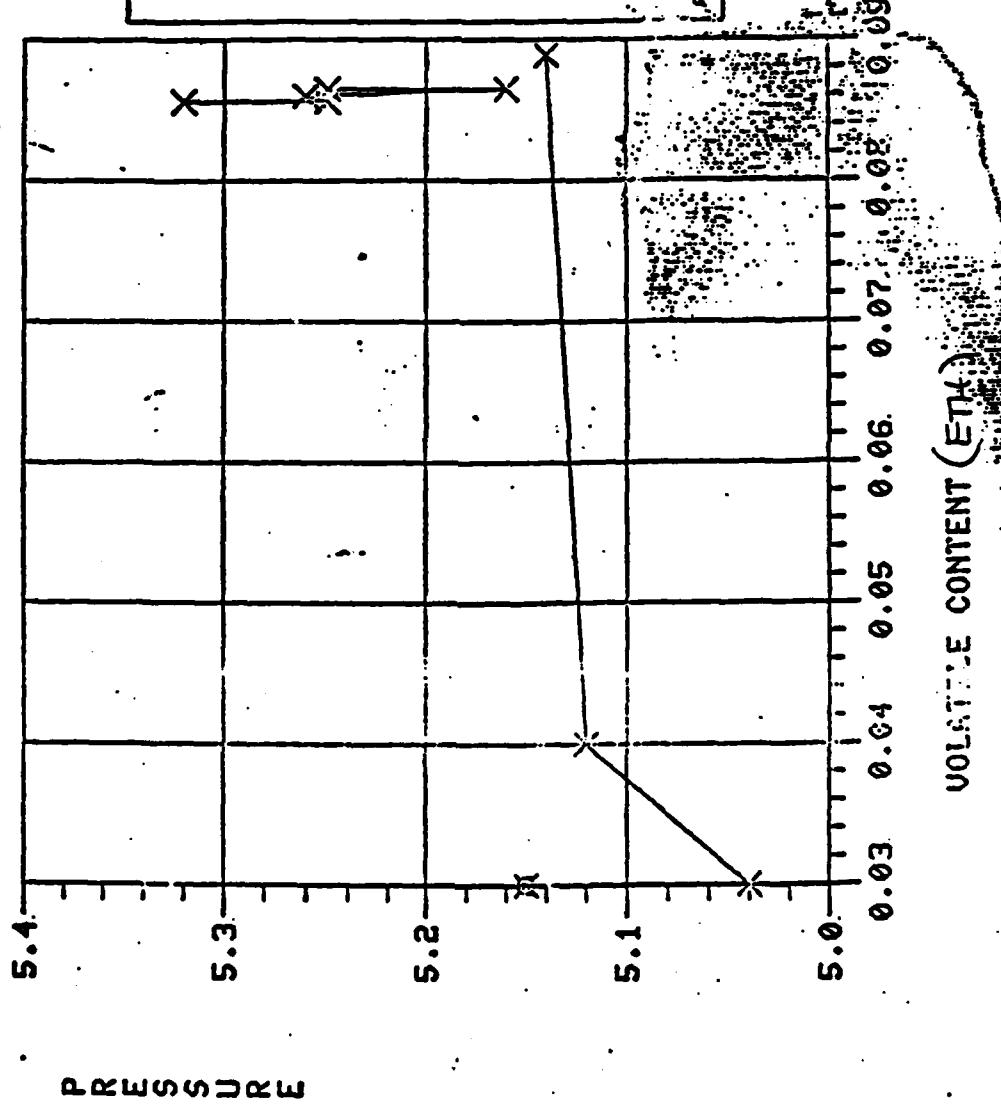


Fig. 41

PRESSURE COEFFICIENT, $\frac{dp}{dt}$ AT VOLATILE CONTENT, C042

TEMP RANGE IS $(70 - 145)^\circ F$

P R E S S U R E C O E F F I C I E N T $D P / D T$

DATA.

0.0300	85.3333
0.0300	65.3333
0.0400	62.0000
0.0800	122.6667
0.0250	116.0000
0.0850	97.3333
0.0350	104.0000
0.0250	108.0000
0.0350	121.3333

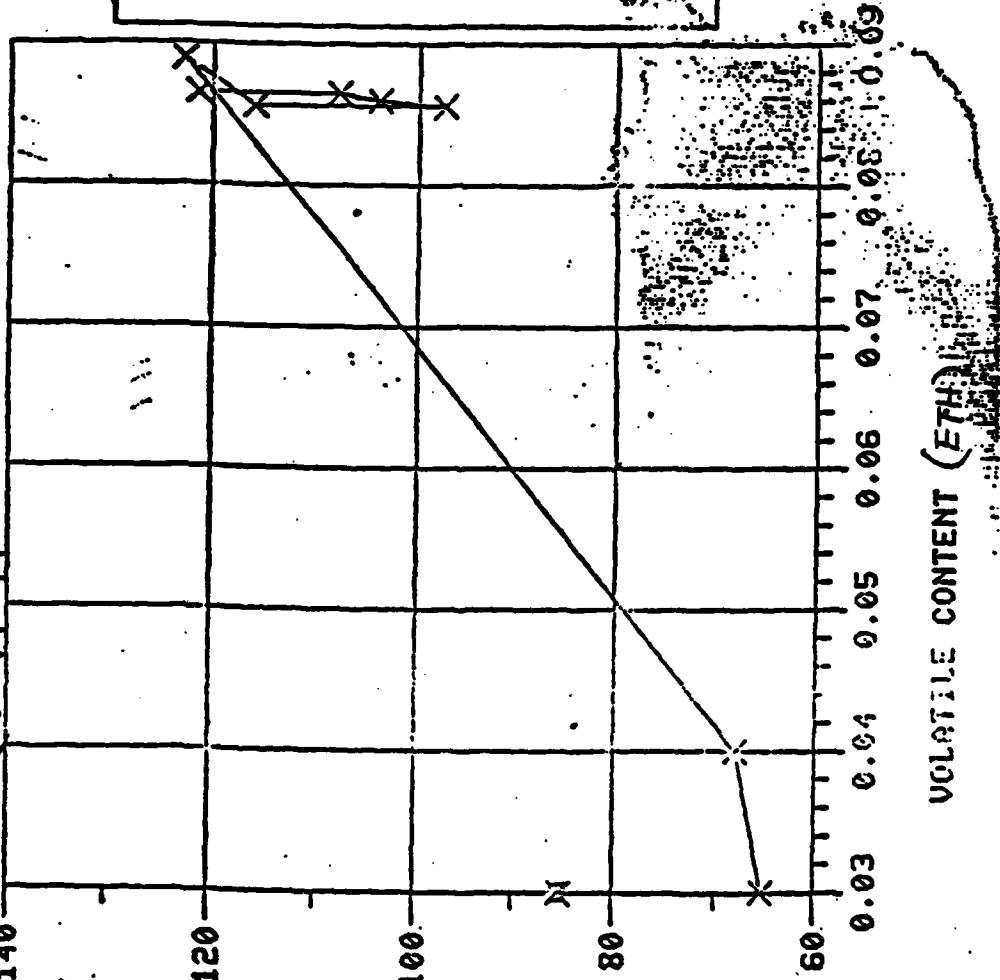


Fig. 42

D_P(RAD-T)/D_P(RAD-C) 145--65 VS U.C.(ETH)

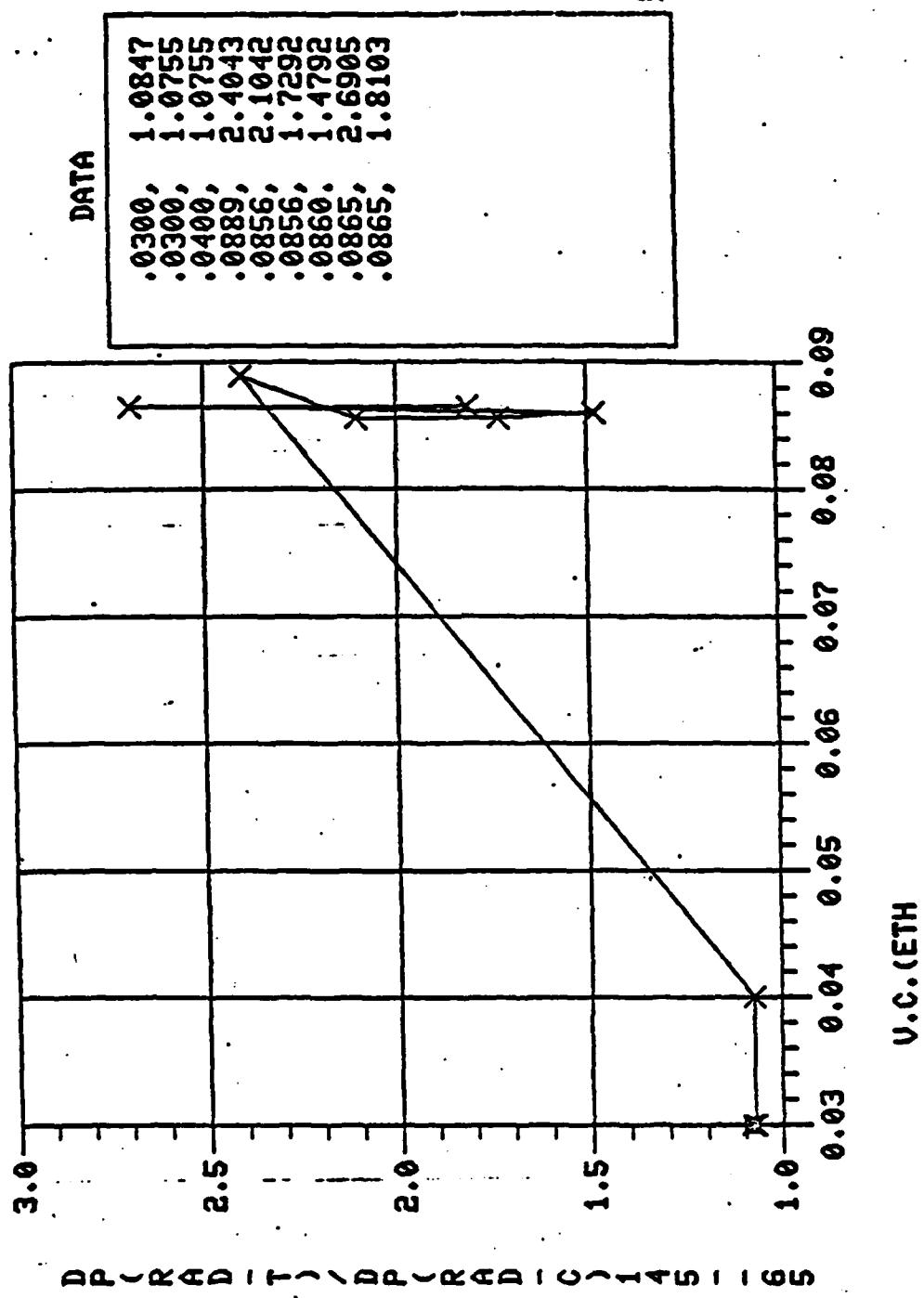


Fig. 43

$D_P(RAD-T)/D_P(RAD-C)145-70$ VS U.C. (ETH)

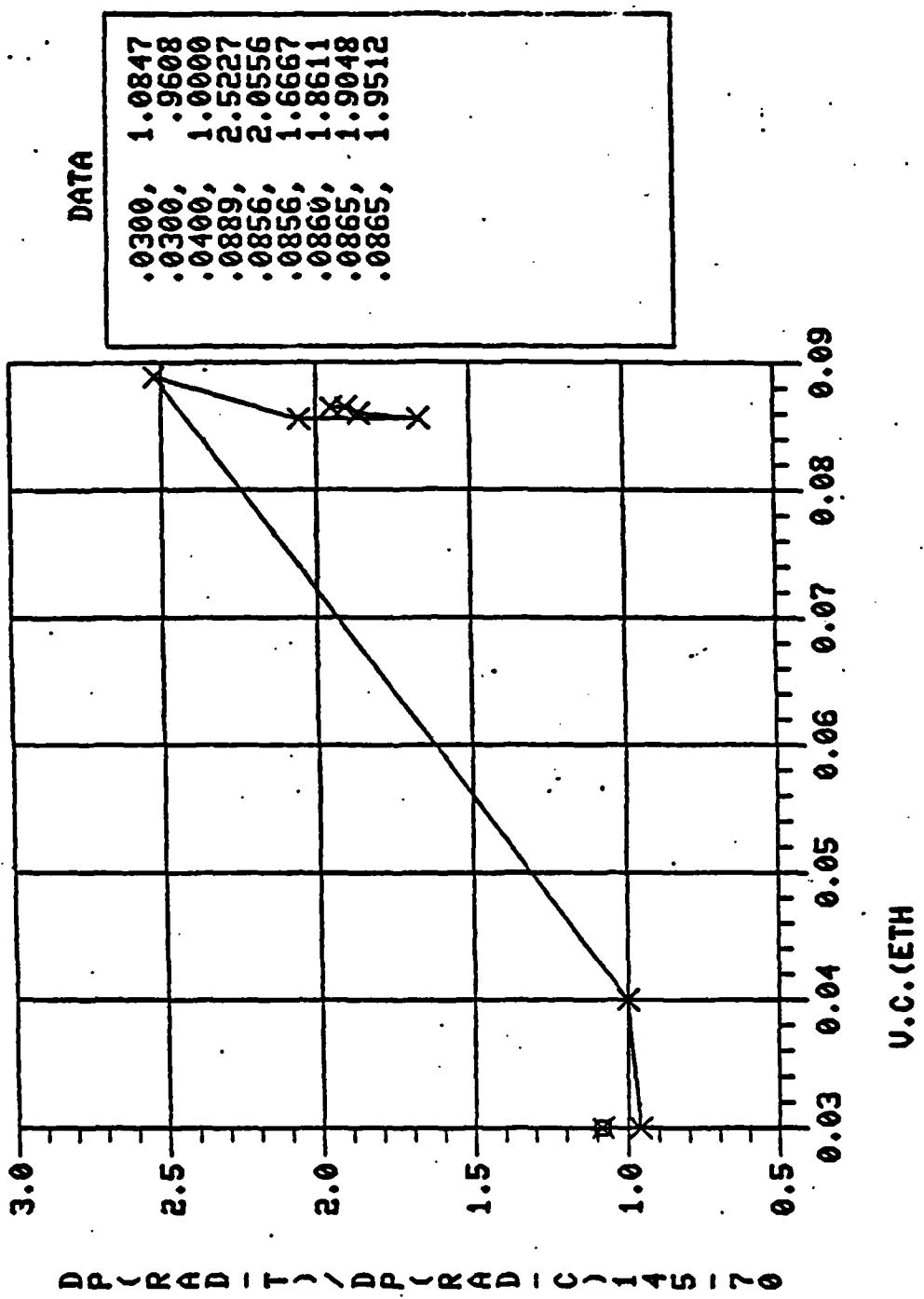


Fig. 44

PRESSURE vs. % MOISTURE , C051 - TEMP = -65.

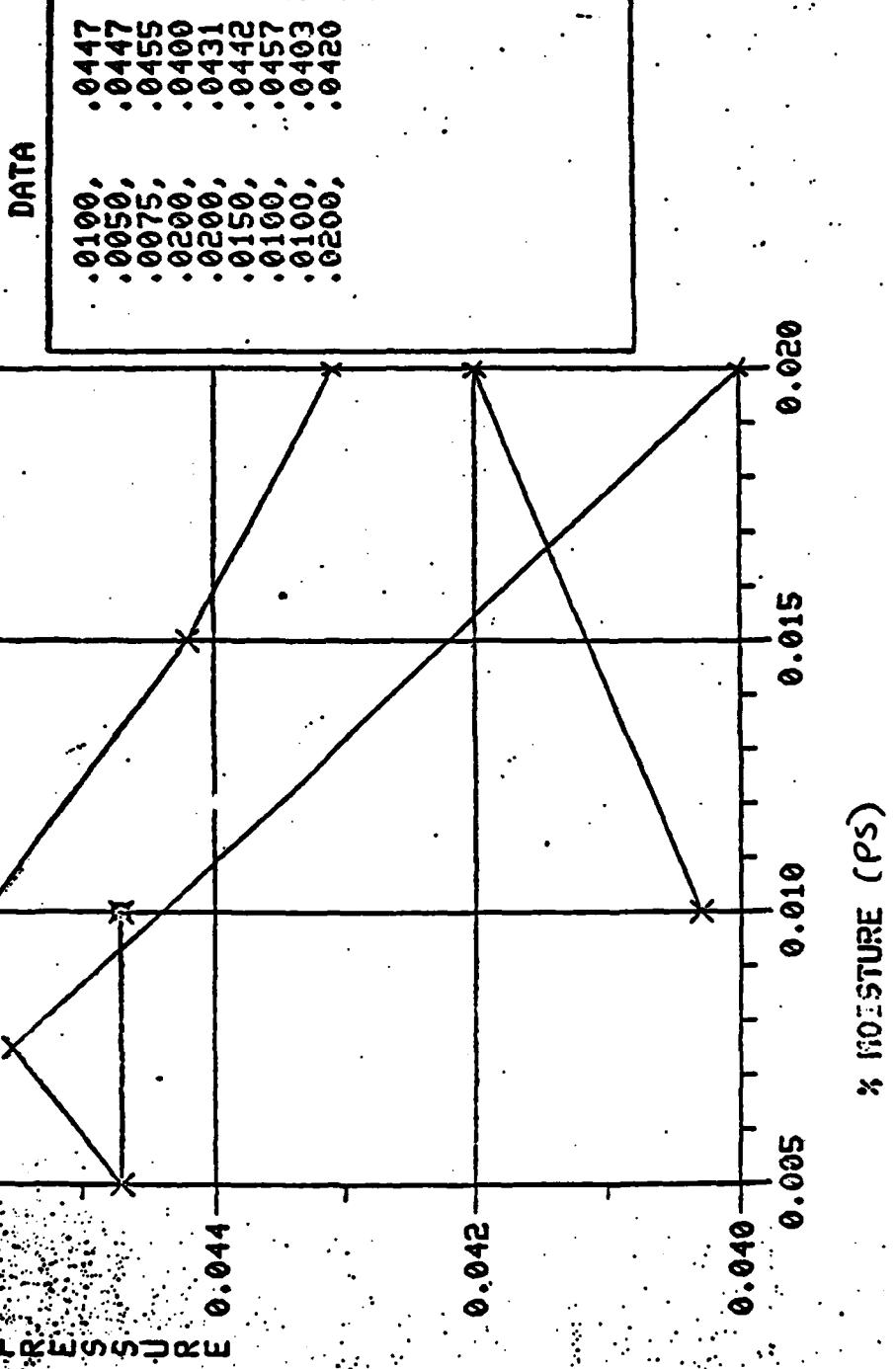


Fig. 45

PRESSURE VS. % MOISTURE , C051 TEMP = 70.

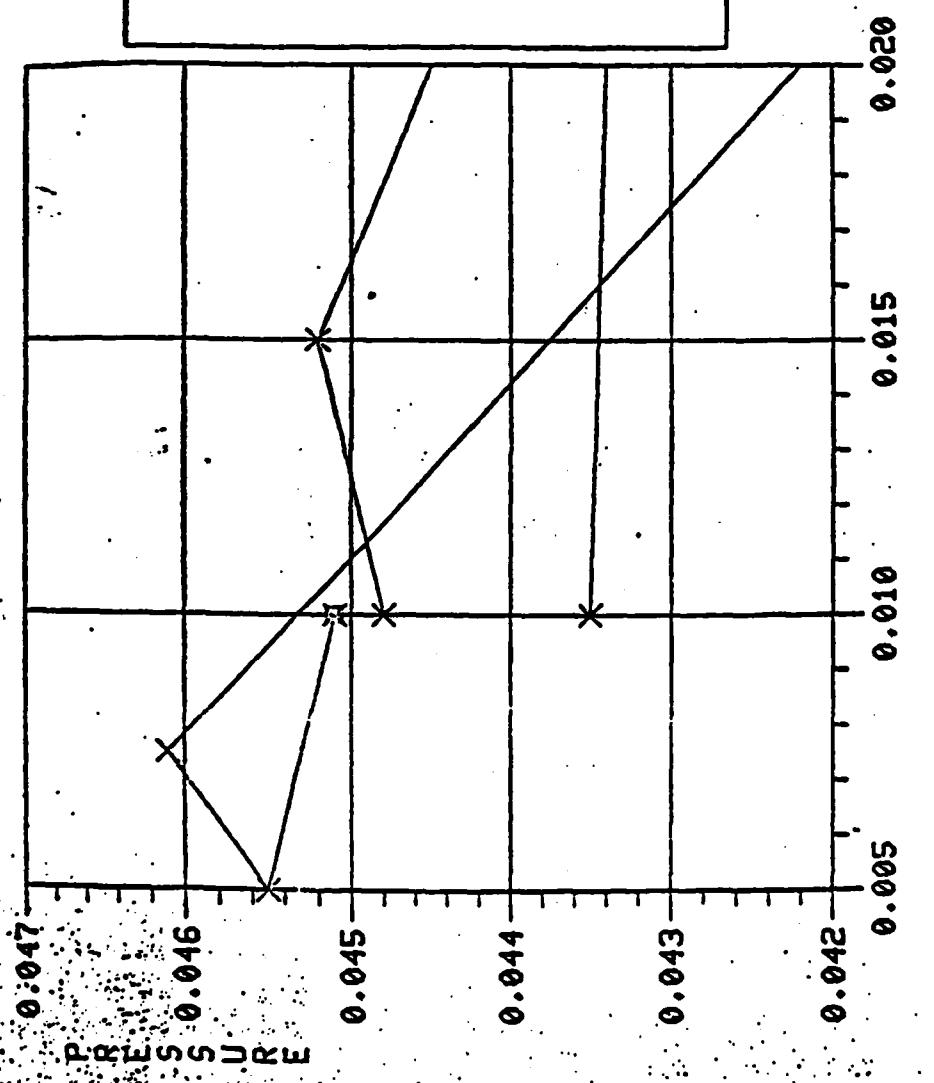


Fig 46

PRESSURE US. % MOISTURE ,C051 TEMP = 145.

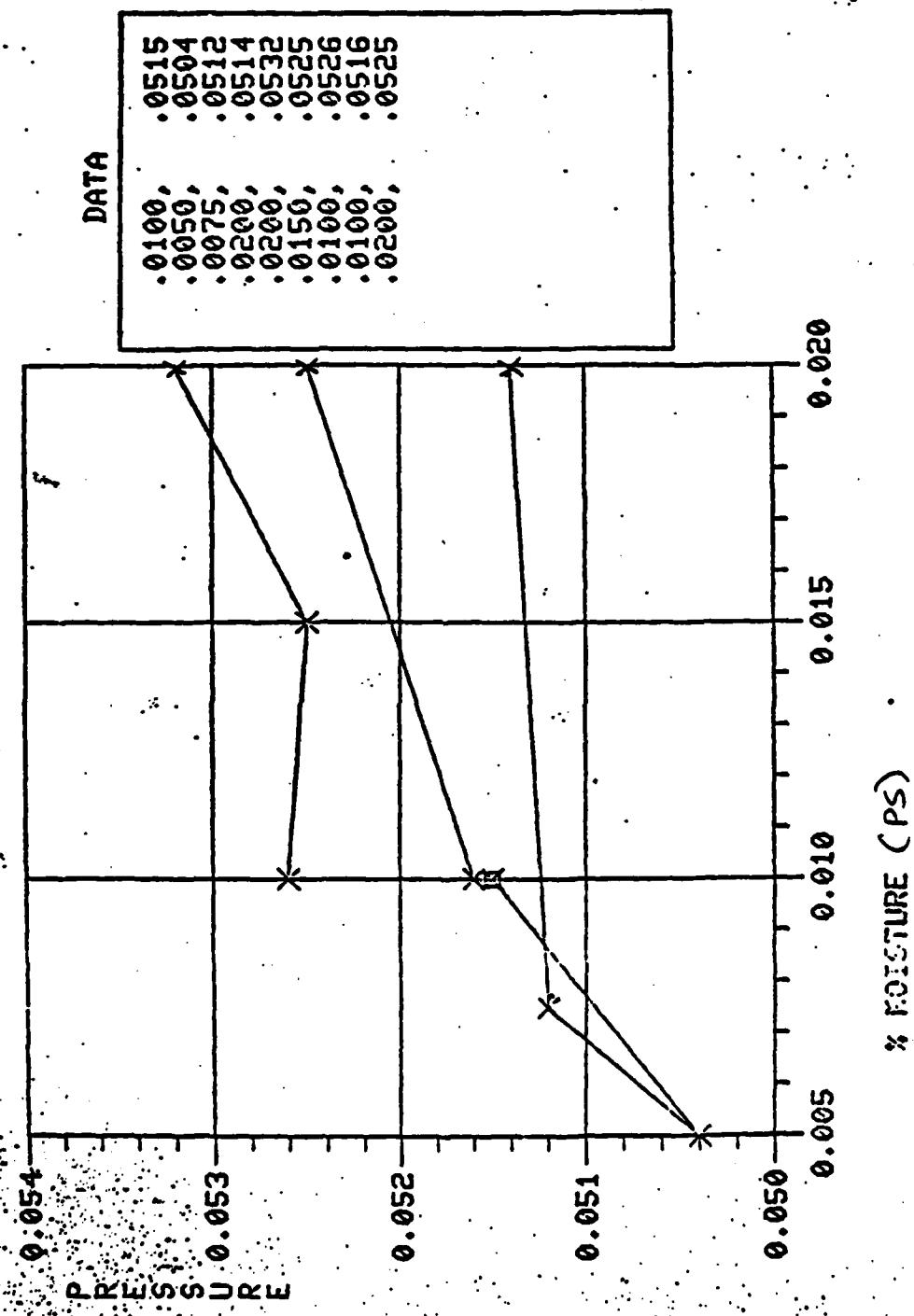


Fig. 47

C051

PRESSURE COEFFICIENT, DP/DT VS. % MOISTURE

TEMP RANGE IS (-65 - 145)°F

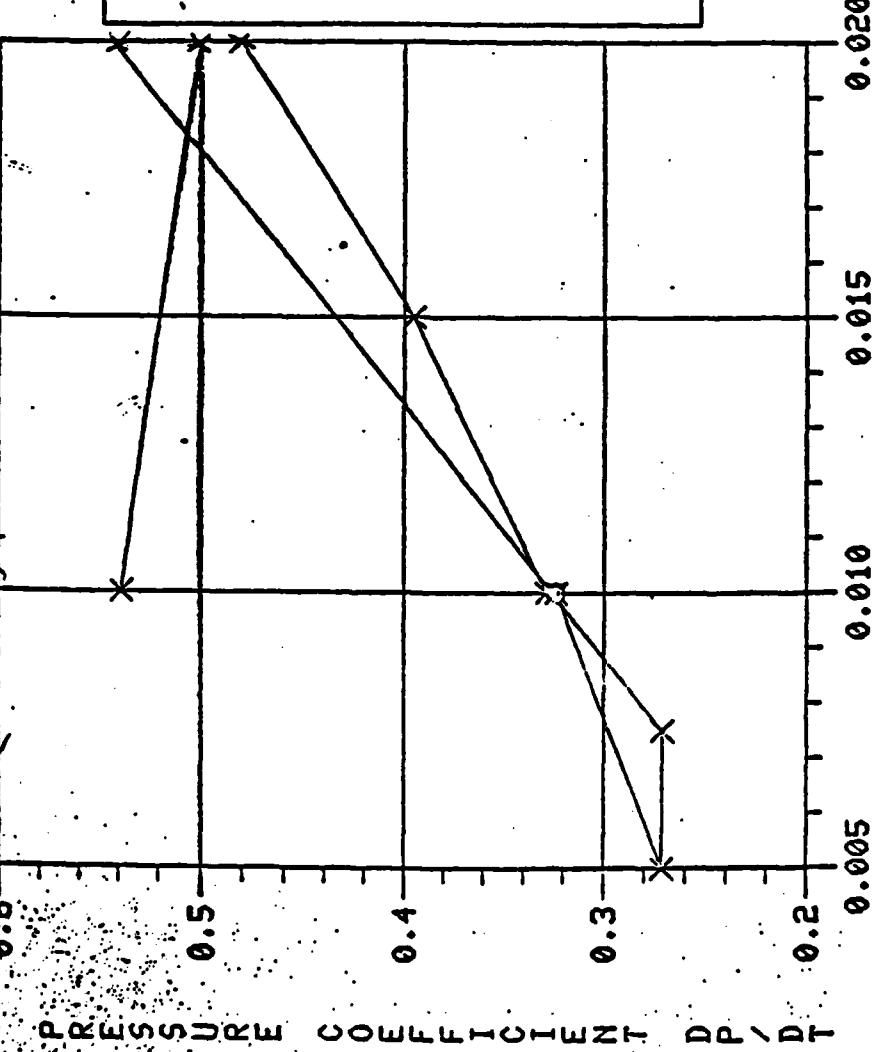


Fig. 48

PRESSURE US. % NITROGLY C102 TEMP = -65.

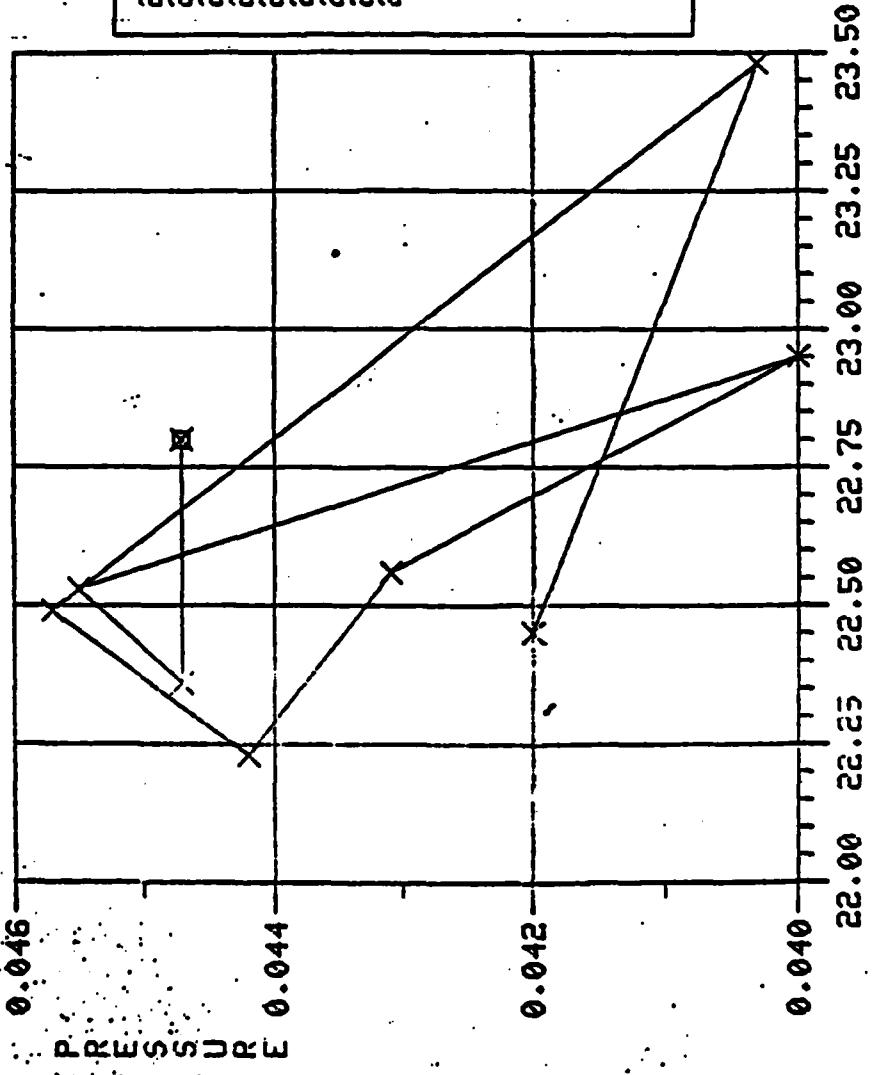


Fig. 49

C102

PRESSURE COEFFICIENT, DP/DT VS. X NITROGLY.

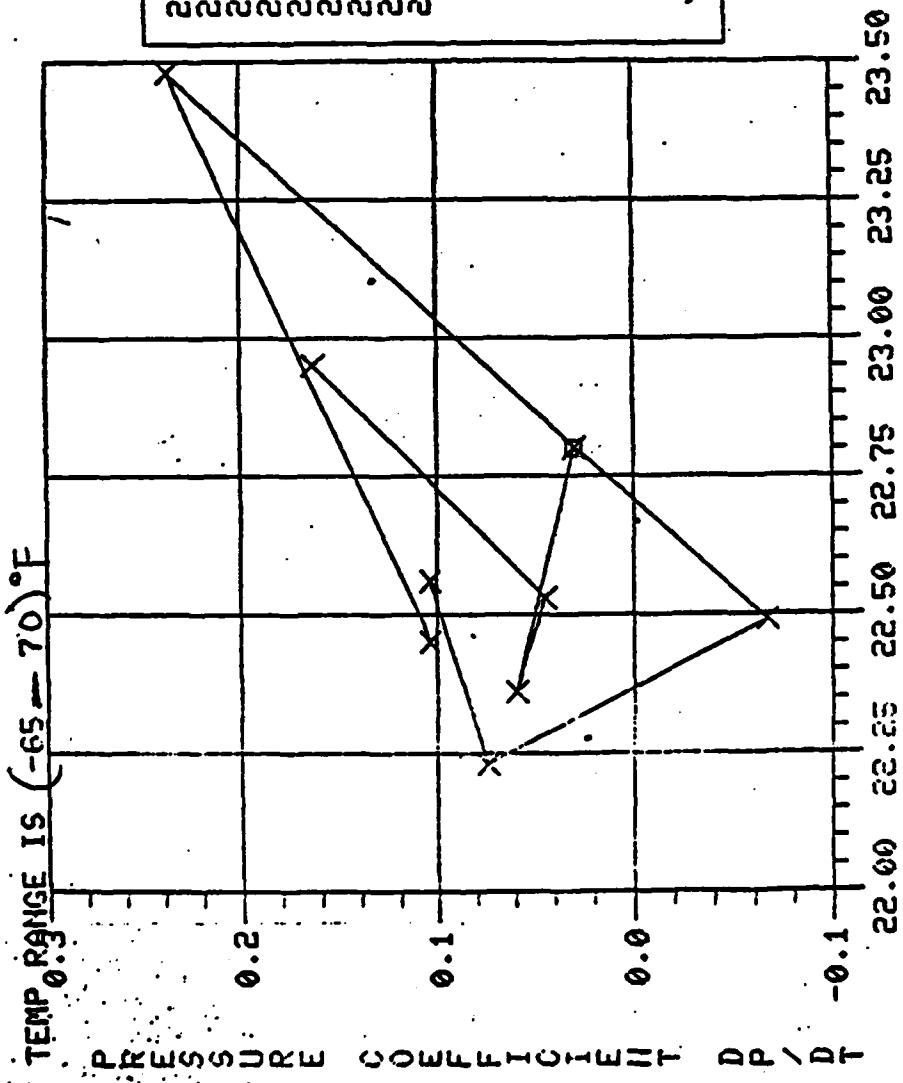


Fig. 59

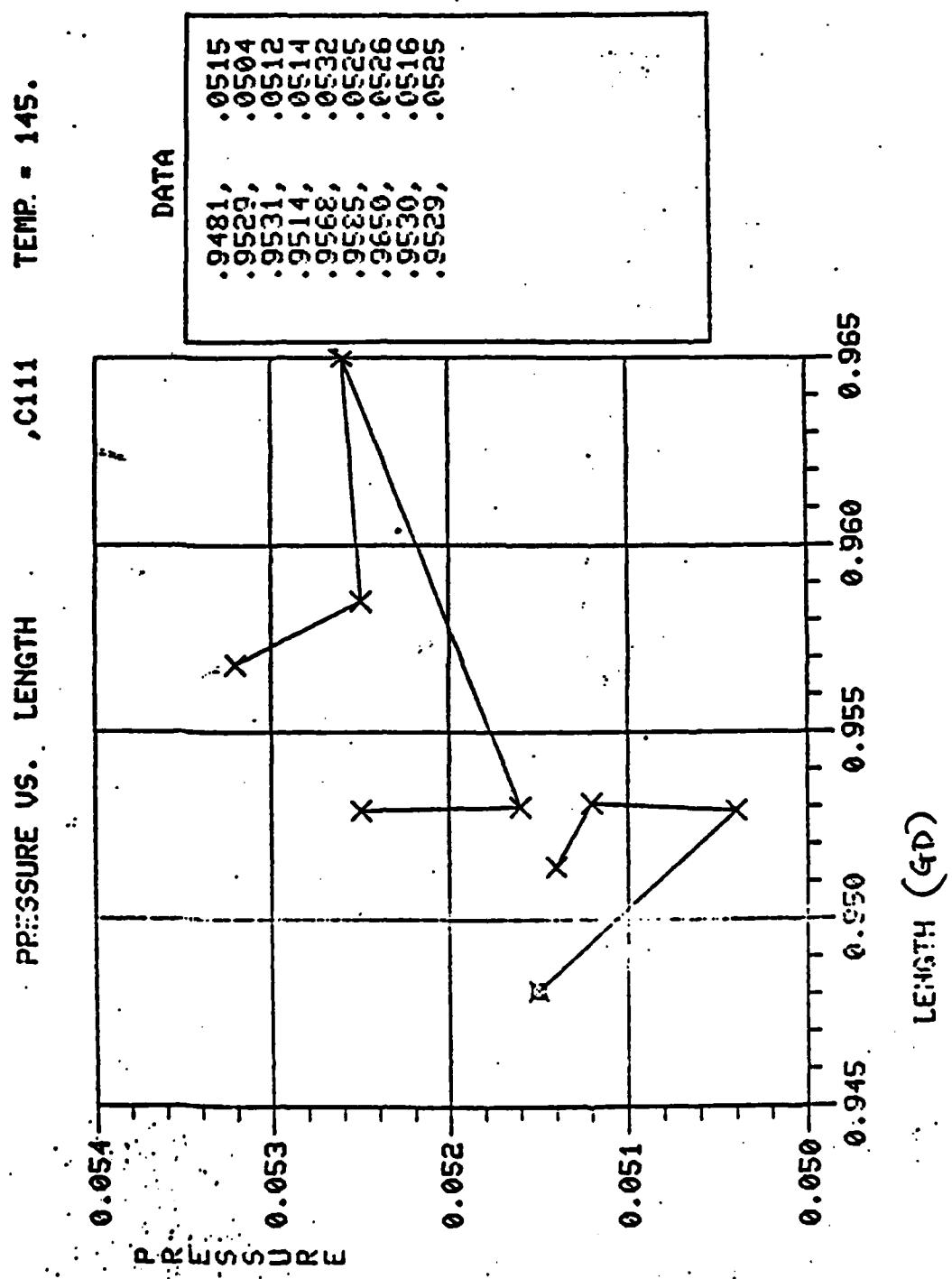


Fig. 51

PRESSURE VS. PERFOR DIAM ,C113 TEMP = -65.

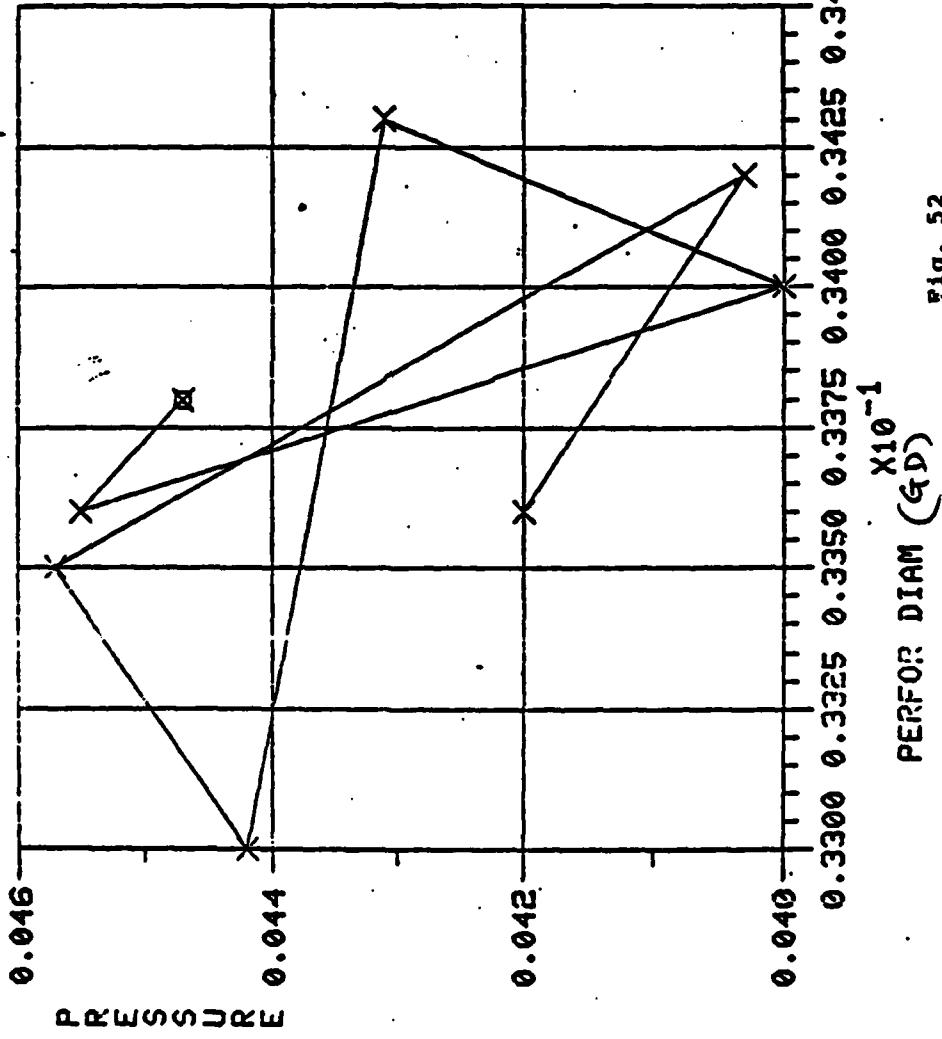


Fig. 52

,C119

PRESSURE COEFFICIENT, DP/DT VS. D/D

TEMP₁ RANGE IS (70.-145)°F

PRESSURE COEFFICIENT DP / DT

DATA

12.4000,	0.8533
12.3000,	0.6533
12.4000,	0.6369
12.2000,	1.2267
12.1000,	1.1669
12.0000,	1.0973
11.9000,	1.0499
11.8000,	1.0899
11.7000,	1.2133

D/D (G/D)

V19. 53

RQ90-RQ-40 USL UNI(GD)

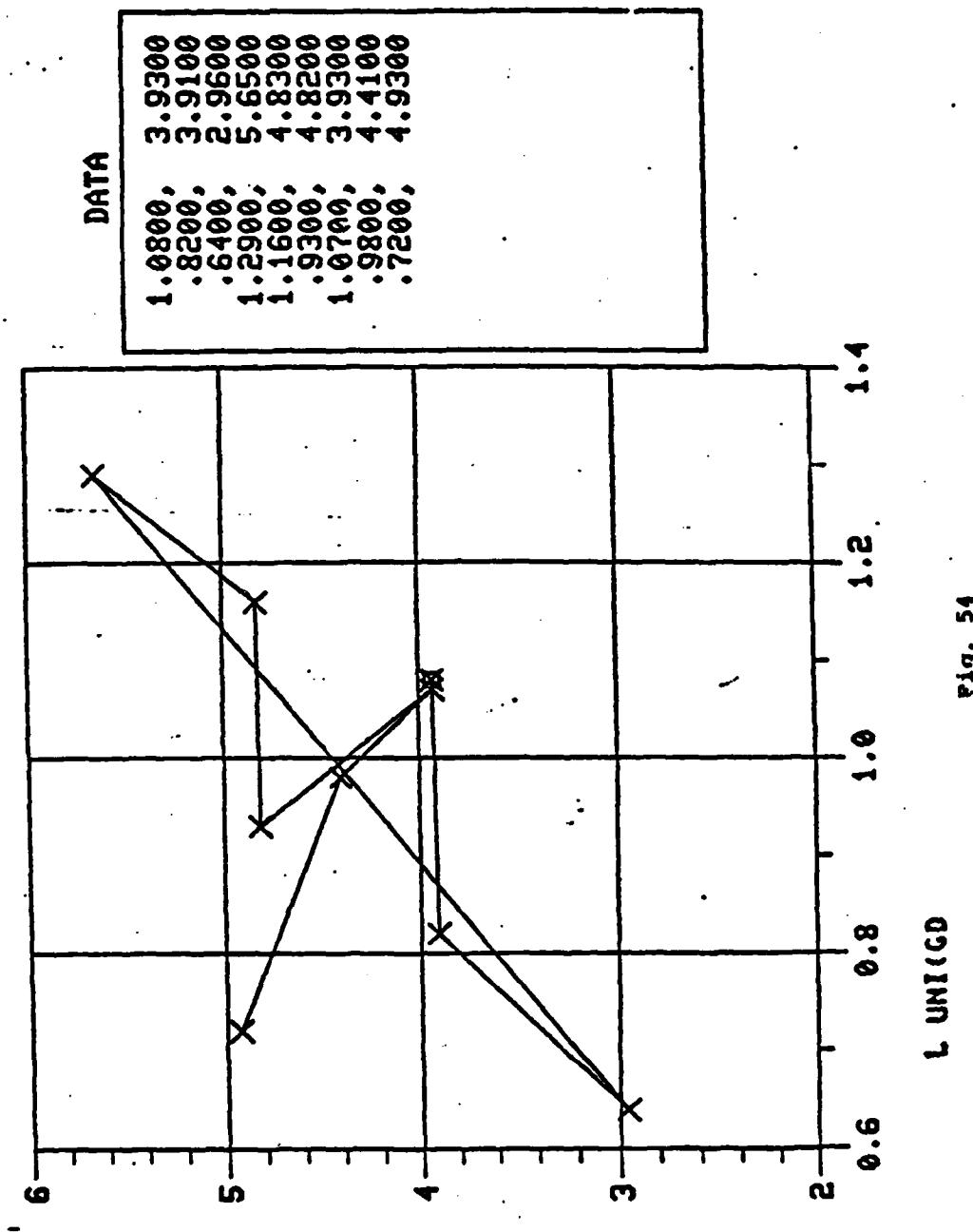


Fig. 54

TEMP = .70.

PRESSURE VS. L UNIFORMITY ,C121

DATA

1.0800,	0.9451
1.8200,	0.9455
6100,	0.9461
1.2900,	0.9462
1.1600,	0.9445
1.9300,	0.9452
1.0700,	0.9443
1.9800,	0.9435
7200,	0.9434

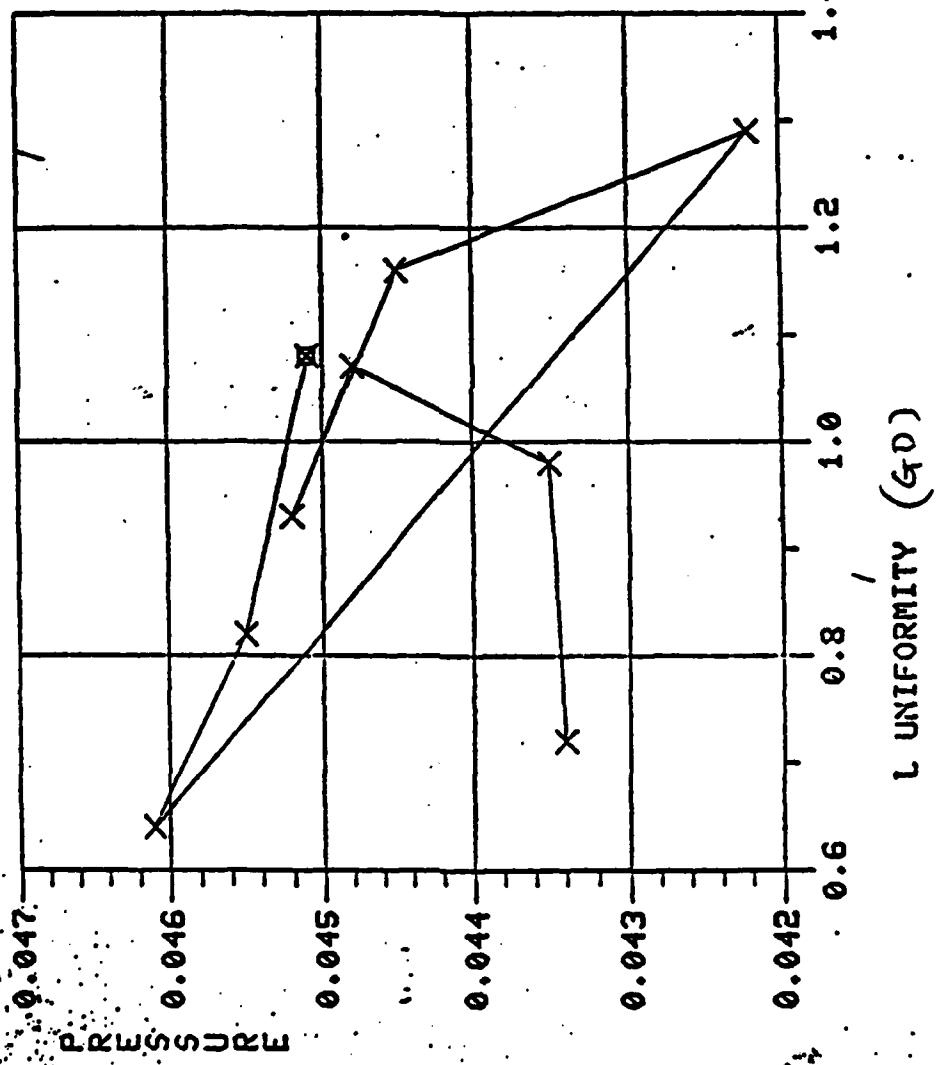


Fig. 55

,C121

PRESSURE COEFFICIENT, DP/DT VS. L UNIFORMITY

TEMP. RANGE IS (70.-145)°F

1

0

-1

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$DP(RAD-T)/DP(RAD-C)_{145-70}$ vs L UNI(GD)

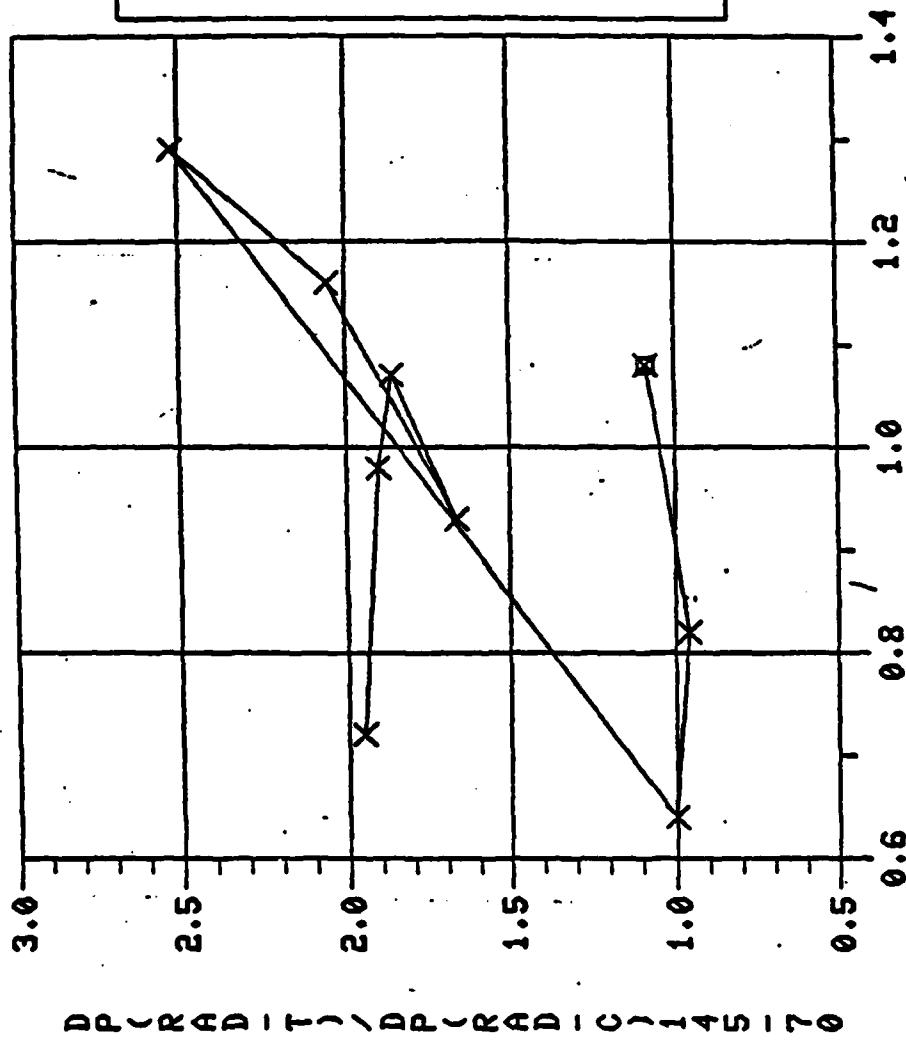


Fig. 57

PRESSURE US. D UNIFORMITY .C122 TEMP = 145.

DATA

1.2800,	.0515
1.2500,	.0504
1.5700,	.0512
1.9500,	.0514
1.1200,	.0532
1.1500,	.0525
1.0100,	.0526
1.5800,	.0516
1.1000,	.0525

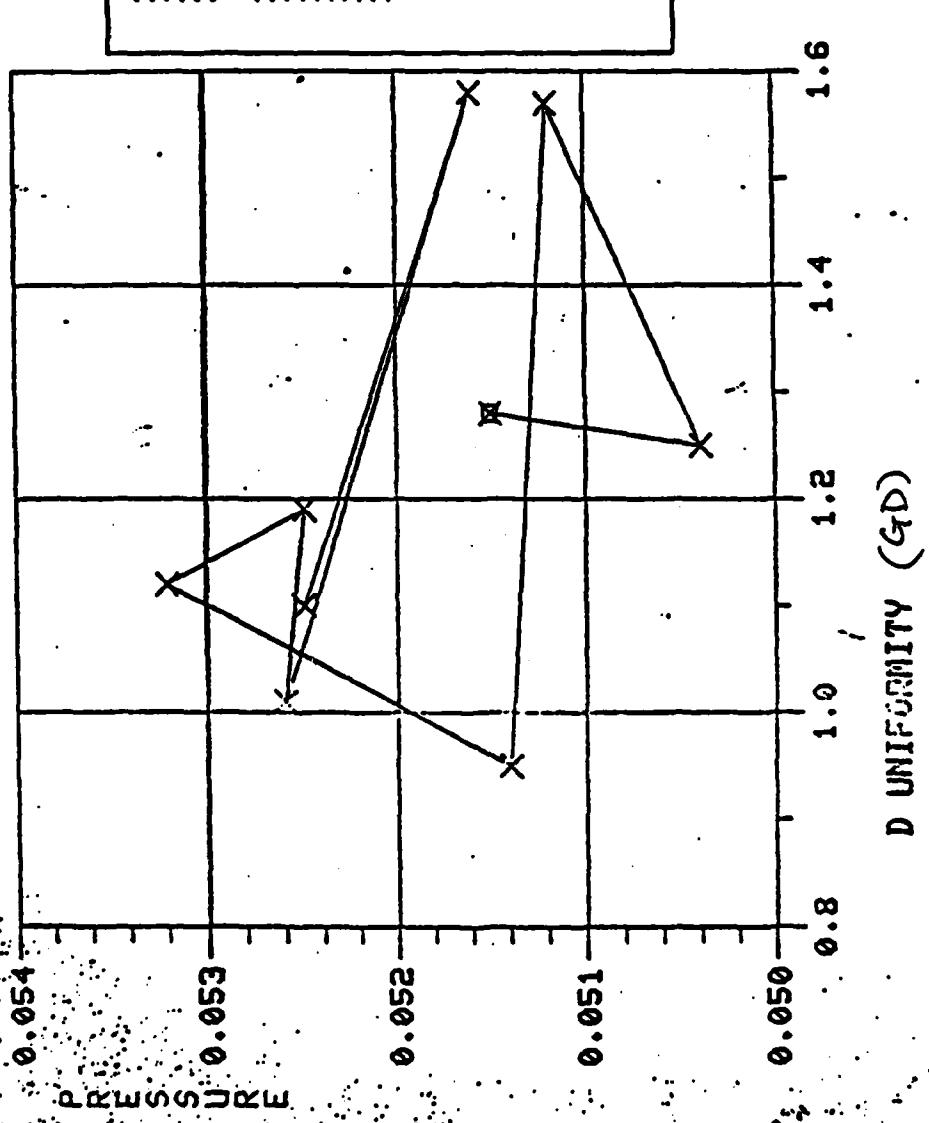


Fig. 59

PRESSURE COEFFICIENT, D_P/D_T VS. D UNIFORMITY

, C122
TEMP. RANGE IS (60.-145)°F

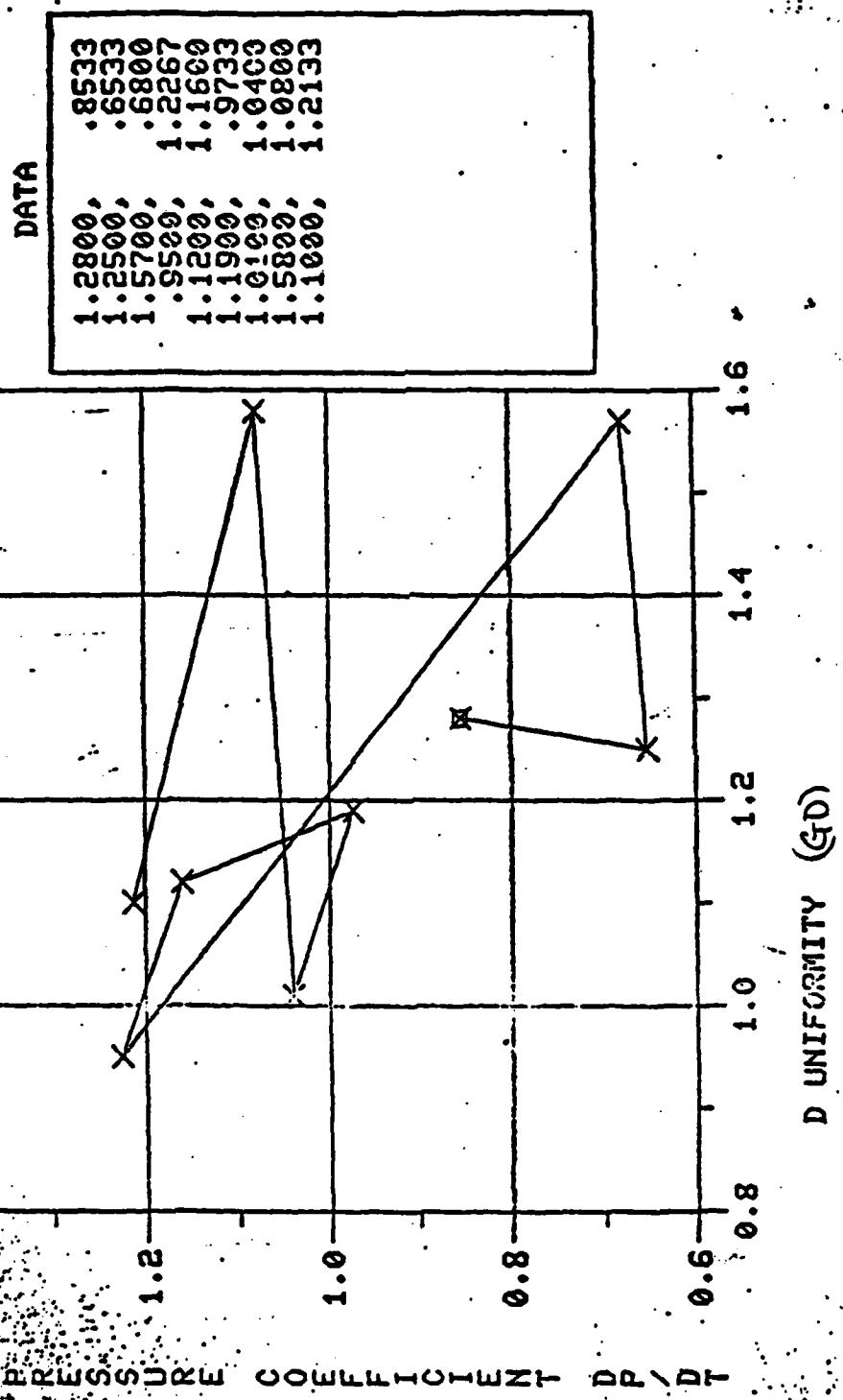
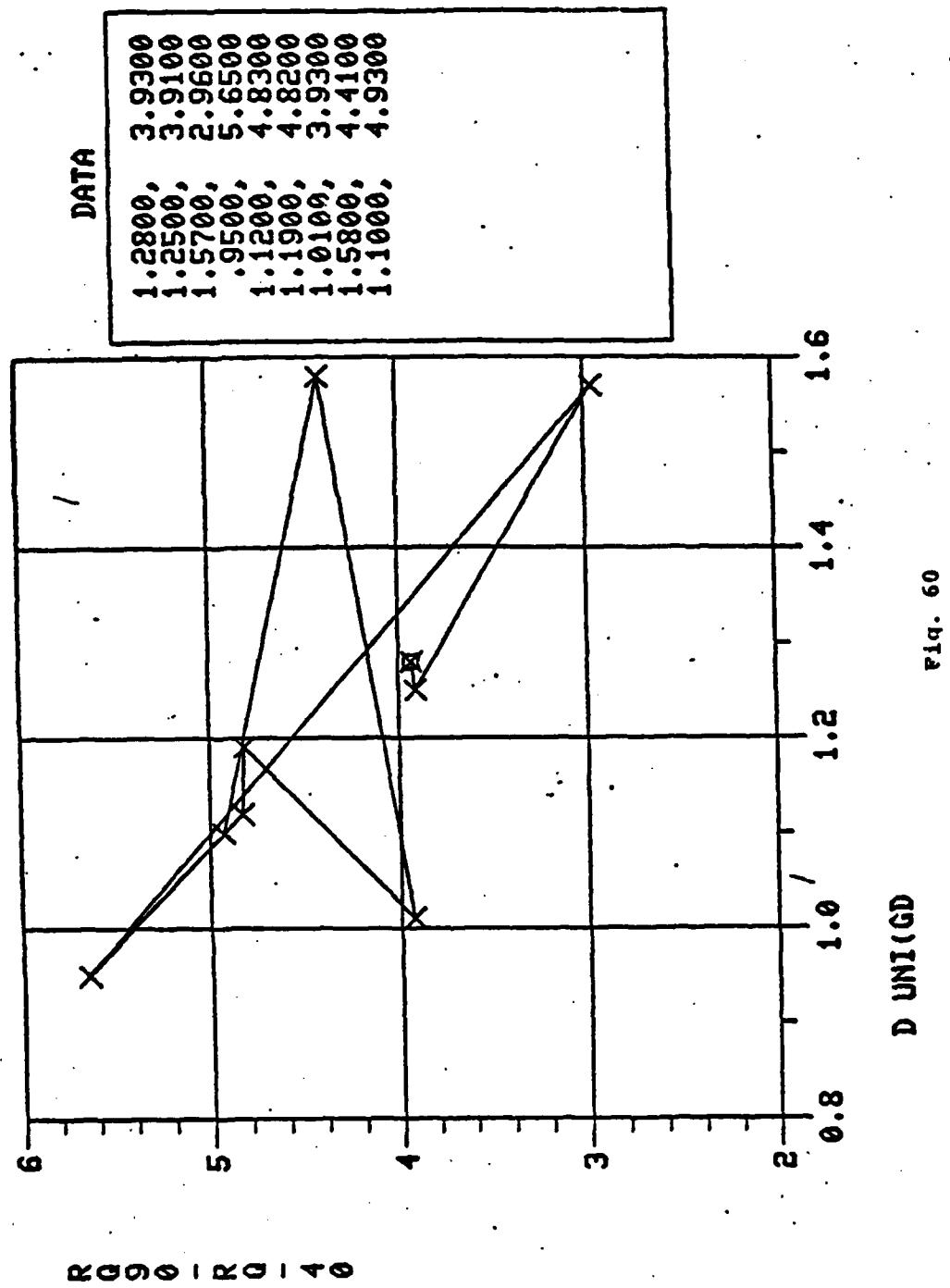


Fig. 59

R090-R0-40 USD UNI(GD)



$DP(RAD-T)/DP(RAD-C)145-70$ VS D UNI(GD)

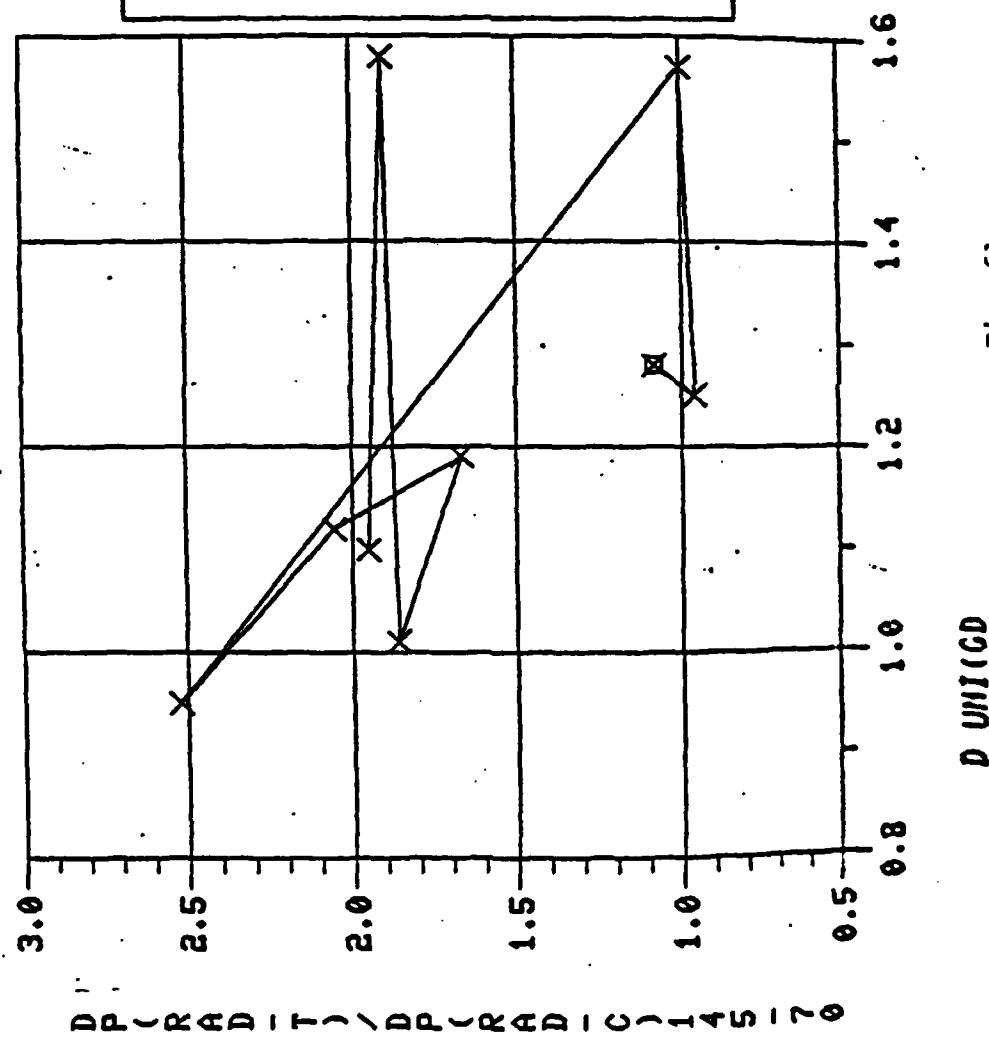


Fig. 61

PRESSURE US. YR(STORAGE NGU) .0191 TEMP = 145.

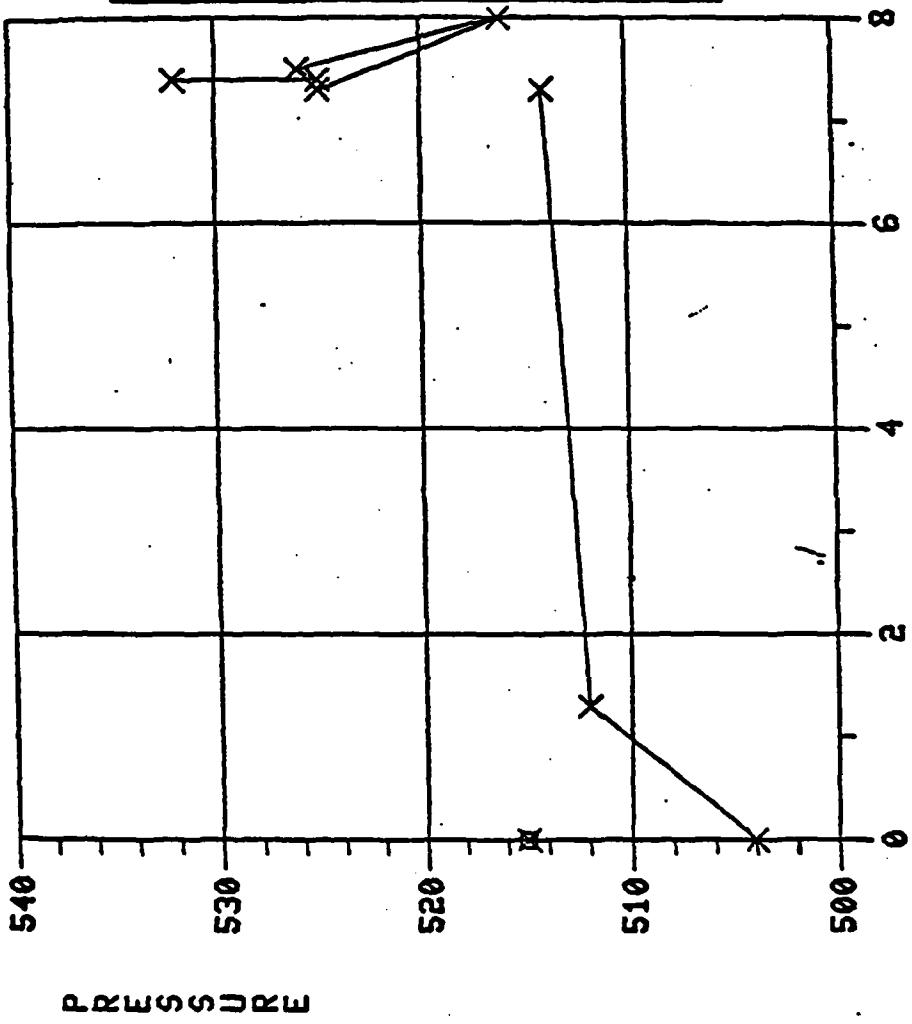
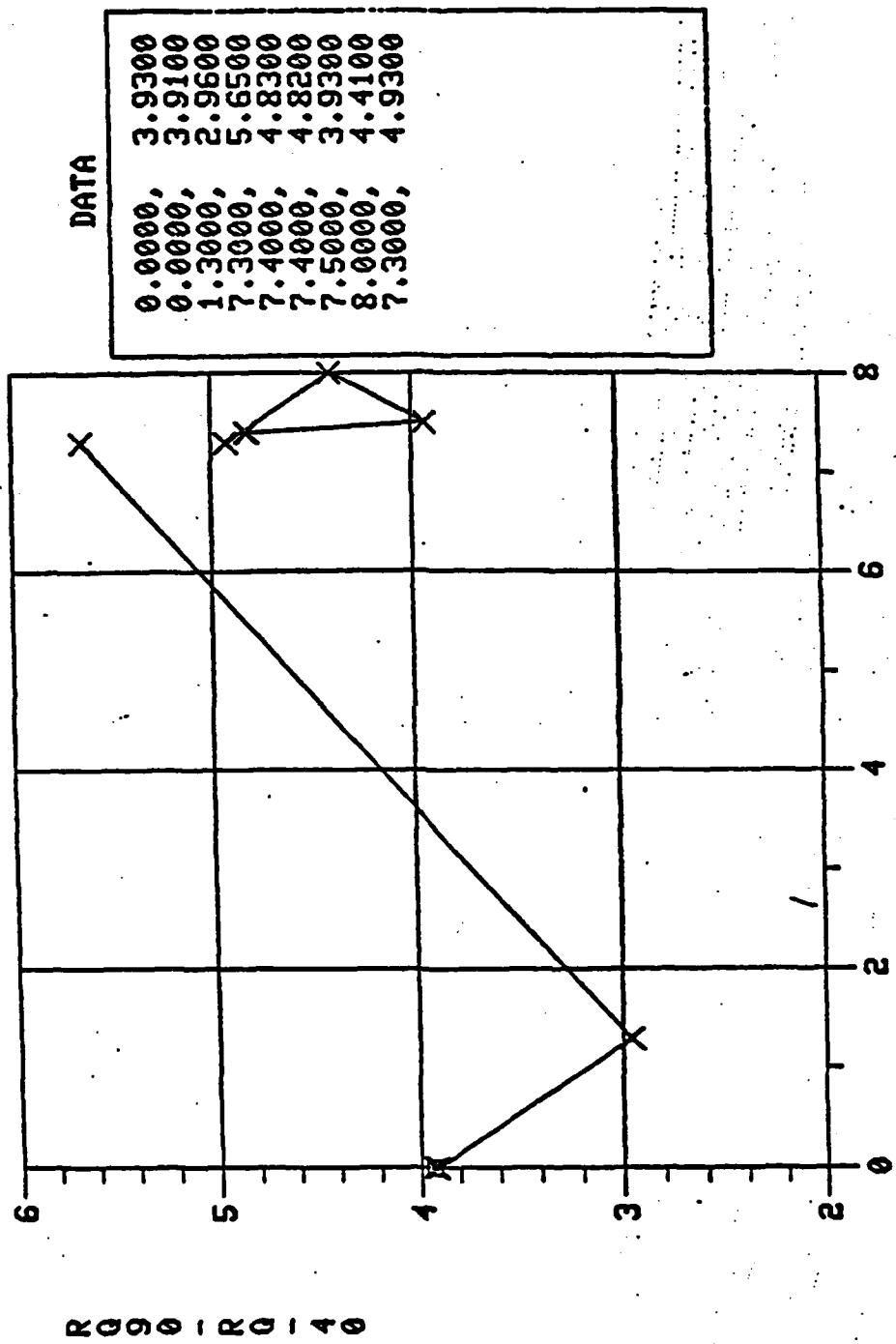


Fig. 62

RQ90-RQ-40 VS YR(STORA)



Appendix 2 = Stepwise Regression Analysis

The regression equation used in this analysis is described as follows:

$$Y = B_0 + B_1 X_1 + B_2 X_2 + \dots + B_i X_i + \epsilon$$

where

Y represents the dependent variable

X_1, X_2, \dots, X_i are the independent variables

B_1, B_2, \dots, B_i are the coefficient constants of the independent variables

ϵ is the random error in each production lots

B_0 is the constant of the equation

The entering independent variables are:

1. % Total volatile (composition)
2. % Graphite (")
3. % Moisture (")
4. pH Value (Nitroguandine)

The entering dependent variables are:

1. Pressure fired at 1450F
2. DP/DT (70 - 145)OF

Table 4
Definition of the regression results:

Parameter	Explanation
R ²	Correlation coefficient; as the R ² approaching 1.0, the equation obtained will explain 100% of the variation about the mean Y
Std Error Est.	Standard error of estimate; STD error approaching to 0.0, the calculated values from the regression equation will be approaching to the actual observed values
F Value	F distribution value is calculated for each entering independent variable. If the calculated F value is equal or greater than the predicted or P value (5.12), the independent variable will be retained in the regression equation; otherwise, the variable will be rejected.

Table 5: Final Result of Stepwise Regression Analysis.

Depend Var (Y)	Indep Vars Entering	Variables / Variables Retain	
		Select	Reject
Pressure (145)°F	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$ $x_4 = \text{ pH}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$ $x_4 = \text{ pH}$
Pressure (145)°F	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$ $x_4 = \text{ pH}$
DP/DR₂ (70 - 145)°F	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$ $x_4 = \text{ pH}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$ $x_4 = \text{ pH}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Graphite}$ $x_3 = \% \text{ Moist}$ $x_4 = \text{ pH}$
DP/DR₂ (70 - 145)°F	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Moist}$ $x_3 = \% \text{ pH}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Moist}$ $x_3 = \% \text{ pH}$	$x_1 = \% \text{ Total Volatile}$ $x_2 = \% \text{ Moist}$ $x_3 = \% \text{ pH}$

Table 5 Continues

Y	Variables retain in regression	R^2 for Retain Var(s)	STD Error Est of Retain Var	Final Regression Equation	
				P Value	P Value
$X_4 = \text{pH}$	$X_4 - X$ Total Volatile	0.6935	5.183	less than 5.12	less than 5.12
Pressure (145°F)	$X_1 - X$ Total Volatile	0.6346	5.659	less than 5.12	less than 5.12
DP/dT2 (70-145)°F	$X_2 - X$ Graphite	0.815	0.0993	30.9035	Y= 1.619-8.49X ₂
DP/dT2 (70-145)°F	$X_1 - X$ Total Volatile $X_3 - X$ total	0.8758	0.088	16.20 less than 5.12	Y= 0.81-0.8X ₁ +24.8X ₃

APPENDIX 3: MANUFACTURING DATA OF M30A1 propellant

Graph showing Current (mA) vs. Voltage (V) for various diodes.

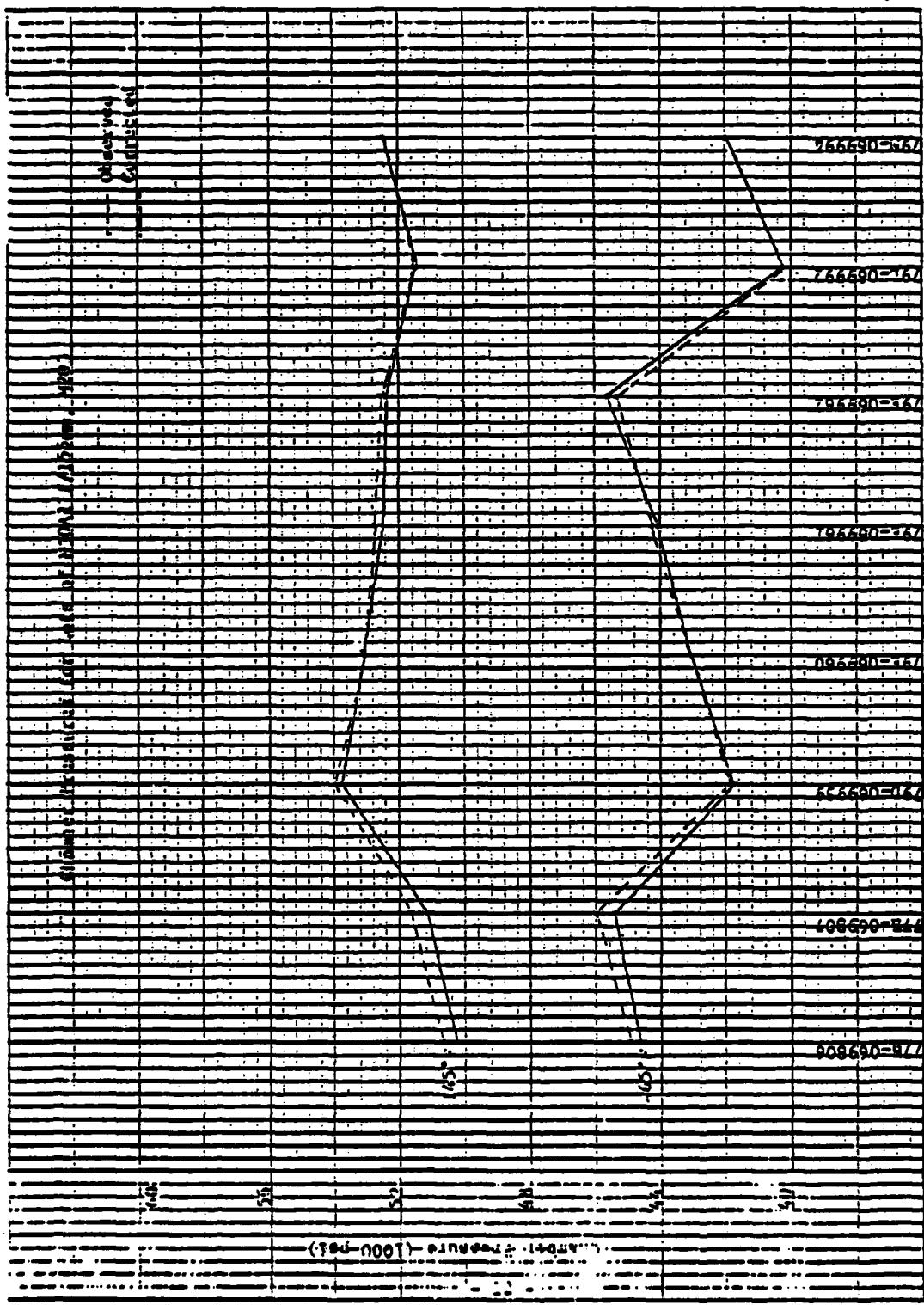
Y-axis: Voltage (V)

X-axis: Current (mA)

Curves:

- 756690-167
- 756690-168
- 756690-169
- 096690-167
- 096690-168
- 108690-167

Chamber - Production - Test & Technical - 1000 Series



HJOMI Propellant for 155mm, M201 Source of Ingredients

Ingredient	69805	69806	69807	69959	69960	69961	69962	69992	69994
Nitrocellulose	Hercules RAAP	Same	Same	Same	Same	Same	Same	Same	Same
Nitroglycerin	Hercules RAAP	Same	Same	Same	Same	Same	Same	Same	Same
Nitroguanidine	CFH Cyanimid' of Canada Ltd. (Shipper)	Same	CFH Cyanimid' of Canada Ltd. (Shipper)	CFH Cyanimid' Ravenna (Shipper)	CFH Cyanimid' Ravenna (Shipper)	Same	Same	Same	Same
Ethyl Centralite	Chemische Werke Low West Germany	Same	Same	Van de Hark New York	Same	Same	Same	Same	Same
Potassium Sulfate	CFH Naval Ammunition Depot Crane, Ind. (Shipper)	Same	Same	Same	Same	Same	Same	Mallinckrodt, Inc.	Same
Graphite	Joseph Dixon Crucible Company	Same	Same	Same	Same	Same	Same	Same	Same

NITROCELLULOSE
H30Al f/1558H, H2O3 Propellant

Loy. No.	N. C. Blown	Percent <u>N₂</u>	Ether-Alcohol Solubility Percent	Fineness <u>HL</u>	KI Starch Time/Hr.	Cetene Time/Min	Acetones Insol. Percent	Ash Percent	Vis Sec.	Freeness <u>HL</u>
TAU77C-069805	C35,556	12.58	99+	84	N/A	30	"	N/A	12	502
	557	12.59	"	86	45+	30+	"	.04	13	480
	558	12.60	"	86	"	30	"	.06	9	486
	565	12.53	"	90	"	30+	"	.05	14	522
	566	12.52	"	90	"	30+	"	N/A	14	512
	570	12.59	"	90	N/A	30+	"	N/A	14	512
	573	12.62	"	82	N/A	30+	"	N/A	13	453
	576	12.58	"	74	N/A	30	"	N/A	11	507
	577	12.50	"	82	N/A	30	"	N/A	11	510
	579	12.56	"	92	45+	30+	"	.02	10	467
TAU77B-069806	C35,571	12.61	"	88	45+	30+	"	.03	10	470
	572	12.59	"	88	N/A	30+	"	N/A	14	490
	573	12.60	"	82	N/A	30+	"	N/A	13	453
	579	12.56	"	82	45+	30+	"	.02	10	467
	581	12.51	"	88	N/A	30	"	N/A	11	507
	583	12.52	"	78	45+	30+	"	.15	13	501
	585	12.55	"	82	N/A	30	"	N/A	13	515
	586	12.50	"	79	45+	30+	"	.05	14	483
	591	12.60	"	94	N/A	30	"	N/A	14	451
	592	12.60	"	94	45+	30	"	.04	19	482
MIL77B-069807	C35,591	12.60	"	94	N/A	30	"	N/A	14	451
	592	12.60	"	94	45+	30	"	.04	19	482
	593	12.61	"	94	N/A	30	"	N/A	19	491
	594	12.59	"	92	45+	30	"	.04	17	487
	598	12.52	"	86	N/A	30	"	N/A	10	502
	603	12.56	"	76	45+	30	"	.04	11	485
	604	12.57	"	78	N/A	30	"	N/A	9	502
	607	12.57	"	80	N/A	30+	"	N/A	10	480
	610	12.56	"	82	N/A	30	"	N/A	11	519
	611	12.55	"	86	N/A	30+	"	N/A	11	479

NITROCELLULOSE
H30A1 F/15584, H203 Propellant

Lot No.	W. C. Blend	Percent N_2	Ether-Alcohol Solubility Percent	Fineness ML	KI Starch Time/Min.	Gelatin Time/Hr.	Acetones Insol. Percent	Ash Percent	Vis Sec.	Fineness ML
					99 min	35' min.	30' min.	0.4 max	0.4 max	
Requirements										
HLL-H-244A		12.6 ± 0.10	99 min	--						
RAD790-069959	C36,275	12.59	99+	94	45+	30	TR	.01	13	498
	277	12.55	"	94	45+	30+	"	.02	13	556
	281	12.62	"	96	45+	30	"	.03	13	480
	284	12.66	"	92	45+	30+	"	.01	14	534
	286	12.62	"	92	45+	30	"	.03	13	523
85										
RAD79E-069960	C36,275	12.59	"	94	45+	30	"	.01	13	498
	277	12.55	"	94	45+	30+	"	.02	13	556
	281	12.62	"	96	45+	30	"	.03	13	480
	286	12.62	"	92	45+	30	"	.03	13	523
	290	12.62	"	90	45+	30	"	.02	15	547
	291	12.63	"	98	45+	30+	"	.03	17	503
	294	12.64	"	92	45+	30+	"	.02	19	510
	300	12.59	"	88	45+	30	"	.04	16	515
	302	12.62	"	92	45+	30+	"	.04	15	527
	303	12.63	"	94	45+	30+	"	.03	15	500
315										
RAD79E-069961	C36,102	12.62	"	92	45+	30+	"	.04	15	527
	303	12.63	"	94	45+	30+	"	.03	15	500
	305	12.70	"	90	45+	30+	"	.05	15	455
	306	12.62	"	94	45+	30+	"	.04	13	487
	307	12.60	"	94	45+	30+	"	.06	15	480
	308	12.66	"	94	45+	30	"	.02	16	450
	311	12.69	"	95	45+	30	"	.04	15	496
	312	12.69	"	95	45+	30+	"	.02	13	504
	313	12.60	"	86	45+	30	"	.01	12	498
	314	12.60	"	86	45+	30+	"	.04	12	518
	315	12.67	"	92	45+	30	"	.04	13	492

NITROCELLULOSE
H30A1 f/155mm, H203 Propellant

Lab No.	N. C. Blend	Percent N ₂	Ether-Alcohol Solubility Percent	Fineness H.L.	Kl Starch		Acetone Insol. Percent	Ash Percent	Vis Sec.	Freeness H.L.
					35' min	30' min				
R&D79E-069962	C36,317	12.69	99+	92	45+	30	TR	.02	11	476
	318	12.69	"	82	45+	30	"	.02	13	488
	319	12.68	"	94	45+	30	"	.01	15	505
	320	12.65	"	94	45+	30	"	.05	17	472
	321	12.65	"	90	45+	30	"	.01	15	525
	322	12.66	"	90	45+	30	"	.03	11	450
	323	12.65	"	84	45+	30	"	.05	12	467
	325	12.61	"	84	45+	30	"	.02	10	485
	327	12.60	"	86	45+	30	"	.02	10	480
86	328	12.61	"	86	45+	30	"	.06	10	496
R&D79L-069992	C36,423	12.53	"	90	45+	30	"	.04	11	482
	426	12.53	"	98	45+	30	"	.04	12	470
	433	12.60	"	76	45+	30+	"	.02	16	536
	434	12.59	"	78	45+	30+	"	.03	9	529
	436	12.58	"	78	45+	30+	"	.03	11	492
	440	12.53	"	82	45+	30+	"	.03	10	490
	444	12.55	"	70	45+	30+	"	.03	8	465
R&D79L-069994	C36,436	12.58	"	78	45+	30+	"	.01	11	492
	437	12.61	"	76	45+	30+	"	.02	9	498
	418	12.58	"	76	45+	30+	"	.02	10	539
	440	12.53	"	82	45+	30+	"	.03	10	490
	442	12.62	"	78	45+	30+	"	.02	9	458
	444	12.55	"	70	45+	30+	"	.01	8	465
	445	12.52	"	78	45+	30+	"	.02	9	501
	450	12.56	"	82	45+	30+	"	.02	9	462
	452	12.58	"	72	45+	30	"	.03	9	473

NITROCNGENIN
H3OAI f/155M, H2O3 PROPELLANT

<u>Lot No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alk.</u>	<u>Acidity</u>	<u>H₂O</u>	<u>N₂</u>
Requirements		10 min	0.0022 Max		0.5% Max	18.40% Min
HLL-N-2468						
RAD77G-69805	149, 151	15				
	154, 155	15				
	168, 171	15				
	166, 162	15				
	169, 163	15				
	164, 159, 158	15				
	170-	15	None		.38	18.45
	178, 173	15				
	172, 179	15				
	174, 175	15				
	176, 186	15				
	185, 183	15				
	182, 181	15				
	180-	15	None		.34	18.44
	2, 1, 4	15				
	13, 12, 6	15				
	5, 11, 8	15				
	7, 15	15				
	20-	15	None		.22	18.45
	19, 17	15				
	21	15				
	16, 14, 10-	15				

NITROGLYCERIN
H30A1 f/153KH, H203 PROPELLANT

<u>Lot No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alk.</u>	<u>Acidity</u>	<u>H₂O</u>	<u>N₂</u>
Requirements HLL-N-2468		10 min	0.002% Max	0.5% Max	18.40% Min	
MAD77C-69805 (Cont'd)	9, 33, 32 28, 27, 23 18, 26, 25 24, 22, 36, 21	15 15 15 15				
RAD77H-069806	37, 42, 46 40- 45, 44, 48 47, 51, 52 58, 56, 53 55, 39, 38 38, 41, 54 61, 62, 68 67, 71 60-	15 15 15 15 15 15 15 15 15 15				
	59, 61, 64 78, 69, 70- 79, 73, 75 77, 74, 85 86, 87, 94 84, 82, 81, 80- 76, 88, 72	15 15 15 15 15 15 15	None	None	.35	18.45

NITROGLYCERIN
H30A1 f/155MM, H203 PROPELLANT

<u>Lut. No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alk.</u>	<u>Aeridity</u>	<u>H₂O</u>	<u>N₂</u>
Requirements		10 min	0.0022 Max		0.52 Max	16.40% Min
HIL-H-2468						
RAD77H-069807	91, 92, 98	15				
	99, 93, 96	15				
	115, 114, 109	15				
	107, 108, 106	15				
100-	15		None		.25	16.46
	95, 102, 103	15				
110	15		None		.35	16.48
	111, 101, 113	15				
	116, 117, 118	15				
	119, 121, 127	15				
	122, 120-, 126	15				
	126, 132, 126	15				
	146, 150-, 149	15				
	144, 147, 148	15				
	143, 142, 141	15				
	116, 115, 119	15				
140-	15		None		.36	16.46
	138, 134, 130	15				
	131, 129, 133	15				

NITROGLYCERIN
H3OAI f/155MH, H2O3 PROPELLANT

<u>Lot No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alk.</u>	<u>Acidity</u>	<u>H₂O</u>	<u>H₂</u>
<u>Requirements</u>		<u>10 Min.</u>	<u>0.0022 Max</u>	<u>0.5 X Max</u>	<u>10.40% Min</u>	
RAD79D-069959	39	17	—	—	.28	16.43
	40	17	—	—	—	—
	41	—	—	—	—	—
	42	17	—	—	—	—
	43	—	—	—	—	—
	44	16	—	—	—	—
	45	17	—	—	—	—
	46	17	—	—	—	—
	47	15	—	—	—	—
RAD79E-069960	49	—	—	—	—	—
	51	16	—	—	—	—
	52	16	—	—	—	—
	53	—	—	—	—	—
	54	16	—	—	—	—
	55	17	—	—	—	—
	56	—	—	—	—	—
	57	16	—	—	—	—
	58	17	—	—	—	—
	59	16	—	—	—	—
	60	—	—	—	—	—
	61	16	—	—	—	—

MCA1 1/15504, M203 PROPELLANT
NITROGLYCERIN

Charge No.	XL (Min.)	Alk.	Acidity	H ₂ O	H ₂ -	0.5% Max	0.5% Min
MAU795-069960 (Initial d)	1, 2	17					
	3	16					
	4, 5, 6	17					
	7, 8, 9, 10	17					
	11	16					
	12, 13, 14	17					
	15	16					
	16	17					
	17	--					
	18	16					
	19	15					
	20	--					
	21	15					
	23	17					
	25	16					
	26	15					
	27, 28	17					
	29	18					
	30, 31, 32	17					
	33, 34,	17					
	35, 36	16					
	37, 38, 39	17					

MATERIALS AND METHODS

<u>Part No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Altus.</u>	<u>Acidity</u>	<u>H₂O</u>	<u>N₂</u>	<u>0.5% Max</u>	<u>10.40% Min</u>
Requirements		10 Min	0.002% Max					

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H30A1 F/155MM, H203 PROPELLANT

<u>Lot No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alka.</u>	<u>Acidity</u>	<u>H₂O</u>	<u>H₂S</u>
Requirements		10 Min.	0.002% Max	0.5% Max	10.40% Min	
RHIL-N-216B						
RAD79E069962 (Cont'd)	9	--				
	10	17				
	11	16				
	12	17				
	13	15				
	14	--				
	15	18				
	16	16				
	17	19				
	18	17				
	19	16				
	20	16				
	21	17				
	22	16				
	23	--				
	24	17				
	25	15				
	26	--				
	27	16				

**NITROGLYCERIN
H2O2 6/155GM, H2O2 PROPELLANT**

<u>Lot No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alka.</u>	<u>Ae1415X</u>	<u>H-Q</u>	<u>0.5X Max</u>	<u>H2-</u>	<u>18.40% Max</u>
Requirements								
HIL-N-2468								
NAU79L-069992	17	16						
	18	15						
	19, 20, 21	17						
	23	--						
	24	16						
	25	17						
	26, 27	19						
	28	--						
	29	18						
	30-	17						
	31	17						
	32	--						
	1, 2, 3	17						
	4	18						
NAU79L-069994	5, 6	16						
	7, 8	--						
	9	16						
	10	17						
	11, 12	17						
	13, 14	16						
	15	--						

NITROGLYCERIN
H3041 6/1558N, H203 PROPELLANT

<u>Lot No.</u>	<u>Charge No.</u>	<u>KI (Min.)</u>	<u>Alka.</u>	<u>Acidity</u>	<u>H₂O</u>	<u>N₂</u>
		10 Min	0.0022 Max		0.5% Max	10.40% Max
MAD79H-069994 (Cont'd)	16, 17, 18	17				
	19	17				
	20	--	None		.36	10.47
	21, 22, 23	17				
	24	17				
	25	--				
	26, 27, 28	17				

Instrumentation
ANAL Freelite 6/152m, N202

Propellant Lot No. Batch Lot No. (WPC No.) CCL-Lot No. (WPC. Lot No.)	770-000002						770-000003					
	12-012	12-014	12-012	12-014	12-012	12-014	12-012	12-014	12-012	12-014	12-012	12-014
<u>Percentages</u>												1329
Limits												
Avg. Particle Size..	2.4 - 6.0	3.3	3.3	4.7	4.6	4.7	—	3.3	4.9	5.9	5.1	4.3
Purity, %	99.0 min	99.0	99.0	99.0	99.0	99.0	—	99.0	99.0	99.0	99.0	99.0
Ash Content, %	0.30 max	0.03	0.03	0.02	0.03	0.02	—	0.04	0.02	0.02	0.05	0.09
pH Value	4.5 - 7.0	5.0	3.4	3.0	3.7	3.0	—	3.9	3.2	3.4	3.1	4.7
Acidity (H ₂ SO ₄ Eq), %	0.04 max	0.01	0.01	0.02	0.01	0.01	—	0.02	0.01	0.01	0.01	0.01
Total Volatiles, %	0.35 max	0.06	0.09	0.06	0.09	0.06	—	0.09	0.13	0.10	0.06	0.14
Sulfates (Na ₂ SO ₄ Eq), %	0.20 max	0.03	0.03	0.02	0.04	0.04	—	0.03	0.04	0.04	0.06	0.12
Water	0.20 max	0.03	0.01	0.04	0.02	0.02	—	0.05	0.02	0.03	0.03	0.04
Insolubles, %	—	—	—	—	—	—	—	—	—	—	—	—
SOURCE:	Summary of Chemica - DIRECT											
No/yr of Manufacture	3/77	3/77	3/77	3/77	3/77	3/77	3/77	3/77	3/77	3/77	3/77	3/77
No/yr Received at NSAP	4/77	4/77	4/77	4/77	4/77	4/77	4/77	4/77	4/77	4/77	4/77	4/77

96

Attachment 6
Page 1 of 18

NITROGENATING
112041 Present 1/13/2001, 11:01

Proprietary Lot No. MAP Lot (ARC No.) CCR-Lot No. (HFG, Lot No.)	112-015025			112-015026			112-015027			112-015028			112-015029		
	11-001	11-002	11-003	11-001	11-002	11-003	11-001	11-002	11-003	11-001	11-002	11-003	11-001	11-002	11-003
<u>Parameters</u>															
Av. Particle Size,	3.4 ~ 6.0	3.4	4.0	4.0	4.0	4.0	—	—	—	4.4	5.3	5.6	3.6	3.6	3.3
Parity, I	99.0 min	99.7	99.8	99.9	99.9	99.9	—	—	—	99.7	99.7	99.7	99.6	99.6	99.1
Ash Content, I	0.20 max	0.03	0.01	0.02	0.03	0.05	—	—	—	0.09	0.06	0.07	0.09	0.02	0.01
pH Value	4.5 ~ 7.0	5.0	5.4	5.1	5.1	5.0	—	—	—	5.4	5.1	5.4	5.2	5.2	—
Acidity, % (H ₂ SO ₄ /Eq), I	0.06 max	0.02	0.01	0.01	0.01	0.02	—	—	—	0.01	0.02	0.01	0.02	0.01	—
Total Volatile, I	0.25 max	0.09	0.07	0.06	0.06	0.07	—	—	—	0.08	0.10	0.05	0.03	0.07	—
Sulfate (Ba ₂ SO ₄ /Eq), I	0.20 max	0.03	0.02	0.02	0.02	0.03	—	—	—	0.03	0.03	0.03	0.03	0.03	0.07
Water	0.20 max	0.15	0.02	0.01	0.01	0.04	—	—	—	0.05	0.04	0.04	0.01	0.01	0.04
Insoluble, I	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
<u>Source</u>															
No/Tr. of Batches	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77
No/Tr. Received at RAAP	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77
<u>STANDARD OF COMPLIANCE - DIRECT</u>															
No/Tr. of Batches	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77
No/Tr. Received at RAAP	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77

NITROSCAMANDINE
REPORT PREPARED 7/13/58 - 9201

Propellant Lot No. BAP Lot (NRC No.) CCL-Lot No. (NLR-Lot No.)	720-059003			720-059004			720-059005			720-059006		
	12-903	12-904	12-907	12-908	12-909	12-910	12-902	12-903	12-904	12-905	12-906	
PERCENTAGE												
Avg. Particle Size.	2.4 - 6.0	4.0	4.3	4.2	4.3	4.2	—	4.2	4.7	4.3	4.9	4.1
Perity, %	99.0 min	99.7	99.0	99.7	99.7	—	—	99.6	99.7	99.7	99.7	99.8
Ash Content, %	0.20 max	0.03	0.02	0.04	0.07	0.06	—	0.04	0.01	0.04	0.04	—
pH Value	4.5 - 7.0	5.9	5.6	5.4	5.8	5.2	—	5.6	6.0	5.5	5.7	5.1
Acidity	0.04 max	0.01	0.01	0.01	0.01	0.01	—	0.01	0.01	0.01	0.01	—
(H ₂ SO ₄ %)	1	—	—	—	—	—	—	—	—	—	—	—
Total Volatiles, %	0.25 max	0.07	0.10	0.08	0.07	—	—	0.08	0.10	0.08	0.12	—
Solutes (H ₂ O ₂ %)	0.20 max	0.03	0.07	0.09	0.07	—	—	0.11	0.07	0.08	0.06	—
Water	0.20 max	0.04	0.04	0.03	0.03	—	—	0.01	0.02	0.02	0.02	—
Insoluble, %	—	—	—	—	—	—	—	—	—	—	—	—

SOURCE

CHARGE OF CHINA - DIRECT

No/Tr. of Hand Checks	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17
No/Tr. Received at BAP	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17	6/17

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NITROGENOUS
Hazardous Waste 5/15/86, #32

Proprietary, lot No. MAP lot (SRC No.) GL lot No. (HFC, lot No.)	77B-069006			77B-069006		
	12-202	12-204	12-202	12-202	12-202	12-204
<u>Parameter</u>						
Min/Max	4.4 - 4.4	4.4	4.2	4.1	4.1	4.1
Avg. Particle Size.	99.0 min	99.7	99.0	99.9	99.7	99.7
Per cent, %	0.30 max	0.03	0.03	0.04	0.03	0.03
Ash Content, %	4.5 - 7.0	5.3	6.0	5.4	6.0	5.3
pH Value	0.06 max	0.01	0.01	0.01	0.01	0.01
Acidity, % (H ₂ SO ₄) ₂	0.10 max	0.10	0.07	0.13	0.09	0.10
Total Volatiles, %	0.25 max	0.10	0.13	0.09	0.09	0.10
Solubles (H ₂ SO ₄) ₂ , %	0.20 max	0.04	0.04	0.03	0.05	0.11
Water Insoluble, %	0.20 max	0.02	0.01	0.02	0.02	0.02

SOURCE: STAMPER OF CANISTER - DIRECT

STAMPER OF CANISTER

No/Tr. of Manufacture	6/77	6/77	6/77	6/77	6/77	6/77
No/Tr. Received at MAP	6/77	6/77	6/77	6/77	6/77	6/77

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URACONCUPINE
BIGEAL Procellaris 6/132mm. #203

Propellant Lot No.	170-00000						170-00000					
	12-219	12-211	12-212	12-213	12-214	12-215	12-216	12-217	12-218	12-219	12-211	1328
<u>Particulars</u>												
Avg. Particle Size..	2.4 - 6.0	4.5	4.8	4.9	4.3	3.2	—	4.8	4.7	3.1	4.7	4.5
Purity, %	99.0 min	99.0	99.0	99.0	99.7	99.0	—	99.0	99.0	99.0	99.0	99.7
Ash Content, %	0.30 max	0.07	0.08	0.05	0.03	0.03	—	0.10	0.07	0.04	0.06	0.09
pH Value	4.3 - 7.0	5.3	5.3	4.7	4.8	5.3	—	4.8	5.4	5.3	4.9	—
Acidity, (H ₂ SO ₄ /Eq). %	0.06 max	0.01	0.01	0.02	0.02	0.01	—	0.02	0.01	0.01	0.01	0.02
Total Volatiles, %	0.25 max	0.03	0.07	0.12	0.10	0.08	—	0.08	0.07	0.12	0.13	0.08
Solubility, (H ₂ SO ₄ /Eq). %	0.20 max	0.04	0.13	0.07	0.04	0.04	—	0.06	0.05	0.06	0.06	—
Water Insoluble, %	0.20 max	0.03	0.03	0.02	0.11	0.04	—	0.02	0.04	0.03	0.04	0.04

SOURCE

	STANDARD OF GAMMA - DILUTED	STANDARD OF GAMMA - DIRECT
No/No. of Revolutions	6/111	6/111
No/No. Received At RAAP	6/111	6/111

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NITROQUINOLINE
NDAI Test Sheet 1/15/69, p. 692

Properties Lot No. NDAI lot (ARC No.) GL-Lot No. (Ref. Lab.)	1/14-022807						1/14-022807					
	12-212	12-211	12-212	12-211	12-214	12-215	12-212	12-211	12-214	12-215	12-212	12-211
Properties												
Avg. Particle Size.	3.4 - 6.0	4.6	3.6	5.3	5.2	3.1	--	3.4	6.3	4.4	4.4	5.0
Purity, %	99.0 min	99.0	99.4	99.8	99.8	--	99.0	99.8	99.9	99.8	99.8	99.13
Ash Content, %	0.30 max	0.03	0.03	0.04	0.05	--	0.01	0.00	0.07	0.03	0.04	0.06
pH Value	4.5 - 7.0	4.7	4.9	4.9	5.9	6.0	--	5.4	5.4	5.1	5.0	4.7
Acidity (H_2SO_4), %	0.05 max	0.01	0.02	0.01	0.02	0.01	--	0.01	0.01	0.02	0.01	0.007
Total Volatiles, %	0.25 max	0.06	0.06	0.12	0.09	0.06	--	0.10	0.09	0.12	0.04	0.04
Sulfate (Na_2SO_4), %	0.20 max	0.06	0.04	0.01	0.04	0.04	--	0.03	0.03	0.04	0.06	0.06
Water Insoluble, %	0.20 max	0.04	0.03	0.01	0.02	0.02	--	0.01	0.01	0.02	0.02	--

10 SOURCE: STANARD OF CANADA - DIRECT

No/Tr. of Manufacture	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77
No/Tr. Received at NAP	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77	6/77

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NITROGUANIDINE
100% Freebase, 1/12/62, H102

Report-Lines lot No. and lot (SRC No.) etc.-lot No. (H102, Lot No.)	718-66-9007				718-66-9007				102
	11-212	12-214	12-217	12-219	12-222	12-223	13-01	13-01	
Properties:									
Avg. Particle Size.	3.4 - 6.0	4.9	4.6	3.9	4.9	4.3	—	4.4	3.3
Ash Content, %	0.20 max	0.04	0.04	0.04	0.03	0.02	—	0.03	0.16
pH Value	4.5 - 7.0	5.3	6.1	5.6	5.3	4.7	—	5.5	4.3
Acidity (H ₂ SO ₄ Eq). %	0.06 max	0.01	0.01	0.01	0.02	0.02	—	0.01	0.01
Total Volatiles, %	0.25 max	0.07	0.10	0.10	0.11	0.06	—	0.03	0.03
Sulfates (H ₂ SO ₄ Eq). %	0.20 max	0.04	0.01	0.06	0.06	0.06	—	0.10	0.04
Water Insoluble, %	0.20 max	0.02	0.02	0.03	0.02	0.02	—	0.06	0.01

SOURCE:

STANDARD OF CANADA - DIRECT

SINTERED ALUMINUM

No/Tr. of Manufacture	6/17	6/17	6/17	6/17	6/17	6/17	10/7/62	10/7/62	10/7/62
No/Tr. Received At RAAP	6/17	6/17	6/17	6/17	6/17	6/17	8/7/77	8/7/77	8/7/77

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NITROGlycerine

Hazardous Material Test Report

Propellant Lot No.	278-099997			1337			199-099992		
HAP Lot (IPC No.)	13-246	13-247	13-248	13-249	13-250	1337	8-027	8-032	8-034
<u>Paraffins</u>									1777
Avg. Particle Size	2.4 - 6.0								
Paraffin, I	99.0 min	99.0	99.0	99.7	99.7	—	99.9	99.9	99.0
Air Content, %	0.20 max	0.06	0.03	0.04	0.07	0.07	—	3.4	4.6
pH Value	4.5 - 7.0	3.0	3.5	6.3	5.7	5.8	—	5.4	4.6
Acidity (H ₂ -SO ₄ Eq), %	0.06 max	0.01	0.01	0.01	0.01	0.01	—	0.01	0.01
Total Volatiles, %	0.25 max	0.11	0.10	0.06	0.12	—	0.15	0.10	0.12
Solutes (H ₂ -SO ₄ Eq), %	0.20 max	0.06	0.07	0.14	0.06	0.07	—	0.03	0.03
Water	0.20 max	0.03	0.02	0.01	0.06	0.06	—	0.01	0.01
Insoluble, %	—	—	—	—	—	—	—	—	—
<u>Solvent</u>									Nitrobenzene
No/Br. of Manufacture	6/77	6/77	6/77	6/77	6/77	7/77	8/71	8/71	
No/Br. Received At DMAP	7/77	7/77	7/77	7/77	7/77	1/78	1/78	1/78	

CHAMBER OF CANADA - DIRECT

NITROBENZENE

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ANALYSIS
DOA1 Propellent 5/13/66 - H292

Propellant Lot No. DAP Lot (DPC No.) Clik-Lot No. (Hdg. Lot No.)	79-031225			79-040919			79-040919		
	8-910	8-911	8-912	8-910	8-911	8-912	8-910	8-911	8-912
Parameter									
Avg. Particle Size, μ	2.4 - 6.0	6.3	4.7	4.6	—	5.7	5.7	5.1	—
Purity, %	99.0 min	99.9	99.9	—	99.9	99.9	99.9	99.9	—
Ash Content, %	0.20 max	0.07	0.03	—	0.03	0.04	0.04	0.01	0.03
pH Value	4.5 - 7.0	5.4	5.1	4.9	—	5.0	5.2	5.1	—
Acidity (H ₂ SO ₄), %	0.06 max	0.01	0.01	—	0.01	0.01	0.01	0.01	0.01
Total Volatiles, %	0.25 max	0.04	0.16	0.03	0.13	0.14	0.13	0.07	0.07
Solubility (Na ₂ CO ₃), %	0.20 max	0.07	0.05	0.10	—	0.07	0.07	—	0.05
Water Insoluble, %	0.20 max	0.04	0.01	—	0.01	0.01	0.01	0.01	—

SOURCE

	SAFETY EXP.							
No./tr. of batches/series	7/71	8/71	9/71	7/71	7/71	7/71	7/71	7/71
No./tr. Received At DAP	1/79	1/79	1/79	1/79	1/79	1/79	1/79	1/79

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MICAL Propellants (1/15/68 - 1968)

Propellant Lot No.	196-00299			196-00299			196-00299		
	B-324	B-325	B-322	B-323	B-321	B-324	B-325	B-322	B-324
Parameter									
Avg. Particle Size, μ	3.4 ~ 6.0			3.3	3.6	3.8	—	3.0	4.9
Purity, %	99.0 min			99.9	99.9	99.9	—	99.9	99.7
Ash Content, %	0.30 max			0.05	0.01	0.03	—	0.04	0.01
pH Value	4.5 ~ 7.0			5.5	4.9	5.1	—	5.9	4.8
Acidity (H ₂ SO ₄ , %)	0.06 max			0.01	0.01	0.01	—	0.02	0.01
Total Volatiles, %	0.25 max			0.05	0.07	0.16	0.07	0.06	0.05
Sulfates (BaSO ₄ , %)	0.20 max			0.04	0.04	0.04	—	0.04	0.04
Water Insolubles, %	0.20 max			0.01	0.01	0.01	—	0.01	0.01

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SAMPLE	RAVENNA API			RAVENNA API		
	7/71	7/71	7/71	7/71	7/71	7/71
Mr/Fr. of Resinester						
Mr/Fr. Received At RAP	2/79	2/79	2/79	2/79	2/79	2/79

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NITROCUMULINE
ANAL PROFILES 7/13/80, N201

Propellant Lot No.	7/12-652262			7/12-652269			7/12-652276			7/12-652281		
	8-211	8-214	8-215	8-211	8-212	8-213	8-211	8-212	8-213	8-211	8-212	8-213
Parameters												
Avg. Particle Diameter	3.4 - 6.0	4.8	4.7	5.1	—	—	3.4	3.2	3.1	—	—	—
Purity, %	99.0 min	99.0	99.7	99.0	—	—	99.9	99.6	99.6	—	—	—
Ash Content, %	0.30 max	0.05	0.07	0.06	—	—	0.04	0.03	0.03	—	—	—
pH Value	4.5 - 7.0	4.8	5.1	5.0	—	—	4.9	5.0	5.0	—	—	—
Acidity (H ₂ S0 ₄ HQ), %	0.04 max	0.02	0.02	0.02	—	—	0.02	0.02	0.02	—	—	—
Total Volatiles, %	0.15 max	0.14	0.06	0.05	0.08	—	0.04	0.06	0.16	0.04	—	—
Solubles (H ₂ S0 ₄ HQ), %	0.20 max	0.03	0.03	0.11	—	—	0.10	0.08	0.08	—	—	—
Water	0.20 max	0.01	0.01	0.01	—	—	0.01	0.01	0.01	—	—	—
Inertiable, %	—	—	—	—	—	—	—	—	—	—	—	—
Source												
No/yr. of Manufacture	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71
No/yr. Received At DAP	2/70	2/70	2/70	2/70	2/70	2/70	2/70	2/70	2/70	2/70	2/70	2/70

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NITROQUINOLINE
NDAAL Reagent 6/15/66, M302

Propellant Lot No. NAAAP Lot No. (WPC No.) CCL-Lot No. (Mfg. Lot No.)	702-662001			702-662001			702-662001			702-662001		
	2-042	2-042	2-042	2-042	2-042	2-042	2-042	2-042	2-042	2-042	2-042	2-042
limits												
Avg. Particle Size.	2.4 - 6.0	4.0	5.3	4.0	—	5.4	5.5	5.0	—	4.9	5.2	5.6
Purity, %	99.0 min	99.0	99.0	99.0	—	99.0	99.0	99.0	—	99.0	99.0	99.0
Ash Content, %	0.30 max	0.01	0.07	0.04	—	0.00	0.04	0.03	—	0.03	0.01	0.03
pH Value	4.5 - 7.0	4.0	5.2	5.0	—	5.1	4.8	5.1	—	5.2	4.9	5.3
Acidity (H ₂ SO ₄ Eq.), %	0.05 max	0.01	0.02	0.02	—	0.02	0.02	0.02	—	0.01	0.02	0.02
Total Volatiles, %	0.25 max	0.12	0.01	0.00	0.00	0.10	0.10	0.00	0.00	0.12	0.07	0.10
Solubility (H ₂ SO ₄ Eq.), %	0.20 max	0.09	0.15	0.10	—	0.12	0.09	0.09	—	0.06	0.11	0.12
Water Insoluble, %	0.20 max	0.01	0.01	0.01	—	0.01	0.01	0.00	—	0.01	0.01	0.01
SOURCE	NAYERS API			FAYERS API			FAYERS API			FAYERS API		
No/Ts. of Manufacture	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71
No/Ts. Received At NAAAP	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72

	107	107	107	107	107	107	107	107	107	107	107	107
No/Ts. of Manufacture	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71	8/71
No/Ts. Received At NAAAP	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72	2/72

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NITROGUMMOLINE
N191 Present in 1/15mm. N1292

Propellant Lot No.
Ride Lot (ARC No.)
CCL-Lot No. (Mfg. Lot No.)

Parameter	Units	196-655911			196-655912			196-655913			196-655914			196-655915		
		g-254	g-251	g-252	g-253	g-254	g-251	g-252	g-253	g-254	g-251	g-252	g-253	g-254	g-251	g-252
Avg. Particle Size, μ	3.4 - 6.0	4.3	4.3	4.7	—	5.1	5.1	5.0	—	4.7	4.5	5.4	—	—	—	—
Purity, %	99.0 min	99.0	99.0	99.0	—	99.9	99.9	99.9	—	99.8	99.8	99.9	—	—	—	—
Ash Content, %	0.30 max	0.05	0.02	0.02	—	0.04	0.03	0.03	—	0.04	0.03	0.03	—	—	—	—
Acidity (H ₂ SO ₄ Eq.), %	0.06 max	0.01	0.01	0.01	—	0.01	0.01	0.01	—	0.02	0.02	0.01	—	—	—	—
Total Volatiles, %	0.15 max	0.06	0.10	0.08	—	0.12	0.08	0.05	0.02	0.04	0.03	0.07	—	0.06	—	—
Sulfates (Ba ₂ SO ₄ Eq.), %	0.10 max	0.09	0.06	0.06	—	0.07	0.10	0.09	—	0.02	0.04	0.05	—	—	—	—
Water Insolubles, %	0.20 max	0.01	0.01	0.01	—	0.06	0.01	0.01	—	0.03	0.02	0.02	—	—	—	—

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SOURCE	BAVNAKA DAP			BAVNAKA AAF					
	No./Tr. of Manufacture	9/71	9/71	9/71	9/71	9/71	9/71	9/71	9/71
No./Tr. Received at DAP	2/79	2/79	2/79	2/79	2/79	2/79	2/79	2/79	2/79

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Propellant Lot No.
BAP Lot (SRC No.)
Cut-Lot No. (WFG Lot No.)

Instrumentation
Blast Test Report (1/12/66, N202)

Parameter	Units	196-601262			196-601263			196-601264			196-601265		
		I-211	I-212	I-213									
Avg. Particle Size, μ	3.4 - 6.0	5.0	4.6	4.3	—	3.6	3.0	—	3.2	3.4	3.0	—	—
Purity, %	99.0 min	99.7	99.9	99.9	—	99.7	99.8	99.7	—	99.8	99.7	99.6	—
Ash Content, %	0.30 max	0.05	0.05	0.05	—	0.05	0.04	0.04	—	0.05	0.04	0.05	—
pH Value	4.5 - 7.0	5.1	5.4	5.2	—	4.6	4.9	5.1	—	4.8	5.2	5.4	—
Acidity, % (H ₂ SO ₄), %	0.05 max	0.01	0.01	0.02	—	0.02	0.02	0.02	—	0.02	0.02	0.02	—
Total Volatiles, %	0.25 max	0.10	0.05	0.04	0.10	0.05	0.10	0.03	0.12	0.05	0.09	0.02	—
Sulfates (Ba ₂ SO ₄), %	0.30 max	0.07	0.06	—	0.07	0.06	0.12	—	0.08	0.06	0.05	—	—
Water Insoluble, %	0.20 max	0.02	0.02	—	0.01	0.01	0.01	—	0.01	0.01	0.01	—	—

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SOURCE

	DAVISON AAF												
No/Tr. of Manufacturer	9/11	9/11	9/11	9/11	9/11	9/11	9/11	9/11	9/11	9/11	9/11	9/11	9/11
No/Tr. Received At BAP	3/11	3/11	3/11	3/11	3/11	3/11	3/11	3/11	3/11	3/11	3/11	3/11	3/11

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Propellant Lot No. Batch lot (NRC No.) U.R. lot No. (OMG. lot No.)	196-062222			196-062232			196-062242			196-062252		
	9-222	9-223	9-224	9-225	9-226	9-227	9-228	9-229	9-230	9-231	9-232	9-233
NITROGUANIDINE												
Propellant Lot No. Batch lot (NRC No.) U.R. lot No. (OMG. lot No.)	9-222	9-223	9-224	9-225	9-226	9-227	9-228	9-229	9-230	9-231	9-232	9-233
Propellant No.	196-062222	196-062232	196-062242	196-062252	196-062222	196-062232	196-062242	196-062252	196-062222	196-062232	196-062242	196-062252
Avg. Particle Size, μ	3.4 - 4.0	4.4	4.6	4.3	—	2.8	4.3	4.7	—	4.6	4.6	3.9
Purity, %	99.0 min	99.1	99.0	99.0	—	99.0	99.0	99.0	—	99.0	99.0	99.0
Ash Content, %	0.20 max	0.01	0.04	0.05	—	0.01	0.01	0.05	—	0.01	0.00	0.01
pH Value	4.5 - 7.0	5.0	5.3	5.0	—	5.0	5.2	5.0	—	5.1	5.5	5.4
Acidity (H_2SO_4 Eq.), %	0.05 max	0.01	0.01	0.01	—	0.01	0.01	0.01	—	0.01	0.01	0.01
Total Volatiles, %	0.25 max	0.10	0.05	0.01	—	0.05	0.05	0.05	—	0.05	0.05	0.05
Sulfates (H_2SO_4 Eq.), %	0.20 max	0.07	0.11	0.14	—	0.03	0.10	0.08	—	0.05	0.09	0.02
Water Insoluble, %	0.20 max	0.02	0.01	0.01	—	0.01	0.01	0.01	—	0.01	0.01	0.01
RAVENNA MAP												
No/Tc. of Manufacture	4/71	4/71	4/71	4/71	4/71	4/71	4/71	4/71	4/71	4/71	4/71	4/71
No/Tc. Received At RMAP	6/71	6/71	6/71	6/71	6/71	6/71	6/71	6/71	6/71	6/71	6/71	6/71

Attachment 6
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INTERCOMPARISON
TEST PRECISION 5/15/69, 1969

Propellant Lot No. SAPL Lot No. (MFG. Lot No.) CCL-Lot No. (MFG. Lot No.)	196-99321			196-99322			196-99323			196-99324			196-99325		
	8-528	8-529	8-530	8-528	8-529	8-530	8-528	8-529	8-530	8-528	8-529	8-530	8-528	8-529	8-530
PARAMETERS															
	Alpha														
Avg. Particle Size, μ	2.4 ~ 6.0	4.2	4.4	4.6	—	—	—	—	—	—	—	—	—	—	—
Porosity, %	29.0 min	29.0	29.0	29.0	—	—	—	—	—	—	—	—	—	—	—
Ash Content, %	0.20 max	0.04	0.03	0.03	—	—	—	—	—	—	—	—	—	—	—
pH Value	4.5 ~ 7.0	5.5	5.3	4.8	—	—	—	—	—	—	—	—	—	—	—
Acidity (H ₂ SO ₄)%, %	0.05 max	0.01	0.01	0.02	—	—	—	—	—	—	—	—	—	—	—
Total Volatiles, %	0.25 max	0.02	0.02	0.02	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30	0.30
Sulfation (Na ₂ SO ₄ Eq.), %	0.20 max	0.07	0.06	0.07	—	—	—	—	—	—	—	—	—	—	—
Water	0.20 max	0.01	0.01	0.02	—	—	—	—	—	—	—	—	—	—	—
Insolubles, %	111														

SOURCE	RAVENNA AAF			RAVENNA AAF		
	4/71	4/71	4/71	4/71	4/71	4/71
No/Pr. of Manufacturer	4/71	4/71	4/71	4/71	4/71	4/71
No/Pr. Received At RAVP	4/71	4/71	4/71	4/71	4/71	4/71

Attachment 6
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Proprietary Log No.
Blast Log (APC No.)
Call-List Log (W.L.)

Date/yr. Received

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ATTACHMENT
N2021 Streetline 7/13/99 - N22

Propellant Lot No. Safp Lot (APC No.) OCL-Lot No. (Ref. Lot No.)	110-251114			100-251114
	11-225	11-226	11-227	
<u>Per cent by weight</u>				
Avg. Particle Size.	3.4 - 6.0	3.0	4.6	—
Purity, %	99.0 min	99.1	99.0	99.0
Ash Content, %	0.20 max	0.00	0.01	0.03
pH Value	4.5 - 7.0	3.9	4.6	3.4
Acetate, (CH_3COO) _n , %	0.05 max	0.01	0.02	0.01
Total Volatiles, %	0.25 max	0.05	0.06	0.05
Sulfates, (Na_2SO_4 Eq.), %	0.20 max	0.02	0.03	0.03
Water	0.20 max	0.05	0.01	0.05
Insoluble, %				
<u>SOURCE</u>				
No/Tr. of Manufacture	3/73	3/73	3/73	3/73
No/Tr. Received At RAAP	9/79	9/79	9/79	9/79

Attachment 6
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ethyl centralite
methyl propylate 1/133am, 11203

Ethyli Concentrate
Initial Preparation 1/1/22, 2022

Propellant Lot No. R&P Lot (NGC No.) Hg - Lot No.	Parameters	115						115						115					
		10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	
Solidification Point, °C	Limits	21.0- 22.5	22.1	22.2	22.1	22.1	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	22.0	
Related Material (Appearance)	Bright, Clear Liquid, Free of Scum & Deposit	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	
Volatile Content, %	0.1 Max.	0.093	0.092	0.093	0.093	0.092	0.093	0.093	0.092	0.093	0.093	0.093	0.093	0.093	0.093	0.093	0.093	0.093	
Ash Content, %	0.1 Max.	0.004	0.002	0.004	0.002	0.003	0.002	0.002	0.003	0.002	0.003	0.002	0.003	0.002	0.003	0.002	0.003	0.002	
Sum of Amines, %	0.00 Max.	0.011	0.012	0.013	0.011	0.012	0.013	0.012	0.013	0.012	0.013	0.012	0.013	0.012	0.013	0.012	0.013	0.012	
Acidity, % HCl, %	0.00 Max.	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	
Hydrolyzable Chlorine Compound, %	0.001 Max.	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	
Particle Form, % Passing through 655 No. 30 Sieve	115	99.9	99.91	99.93	99.96	99.91	99.94	99.92	99.91	99.93	99.94	99.92	99.91	99.93	99.94	99.93	99.92	99.91	
Microscopie	Free from grit, visible particles, foreign matter	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	

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096690-266 207 207 00 00003

096690-266 207 207 00 00003

Attachment 7
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Ruby Centrifuge
No.1 Propellant 6/155mm, M201

Propellant Lot No. RARP Lot (WPC No.) Mfg. Lot No.		7SL-669922										1397-2	
Parameter	Units	40A	50A	60A	80A	90A	91A	92A	93A	94A	95A	96A	
Solidification Point, °C	71.0- 72.5	72.2	72.1	71.6	71.7	72.0	71.8	71.7	71.6	71.9	71.7	72	
Mixed Materials (Appearance)	Bright, Clear Liquid Free of Scum & Deposit	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	
Volatile Content, %	0.1 Max.	0.078	0.085	0.082	0.094	0.091	0.095	0.097	0.094	0.091	0.084	0.084	
Ash Content, %	0.1 Max.	0.008	0.001	0.001	0.002	0.002	0.002	0.002	0.002	0.002	0.001	0.001	
Sum of Ashes, %	0.20 Max.	0.056	0.053	0.054	0.061	0.053	0.057	0.058	0.100	0.116	0.094	0.091	
Acidity, as HCl, %	0.04 Max.	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	
Hydrolyzable Chlorine Compound, %	0.001 Max.	0.0001	0.0001	0.0001	0.0002	0.0002	0.0002	0.0002	0.0001	0.0001	0.0001	0.0001	
Particle Form, % Passing through USS No. 30 Sieve	99.9 Max.	99.91	99.99	99.92	99.93	99.94	99.97	99.96	99.97	99.97	99.97	100	
Nonflammability	Free from grit, visible separation, foreign matter	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	Passes	

K30A1 Propellant 6/155mm. H202

Propellant Lot No. RAAP Lot (IPC No.) Hfg. Lot No.	77C-069805 485R-1 CPH	77H-069806 486R-1 CPH	79D-069807 486R-1 CPH	79D-069859 487R-1 CPH	79E-069960 508R-1 CPH	79E-069961 511R-1 CPH
Parameters	Limits					
Purity, %	99.0 min.	-	-	-	-	-
K content, %	99.0 min.	-	-	-	-	-
Moisture, %	1.0 max.	0.01	0.005	0.01	0.02	0.02
Insoluble Matter, %	0.1 max.	-	-	-	-	-
Grit, %	None	-	-	-	-	-
pH	6-8	-	-	-	-	-
Chlorides, as KCl, %	0.02 Max.	-	-	-	-	-
Granulation, % Passing USS No. 50 Sieve USS No. 70 Sieve		100 min.	-	-	-	-
		95 min.	-	-	-	-

Attachment 8
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H2O1 Propellant / 152mm, M203 (comes in box)

Propellant Lot No.	AlM Lot (IMC No.)	Hg. Lot No.	79E-069962	79L-069992	79H-069994
			S12R1	S12N1	S32
			GPN	GPN	GPN
Parameters	limits				
Purity, %	99.0 min.	-	-	99.6	99.84
K Content, %	99.0 min.	-	-	99.9	99.90
Moisture, %	1.0 max.	0.01	> 0.01	None	0.0
Insoluble Matter, %	0.1 Max.	-	> 0.004	0.01	< 0.1
Crit. I	None	-	None	None	-
pH	6-8	-	6.3	7	6.5
Chlorides, as KCl, %	0.02 Max.	-	> 0.02	None	< 0.02
granulation, %					
Passing					
USS No. 50 Sieve	100 min.	-	-	99.9	100
USS No. 70 Sieve	95 min.	-	-	100	100

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Attachment 8
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Graphite, Grade IV
Metal Prohibited 1/15mm. max

Propellant Lot No. SAMP Lot (NGC No.) NGC Lot No.	790-069803 127	790-069806 127	790-069807 127	790-069829 127	790-069950 124	790-069951 123	790-069952 125	790-069954 126
Percentages	Linkage							
Reinforce, 2	0.50 Max.	0.50	0.50	-	0.4	0.22	0.9	0.9
Ash, %	0.0 Max.	1.91	-	-	1.13	-	1.20	1.54
Silica, %	2.75 Max.	0.58	-	-	0.65	-	0.58	1.10
Other Grit, %	None							
Acidity, %	None							
Free Sulfur, %	0.03 Max.	None	-	None	None	None	None	None
Total Sulfur, %	0.50 Max.	0.10	-	0.13	-	0.13	-	0.21
Crystallization, % Passing through USS No. 325 (44.0/phi screen)	36.0 Min.	37.4	-	-	37.8	36.12	36.2	38.0

Acetone
HODA1 Propellant 6/155mm, H203

<u>HODA1 Lot No.</u>	<u>NPC Lot No.</u>	<u>Car No.</u>	<u>Mercurius Analyzes</u>		
			<u>Specific Gravity</u>	<u>Moisture, %</u>	<u>0.50% Max.</u>
<u>SPECIFICATION LIMITS:</u>					
77C-069805	1212	CATX-75208	Ashland Chemical Co. 6-6-77	0.7917	0.39
77H-069806	1213	CATX-95502	" 7-7-77	0.7919	0.43
77H-069807	1214	CATX-76953	" " 7-12-77	0.7915	0.36
	1215	CATX-95415	" " 7-19-77	0.7923	0.37
79D-069959	1251	CATX-17976	Devon Chemicals, Inc 2-26-79	0.7927	0.06
79E-069960					
79E-069961					
79E-069962					
79L-069992	1252	ACFX-81001	Ashland Chemical Co. 9-24-79	0.7928	0.42
79H-069994					

Alcohol
M30AL Propellant f/155mm, M203

<u>M30AL Lot No.</u>	<u>NPC Lot No.</u>	<u>Car No.</u>	<u>Supplier</u>	<u>Date Rec'd.</u>	<u>Hercules Analysts</u>		
					<u>Sp.Gr.</u>	<u>Toluene (%)</u>	<u>Alcohol (%)</u>
SPECIFICATION LIMITS:							
77C-069905	646	GCBX-959	Union Carbide Corp.	6-13-77	0.8151	0.42	95.2
	647	GCBX-1065	"	6-20-77	0.8158	0.75	95.0
	648	GATX-87993	INC Chemical Group, Inc.	6-28-77	0.8153	0.75	95.1
	649	GCBX-959	Union Carbide Corp.	6-29-77	0.8168	0.75	95.3
77H-069906	650	HATX-24803	INC Chemical Group, Inc.	7-6-77	0.8152	0.75	95.15
	651	GATX-87993	"	7-6-77	0.8147	0.75	95.28
77H-069907	652	GATX-87997	"	"	0.8162	0.75	96.9
	653	GATX-99110	"	"	0.8157	0.75	95.0
79B-069959	703	HATX-6244	Union Carbide Corp.	2-19-79	0.8157	0.75	95.0
79E-069960	704	SCMX-2778	Shell Chemical Co.	4-2-79	0.8141	0.75	95.42
79E-069961	705	SCMX-2782	"	4-9-79	0.8142	0.75	95.41
	706	SCMX-2235	"	4-15-79	0.8135	0.75	95.6
79E-069962	707	SCMX-2778	"	5-3-79	0.8152	0.75	95.15
79L-069992	712	SCMX-2538	"	"	0.8150	0.75	95.2
79L-069994	714	SCMX-2782	"	"	0.8155	0.75	95.08
	715	SCMX-2778	"	"	0.8163	0.75	94.9

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Process Conditions
200A1 Precoat, 1/15mm, 12001

Process	210-069881	210-069886	210-069892	210-069899	210-069906	210-069913	210-069920	210-069927	210-069934	210-069941	210-069948	210-069955	210-069962	210-069969	210-069976
AC Stirring	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN	CIN
<u>Substitution:</u>															
Quart Dry Alcohol, gals.	1 tub 17 minutes	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Dwell Time, minutes	5	:	:	:	:	:	:	:	:	:	:	:	:	:	
Block Breaker & MF. <u>Mixing</u>															
Screen Opening	1 tub x 3/4"	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
No. Tubefills	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6
Dry RC Weight/tub, lb	37.0	40.5	37.0	40.5	37.0	40.5	37.0	40.5	37.0	40.5	37.0	40.5	37.0	40.5	37.0
Total RC Dry Weight/gals, lb	180.0	210.0	180.0	210.0	180.0	210.0	180.0	210.0	180.0	210.0	180.0	210.0	180.0	210.0	180.0
<u>Precoat</u>															
Type Precoat	Schrader Seal Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
No. Chrs./Prcntn	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2
Per Chr. mi/Charge, lb	26.0	21.0	26.0	21.0	26.0	21.0	26.0	21.0	26.0	21.0	26.0	21.0	26.0	21.0	26.0
No. Chr./Charge, lb	52.0	42.0	52.0	42.0	52.0	42.0	52.0	42.0	52.0	42.0	52.0	42.0	52.0	42.0	52.0
Wasted Time, minutes	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2
<u>Final Mixing</u>															
Ingredients/lbs.															
Bituminous Resin, lb	145.00	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Bitumen Oxide, lb	125.00	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Ethy Centralite, lb	250.00	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Potassium Sulfate, lb	0.00	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Total	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00	537.00
Substitutes															
Alcohol, lb	75.0	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Acetone, lb	47.0	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Temperature at Precoat	110 to 120° F														
Total Mixing Time, hrs.	3														
Beijing	With React Gas														
Callling of Mix	Reduce water	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
	temperature	to 45-48° F													
	and mix 15	minutes,													
	minutes,	minimum													
<u>Blocking</u>															
Type Blocker	12" Frame	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same
Partl. Time, minutes	2 1/2	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same	Same

Same Attachment 12
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Process Conditions
Final Propellant (1/15Sec. N2O)

Process	120-00902	120-00906	120-00907	120-00919	120-00949	120-00961	120-00963	120-00972	120-00974
<u>Finning</u>									
Type	None	None	None	None	None	None	None	None	None
No. Blows/Pound	5	5	5	5	5	5	5	5	5
No. Insects									
Auger Size									
Fin Dia.									
Fin Circle									
No. Screens									
Entration Pressure									
<u>Cutting</u>									
Type	Machin	Semi							
Length, Inch	0.565	0.605	0.565	0.605	0.565	0.605	0.565	0.605	0.565
Wt. /Fray, lb	23	23	23	23	23	23	23	23	23
Grapes/Cabinet	10	10	10	10	10	10	10	10	10
<u>Baking</u>									
Trots/Day	276	276	276	276	276	276	276	276	276
Loading Temp.	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient	Ambient
Build-up	5° F/hr	5° F/hr	5° F/hr	5° F/hr	5° F/hr	5° F/hr	5° F/hr	5° F/hr	5° F/hr
Cycle Temp.	140° F	140° F	140° F	140° F	140° F	140° F	140° F	140° F	140° F
Cycle Time	72 hrs	72 hrs	72 hrs	72 hrs	72 hrs	72 hrs	72 hrs	72 hrs	72 hrs
<u>Blending/Cleaning</u>									
Blending	3400 Prop.	Semi							
Graphite	5 lb 6.4 oz	3 lb 9 oz	3 lb 9 oz	3 lb 9 oz	3 lb 9 oz	3 lb 9 oz	3 lb 9 oz	3 lb 9 oz	3 lb 9 oz
Graphite	Graphite	Graphite	Graphite	Graphite	Graphite	Graphite	Graphite	Graphite	Graphite
Screen	90 minutes	90 minutes	90 minutes	90 minutes	90 minutes	90 minutes	90 minutes	90 minutes	90 minutes
<u>Screening</u>									
Acceptance Screen, Inch	0.700-0.910	Same							
Fine Screen, Inch	0.315 Max.								
Wt./Fiber Drum, lb	100								
No. Drums/Batch	24								
Final Blending Time	10 min.	Same							
<u>Packing</u>									
Type	Fiber Drum	Same							
Wt./Fiber Drum	160 lbs								

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Attachment 12
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Batch Data
H300A1 Propellant I/155mm. H203

Batch Numbers	79C-069805						77H-069806					
	Closed Bomb			Closed Bomb			Closed Bomb			Closed Bomb		
	TV, %	At 90° F RQ, %	RF, %	At -40° F RQ, %	RF, %	At 90° F RQ, %	RF, %	At -40° F RQ, %	RF, %	At 90° F RQ, %	RF, %	At -40° F RQ, %
1-10	0.04	97.62	99.82	96.41	99.26	61-70	0.23	96.89	99.98	93.83	98.47	—
11-20	0.04	97.46	99.69	—	—	71-80	0.23	99.55	100.15	—	—	—
21-30	0.21	98.20	100.15	94.37	98.24	81-90	0.16	96.70	99.65	91.83	97.69	—
31-40	0.31	98.29	99.79	—	—	91-100	0.16	95.97	99.80	—	—	—
41-50	0.12	97.12	100.16	94.29	98.20	101-110	0.13	96.08	99.73	92.57	97.59	—
51-60	0.20	95.90	100.32	—	—	111-119	0.18	97.41	99.85	—	—	—
Weighted Average	0.15	97.43	99.99	95.02	98.57	—	0.18	97.10	99.86	92.74	97.92	—
Final Lot 0.13	96.51	99.74	92.58	98.16	—	0.36	96.35	99.44	92.46	97.93	—	—
<u>124</u>												
<u>79D-069919</u>												
120	0.18	97.41	99.85	—	—	1-10	0.12	96.54	100.90	91.76	99.18	—
121-130	0.13	96.64	99.69	91.00	97.81	11-20	0.13	96.64	100.53	—	—	—
131-140	0.11	95.60	99.23	—	—	21-29	0.11	96.80	100.47	92.82	98.49	—
141-150	0.17	96.60	99.51	91.22	98.63	—	—	—	—	—	—	—
151-160	0.20	95.31	99.78	—	—	—	—	—	—	—	—	—
161-170	0.14	95.41	99.93	91.40	98.39	—	—	—	—	—	—	—
171-176	—	—	—	—	—	—	—	—	—	—	—	—
Weighted Average	0.15	95.94	99.63	91.21	98.28	—	0.12	96.66	100.64	92.26	98.85	—
Final Lot 0.26	96.16	99.85	93.20	98.04	—	0.18	96.57	100.06	90.92	97.93	—	—

Attachment 11
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Batch Date
NMOA Prepolycell 5/15/99, M201

79E-069960						79E-069961					
Closed Bomb at 90° F			Closed Bomb at -40° F			Closed Bomb at 90° F			Closed Bomb at -40° F		
Batch Numbers	T.V. <u>Z</u>	RQ. <u>Z</u>	RF. <u>Z</u>	RQ. <u>Z</u>	RF. <u>Z</u>	Batch Numbers	T.V. <u>Z</u>	RF. <u>Z</u>	RQ. <u>Z</u>	RF. <u>Z</u>	RQ. <u>Z</u>
30	0.11	96.80	100.57	92.82	96.49	100	0.15	96.86	100.51	---	---
31-40	0.15	96.61	100.05	--	--	101-110	0.12	97.04	100.35	91.51	96.23
41-50	0.16	95.55	99.96	89.61	97.64	111-120	0.27	97.05	100.63	---	---
51-60	0.10	95.71	100.45	--	--	121-130	0.19	97.03	100.38	91.20	99.05
61-70	0.12	95.63	100.40	91.16	98.55	131-140	0.15	97.59	100.55	---	---
71-80	0.13	97.82	100.79	--	--	141-150	0.22	95.42	100.07	91.68	98.19
81-90	0.19	97.08	100.46	91.88	98.42	151-160	0.11	96.10	99.61	---	---
91-99	0.15	96.86	100.51	--	--	161-168	0.13	97.38	100.42	92.89	98.46
<u>125</u>											
Weighted Average	0.16	96.48	100.37	90.95	98.21		0.17	96.79	100.29	92.29	98.49
Final Lot	0.07	96.45	100.39	91.62	98.91		0.18	96.12	100.16	91.30	98.57

79E-069962						79E-069962					
Closed Bomb at 90° F			Closed Bomb at -40° F			Closed Bomb at 90° F			Closed Bomb at -40° F		
Batch Numbers	T.V. <u>Z</u>	RQ. <u>Z</u>	RF. <u>Z</u>	RQ. <u>Z</u>	RF. <u>Z</u>	Batch Numbers	T.V. <u>Z</u>	RF. <u>Z</u>	RQ. <u>Z</u>	RF. <u>Z</u>	RQ. <u>Z</u>
169-170	0.13	97.38	100.42	92.59	98.48	231-240	0.12	95.05	100.51	89.73	98.59
171-180	0.10	98.09	100.69	--	--	241-250	0.13	93.96	99.88	--	---
181-190	0.17	96.64	100.00	91.98	98.19	251-260	0.13	94.38	100.11	90.32	97.61
191-200	0.14	95.56	100.58	--	--						
201-210	0.14	96.01	100.16	91.65	98.78						
211-220	0.10	96.09	100.08	--	--						
221-230	0.15	96.17	100.08	92.17	98.46						
<u>125</u>											
Weighted Average	0.13	96.47	100.27	91.99	98.48		0.13	94.46	100.17	90.03	98.10
Final Lot	0.13	96.17	100.17	92.24	98.43		0.12	94.13	99.63	89.72	97.71

Attachment 13

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M204 Propellant 6/155mm, M203
Batch Data

		Closed Bomb			
		90.7	90.7	90.7	90.7
		at -90° F	at -40° F	at -40° F	at -40° F
Batch	TV.				
Numbers	Z				
261-270	0.10	94.18	100.01	--	--
271-280	0.11	91.33	99.86	99.17	98.16
281-290	0.13	93.94	99.98	--	--
291-300	0.13	91.67	100.16	99.69	98.09
301-310	0.09	94.07	100.25	--	--
311-316	--	--	--	--	--
Weighted Average	0.11	94.09	100.02	99.43	98.13
Final Lot 0.15	94.13	100.30	99.60	98.25	

PRODUCTION LOTS
H30A1 6/15/59&H, H203

<u>COMPOSITION</u>	<u>REQUIREMENTS</u>	<u>RAD77C- 069805</u>	<u>RAD77H- 069806</u>	<u>RAD77H- 069807</u>	<u>RAD79D- 069959</u>	<u>RAD79E- 069960</u>	<u>RAD79E- 069961</u>	<u>RAD79L- 069962</u>	<u>RAD79L- 069962</u>
Nitrocellulose	28.00 ± 1.30	27.18	28.00	27.74	27.43	27.76	28.16	28.65	28.90
Nitroglycerin	22.50 ± 1.00	22.80	22.36	22.53	22.95	22.56	22.23	22.49	23.48
Nitroglycerine	47.00 ± 1.00	47.54	47.06	47.04	46.91	47.20	47.04	46.29	46.97
Ethyl Cellulose	1.50 ± 0.10	1.55	1.56	1.58	1.55	1.51	1.51	1.46	1.53
Potassium Sulfate	1.00 ± 0.30	0.93	1.02	1.11	1.14	0.97	1.06	1.11	1.12
TOTAL		100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00
Total Volatiles	0.05 Max	0.33	0.34	0.26	0.18	0.07	0.18	0.03	0.12
Graphite (Glaze)	0.08	0.10	0.12	0.05	0.07	0.06	0.07	0.07	0.05
Stability	40" Min.	60"	60"	60"	60"	60"	60"	60"	60"
Bulk Density	—	—	—	—	—	—	—	—	—

GRAIN DIMENSIONS

Length (L)	0.9481	0.9529	0.9531	0.9514	0.9568	0.9585	0.9695	0.9551	0.9529
Diameter (D)	0.4173	0.4170	0.4166	0.4163	0.4145	0.4145	0.4167	0.4170	0.4186
Perforation Dia. (d)	0.0328	0.0338	0.0336	0.0340	0.0343	0.0330	0.0335	0.0342	0.0336
Inner Web (i:i)	0.0793	0.0776	0.0783	0.0771	0.0777	0.0792	0.0779	0.0776	0.0782
Outer Web (i:o)	0.0806	0.0817	0.0812	0.0814	0.0796	0.0813	0.0821	0.0811	0.0819
Avg. Web (i:a)	0.0800	0.0796	0.0797	0.0793	0.0786	0.0803	0.0800	0.0793	0.0801
Web Diff.	15 Max	2	5	5	2	3	5	4	5
L/D	2.10-2.50	2.27	2.29	2.30	2.31	2.31	2.31	2.29	2.28
D/d	5.0-1.5	12.4	12.3	12.4	12.2	12.1	12.6	12.2	12.4
L. Unif.	6.25 Max	1.08	0.82	0.64	1.29	1.16	0.93	1.07	0.92
D. Unif.	3.125 Max	1.28	1.25	1.57	0.95	1.12	1.19	1.01	1.56

CLOSED BOIL

RQ. 90°F	96.51	96.35	96.16	96.17	96.45	96.12	96.17	94.13	94.33
RF. 90°F	99.74	99.44	99.85	100.06	100.39	100.16	100.17	99.63	100.30
RQ. -40°F	92.58	92.44	93.20	90.92	91.62	91.30	92.24	89.72	89.40
RF. -40°F	98.16	97.93	98.04	97.93	98.91	98.57	98.43	97.71	98.25

DIE DIMENSIONS

Agate	0.470	0.470	0.470	0.470	0.470	0.470	0.470	0.470	0.470
Pin (Center)	0.037	0.037	0.037	0.037	0.037	0.037	0.037	0.037	0.037
Pin (Outer)	0.039	0.039	0.039	0.039	0.039	0.039	0.039	0.039	0.039
Pin Circle	0.262	0.262	0.262	0.262	0.262	0.262	0.262	0.262	0.262

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พิมพ์ครั้งที่หนึ่ง

二十一

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Ch. 56. a.	Ch. 56. a.
Bauer, Bkt., lge	Bauer, Bkt., lge
Ges., Bkt., lge	Ges., Bkt., lge
Gesamt-Freizeit	Gesamt-Freizeit
Frustrie 16d. Ber.	Frustrie 16d. Ber.
I. 1. Wahlkreis Baden	

Attachment 16
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Appendix 4

Pressure Data of
H30A1 Propellant F/155mm, H203

Lot Number	Test Date	P145°F, psi	P70°F, psi	P-65°F, psi	Calib/Test, Pds.
RAD-77G-069805	10/77	51500 49800	45100 43900	-	calib test
RAD-77H-069806	3/78	50400 51800	45500 46700	44700 46500	calib test
RAD-77H-069807	3/78	51200 51800	46100 46700	45500 46500	calib test
RAD-79D-069959	4/79	51400 49200	42200 44200	40000 44500	calib test
RAD-79E-069960	9/79	52200 49800	44500 46200	43100 45000	calib test
RAD-79E-069961	9/79	52500 49800	45200 46200	44200 45000	calib test
RAD-79E-069962	9/79	52600 49800	44800 46200	45700 45000	calib test
RAD-79L-069992	1/80	51800 -	43500 44900	40300 -	calib test
RAD-79M-069994	5/80	52500 50000	43400 45900	42000 44200	calib test